

ITS TEST REPORT #J20049092, 3005306
TEST OF A WOOD BURNING STOVE
FOR EMISSIONS AND EFFICIENCY
PER EPA METHOD 28 AND 5G-3
MODEL: 3600
FOR
MORSO JERNSTOBERI
DK-7900
NYKOBING MORS, DENMARK
REPORT DATE: 15 AUGUST, 2001

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FOR

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#J20049092, 3005306

MODEL: 3600

FOR

MORSO JERNSTOBERI NYKOBING MORS, DENMARK

TESTED BY:

INTERTEK TESTING SERVICES NA INC. 8431 MURPHY DRIVE MIDDLETON, WISCONSIN 53562

> TEST DATES: August 8-9, 2001 REPORT DATE: August 15, 2001

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I.

#### INTRODUCTION

#### I.A. GENERAL

From August 6 through 9, 2001 Intertek Testing Services NA Inc. (ITS) conducted tests on Morso's model 3600 wood burning stove to determine compliance with U.S. EPA emissions regulations.

Tests were conducted by Bill Keen. Present, as an observer for tests, was Bob Ferguson, a representative of Morso. The tests were conducted at the Intertek Testing Services NA Inc. laboratory located at 8431 Murphy Drive, Middleton, Wisconsin. The laboratory elevation is 860 feet above sea level. Tests were conducted to EPA Method 28 and 5G-3 criteria.

#### I.B. TEST UNIT DESCRIPTION

The Morso 3600 wood burning stove is rectangular in shape. The unit is constructed from cast iron. Two glass and cast iron front doors are hinged on the outside edges while latching in the middle. The doors are latched by closing the left door first and then the right door, with the latch handle located on the right side door. The unit sits on four cast iron legs. The firebox is of single wall construction with firebrick lining. An ash pan is contained inside the unit below a grated bottom. A permanent log retainer is located at the front of the firebox. The lever to control the air setting is located below the ash lip.

#### I.C. RESULTS

The unit as tested produced a weighted average emissions rate of 5.19 grams/hour and did not exceed any of the emissions rate caps specified in the EPA regulations. The unit thus meets EPA certification requirements for 1990.

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#### I.D. PRETEST INFORMATION

The test unit was received at Intertek Testing Services NA Inc. in Middleton, Wisconsin on August 3, 2001 via Tax Air. The unit was inspected upon receipt and found to be in good condition. The unit was set up following the manufacturer's instructions without difficulty. Following assembly, the unit was placed on the test stand and instrumented with thermocouples in the specified locations. Prior to beginning the emissions tests the unit was operated for a minimum of 10 hours at high-to-medium burn rates. The unit was found to be operating satisfactory during this break-in. The 12 plus hours of pre-burning was conducted August 3-4, 2001. The fuel used for the break-in process is all Red Oak cordwood with Douglas Fir scrap as kindling. The moisture content of the cordwood was 16-20% on the wet basis.

Following the pre-burn break-in process, the unit was allowed to cool. The chimney system and laboratory dilution tunnel was cleaned using standard wire brush chimney cleaning equipment.

On August 5, 2001 the unit was ready for testing.

#### I.E. REPORT ORGANIZATION

This report includes summaries of all data necessary to determine compliance with the regulations. Raw data, calibration records, intermediate calculations, drawings and specifications and other supporting information are contained in appendices to this report.

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II.B.

#### SUMMARY OF TEST RESULTS

#### II.A. EMISSIONS

Run Number	Test Date	Burn Rate (kg/hr)	Emission Rate (g/hr)	Adjusted Emission Rate (g/hr)	Heating Efficiency** (% Overall)
1	8/6/01	1.239	3.980	5.728	67.71
2	8/7/01	0.949	1.297	2.257	69.36
3	8/8/01	4.103	6.285	8.369	59.14
4	8/9/01	1.827	5.497	7.489	65.26

<sup>\*\*</sup>Calculated as specified in CSA B-415

WEIGHTED	AVERA	GE CAL	CIII A	LION

		11131	WEIGHTED HYEIGHGE CHECCENTION					
Run Number	Burn Rate	(E) Adjusted Emission Rate g/hr	(OHE)*	Output *(BTU/HR)	Prob	(K) Weighting Factor	(KxE)	(KxOHE)
2	0.949	2.257	69.36	11443.23	.3274	0.5672	1.2801	39.34
1	1.239	5.728	67.71	14940.11	.5672	.5513	3.1581	37.33
4	1.827	7.489	65.26	22030,33	.8788	.4278	3.2041	27.92
3	4.103	8.369	59.14	49474.79	.9950	.1212	1.0145	7.17
					Sums:	1.66756	8.6567	111.76

Weighted Average Emissions Rate:  $8.6567 \div 1.66756 = 5.1913$ 

Weighted Average Overall Heating Efficiency: 111.76 ÷ 1.66756 = 67.02%

\*Calculated as specified in CSA B-415

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II.C. TEST FACILITY CONDITIONS

	Room Ten	nperature	Barometrio		Relative I		Air Velocity	
Run Number	Before After		Before After (in. Hg)		Before After (%)		Before After (ft/min)	
1	90	90	29.30	29.30	84	63	0	0
2	90	88	29.28	29.26	72	67	0	0
3	88	90	29.04	29.03	79	61	0	0
4	84	89	29.00	28.96	63	70	0	0

			£	ITIES					
	Pre	e-Test Load		Test Load					
	Loading	Moisture				Moisture			
	Weight	Content	Coal Bed	Weight	Loading	Content	Piece		
Run	Wet Basis	Dry Basis	Weight	Wet Basis	Density	Dry Basis	Length	Numbe	rof
Number	(lb.)	(%)	(lb.)	(lb.)	$(lbs/ft^3)$	(%)	(in.)	2x4's	4x4's
1	15.49	20.66	3.1	14.87	6.949	21.00	19.00	3	2
2	16.96	20.19	3.4	15.54	7.262	20.42	19.00	3	2
3	15.50	22.04	3.2	15.69	7.332	22.44	19.00	3	2
4	18.31	21.16	3.3	15.61	7.294	20.51	19.00	3	2

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### .E. DILUTION TUNNEL FLOW RATE MEASUREMENTS AND SAMPLING DATA (5G-3)

Ay	verage Di	lution Tunn	el Measuremen	ts	Sample Data				
Run Burn Time Velocity		Volumetric Velocity Flow Rate		Total Samp Temp. Volume			culate (mg)		
Number	(min)	(ft/sec)	(dscf/min)	(°R)	1	2	1	2	
1	270	13.70	141.28	566.50	62.39	63.06	29.5	29.4	
2	370	13.29	137.15	565.79	85.59	86.38	12.9	14.2	
3	85	16.81	147.24	661.10	19.66	19.70	14.1	13.9	
4	193	14.02	136.77	592.38	44.33	44.79	30.0	29.7	

### I.F. DILUTION TUNNEL DUAL TRAIN PRECISION

Run	Sample	Ratios	Total Er (gra	nissions ms)	
Number	Train 1	Train 2	Train 1	Train 2	% Deviation
1	611.45	604.94	18.04	17.79	1.17
2	592.92	587.47	7.65	8.34	7.20
3	636.66	635.26	8.96	8.83	1.37
4	595.49	589.29	17.86	17.50	1.70

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I.G.

### GENERAL SUMMARY OF RESULTS

				Change				
Run Number	Burn Rate (kg/hr)	Average Temperatu Combustion		In Surface Temperature e (F)	Initial Draft (in. H2O)	Primary Air Setting	Run Time (min)	Average Draft (in. H <sub>2</sub> O)
1	1.239	649.50	324.59	-82.60	.065	full closed	270	.060
2	0.949	588.26	305.91	-97.80	.070	full closed	370	.069
3	4.103	1126.10	471.98	-14.60	.096	full open	85	.098
4	1.827	759.00	365.74	-18.00	.072	1-7/8"	193	.076

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#### PROCESS DESCRIPTION

#### III.A. DISCUSSION

RUN #1 (August 6, 2001) The primary air was set at full closed. The test was loaded in 30 seconds. The door was open for 90 seconds and the air control was full open for 5 minutes. Burn time was 270 minutes for a category 2-burn rate of 1.239 kg/hr..

RUN #2 (August 7, 2001) The air control was set at full closed. The test was loaded in 30 seconds. The door was open for 90 seconds. The air control was full open for 3-1/2 minutes and slowly closed till 5 minutes. Burn time was 370 minutes for a category 1-burn rate of 0.949 kg/hr.

RUN #3 (August 8, 2001) The air control was set to full open. The test was loaded in 40 seconds and the door was open for 40 seconds. The air control was not adjusted. Burn time was 85 minutes for a category 4-burn rate of 4.103 kg/hr.

RUN #4 (August 9, 2001). The primary air control was set at 1-7/8" from ash lip. The test was loaded in 38 seconds. The door was open for 90 seconds. The air control was full open for 4-1/2 minutes, then slowly set to 1-7/8" from lip aat 5 minutes. Burn time was 193 minutes for a category 3-burn rate of 1.827 kg/hr.

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III.B.

UNIT DIMENSIONS

30" high, 29.5" wide and 25" deep.

### III.C. AIR SUPPLY SYSTEM

Primary combustion air enters the unit at the rear of the unit and enters the firebox at the front below the grate. Secondary air is channeled up the rear of the firebox and forward in the baffle where it spills out through 4 steps of holes. A single handle controls primary air and secondary air. This handle opens both an oval hole and a parallelogram shaped hole. Combustion products then exit the unit through a six-inch flue collar located centrally at the rear of the stovetop.

### III.D. OPERATION DURING TEST

The unit ran well. The first test did not meet the category 1 burn rate and the second test was run with the same settings but closing down the air control sooner in the start up.

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#### III.E. START-UP OPERATION

Each test was started with a clean firebox and the scale zeroed. A fire was started using newspaper and Douglas Fir scraps for kindling. For the low burns, a pre preload test was used to warm up the stove, then the stove was cleaned out and rezeroed. The rest of the tests were then started with two to three pounds of kindling and a warm-up pre-test load of fuel was put in as space allowed. Pretest loads were fired on high until burning well. Stirring was done as required to insure uniform charcoalization. At least one hour prior to reloading the air control was set to the approximate position used during the test. Stirring was limited to less than 1 minute during the last 15 minutes of the pre-test.

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#### IV. SAMPLING SYSTEMS

#### IV.A. SAMPLING LOCATIONS

Particulate samples are collected from the dilution tunnel at a point 20 feet from the tunnel entrance. The tunnel has two elbows and two mixing baffles in the system ahead of the sampling section. (See Figure 3.) The sampling section is a continuous 13 foot section of 6 inch diameter pipe straight over its entire length. Tunnel velocity pressure is determined by a standard Pitot tube located 60 inches from the beginning of the sampling section. The dry bulb thermocouple is located six inches downstream from the Pitot tube. Tunnel samplers are located 60 inches downstream of the Pitot tube and 36 inches upstream from the end of this section. (See Figure 1.)

Stack gas samples are collected from the steel chimney section 8 feet  $\pm$  6 inches above the scale platform. (See Figure 2.)

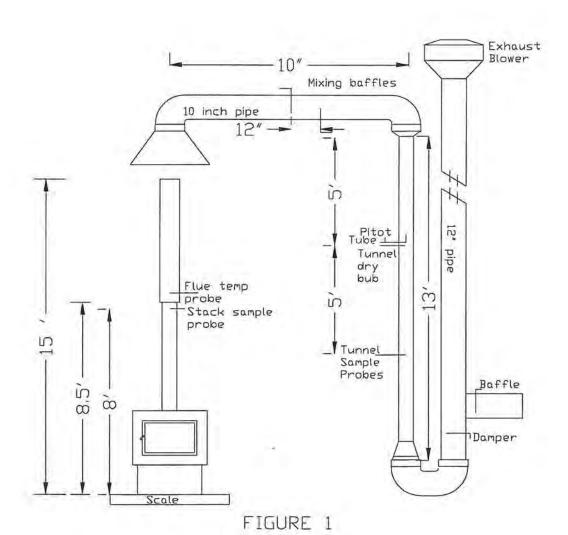
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IV.A.(1)

DILUTION TUNNEL



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IV.B.

#### OPERATIONAL DRAWINGS

IV.B.(1) STACK GAS SAMPLE TRAIN

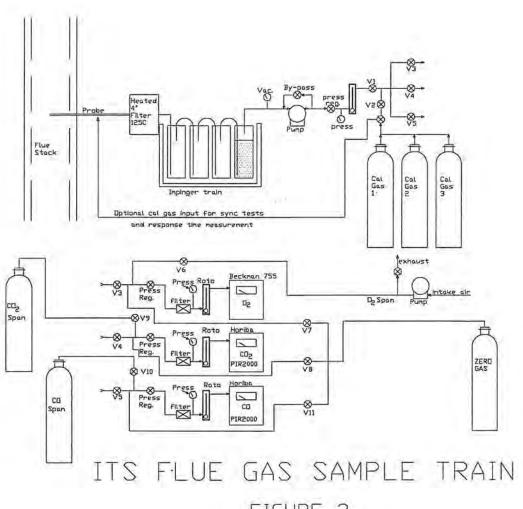


FIGURE 2

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### IV.B.(2). DILUTION TUNNEL SAMPLE SYSTEMS

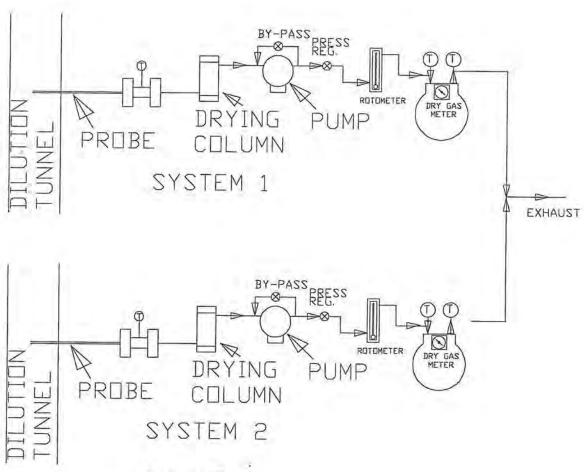


Figure 3

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### IV.B.

### EMISSION AND EFFICIENCY EQUIPMENT LIST

ITEM DESCRIPTION	MANUFACTURER	MODEL	SERIAL#
1. CO2 Analyzer (WHI#010)	HORIBA	PIR-2000	607023
2. CO Analyzer (WHI #009)	HORIBA	PIR-2000	6110019
3. O2 Analyzer (WHI #011)	BECKMAN	755	1001926
4. Dry Gas Meter (WHI #012)	Rockwell	T-110	26866
5. Dry Gas Meter (WHI #013)	Rockwell	T-110	26873
6. Rotometer (WHI # 015)	Matheson	602 Tube	20073
7. Rotometer (3) (WHI # 016)	Matheson	603 Tube	
8. Rotometer (2) (WHI # 019)	Matheson	604 Tube	
9. Hot Wire Anemometer (WHI #021)	Alnor	8525	A 470 1000
10. Inclined Manometer (WHI #022)	Dwyer		MD 1057
11. Pitot Tube (WHI # 044)	Dwyel	125-AV	
12. Manometer 0-10" (WHI #024)	Dwyer	100 10	
13. Mercury Barometer (WHI # 142)		400-10	******
14. Draft Indicator (WHI #027)	Meriam	310EC10WM	184550-X1
15. Scale, 1000# Cap./Record.(WHI #025)	Dwyer	2000-00	R60825 M29
	Toledo Masstron	ML222	8013
16. Readout for 1000# Scale (WHI #007)	NCI	5780	C800174
17. Scale, 75# Capacity (WHI #006)	NCI	3824-100	762117
18. Readout for 75# Scale (WHI #008)	NCI	5780	G800082
19. Analytical Balance (WHI #028)	OHAUS	G-110	5336
20. Dial-o-gram Balance 2610 g (WHI # 031)	OHAUS	1650	
21. Audit Weights 1 mg-100 g/Class-S (WHI # 029)	Ainsworth	4254-S	39392
22. Diaphragm Pumps (4) (WHI # 032 - 035)	Dayton	ZO24 (1) 2Z866 (3)	
23. Method 5H Glassware (WHI # 036)	Andersen	4" Filter, 4-250 ml Im	pingers
24. Gases; Calibration, Zero, Span	Matheson		
25. Regulators for Gases (6) (WHI # 037 - 043)	Matheson	8-(XXXXX)	
26. High Accuracy Needle Valves (9)	Matheson	S. Newscale	
27. Solenoid Valves (12) (WHI # 045)	Dayton		
28. Switches (Misc.) (WHI # 045)	Dayton		
29. ORSAT Gas Analyzer (WHI # 048)	Fisher	D	
30. Oxygen Bomb Calorimeter (WHI # 047)	Parr	1341	4514
31. Moisture Meter (WHI #049)	Delmhorst	RC-1C	14356
32. Humidity Chamber (WHI # 050)	Lab Built	KC-IC	14330
33. Dilution Tunnel (WHI # 046)	Lab Built		
34. Spirometer (WHI # 51)	Lab Built		
35. Data Acquisition System (WHI # 052)	Lab Built		
36. Drying Oven (WHI # 002)	Blue-M	CW 11TA 1	OUT DO
37. Filter Holders, 47-mm (8) (WHI # 053)		SW-11TA-1	SW-291
38. Type-K Meter (WHI #054)	Nalgene	100	10 2 5 5 EV
39. Digital Voltmeter (WHI #055)	Omega	199	21662
	Newport	2004-3	6090022-3
40. Type K Thermocouple Wire 24 Ga.	Gordon	Special Limits of Error	
41. Type K T/C Plugs	Gordon	K-901/900	
42. Dry Gas Meter (WHI #014)	Rockwell	T-110	27002
43. Audit Weights; 5#, 10# (WHI # 160)	Rice Lake Weighing Sys	stem	Class-F
44. Sling Psychrometer (WHI # 126)	Taylor	The state of the s	
45. Chart Recorder (WHI # 056)	Cole-Palmer	2030-0000	221063
46. Infrared Pyrometer (WHI #102)	Omega	OS-2000A	A4048T
47. Class C Weights 1-500 g (WHI # 161)	Ohaus		
48. Bomb Calorimeter Thermometer (WHI # 162)	Parr	1603	3K9347
49. Microtector Gauge (WHI # 103)	Dwyer	1430	
50. Bubble flow meter (WHI # 415)	Humonics	650	570192
51. Soxhlet extractor (WHI # 413)	Fisher Scientific		100000
52. ESS Unit (WHI # 416)	Omni		
53. Unimantle (WHI # 413)			
54. Magnehelic (WHI #027)			

54. Magnehelic (WHI #027) Prepared January 1988 by Rick Curkeet / Rev. May1997 by Rick Armstrong

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V.

#### SAMPLING METHODS

V.A.

#### PARTICULATE SAMPLING

Particulates were sampled in strict accordance with EPA Method 5G-3. This method uses two identical sampling systems with Gelman A/E 61631 binder free, 47-mm diameter filters. The dryers used in the sample systems are filled with "Drierite" before each test run.

#### V.B. EFFICIENCY

Efficiencies reported were based on Method CSA-B415 (calculation). Stack gas analysis for oxygen, carbon dioxide and carbon monoxide was performed in accordance with EPA Method 5H.

### VI. QUALITY ASSURANCE

VI.A. INSTRUMENT CALIBRATION

VI.A.(1). DRY GAS METERS

At the conclusion of each test program the dry gas meters are checked against our standard dry gas meter. Three runs are made on each dry gas meter used during the test program. The average calibration factors obtained are then compared with the six-month calibration factor and, if within 5%, the six-month factor is used to calculate standard volumes. Results of this calibration are contained in Appendix D.

An integral part of the post test calibration procedure is a leak check of the pressure side by plugging the system exhaust and pressurizing the system to 10" W.C. The system is judged to be leak free if it retains the pressure for at least 10 minutes.

The standard dry gas meter is calibrated every 6 months using a Spirometer designed by the EPA Emissions Measurement Branch. The process involves sampling the train operation for 1 cubic foot of volume. With readings made to .001 ft<sup>3</sup>, the resolution is .1%, giving an accuracy higher than the ±2% required by the standard.

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STACK SAMPLE ROTAMETER

The stack sample rotometer is checked by running three tests at each flow rate used during the test program. The flow rate is checked by running the rotometer in series with one of the dry gas meters for 10 minutes with the rotometer at a constant setting. The dry gas meter volume measured is then corrected to standard temperature and pressure conditions. The flow rate determined is then used to calculate actual sampled volumes.

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### VI.A.(3). GAS ANALYZERS

The continuous analyzers are zeroed and spanned before each test with appropriate gases. A mid-scale multi-component calibration gas is then analyzed (values are recorded). At the conclusion of a test, the instruments are checked again with zero, span and calibration gases (values are recorded only). The drift in each meter is then calculated and must not exceed 5% of the scale used for the test.

At the conclusion of each unit test program, a five-point calibration check is made. This calibration check must meet accuracy requirements of the applicable standards. Consistent deviations between analyzer readings and calibration gas concentrations are used to correct data before computer processing. Data is also corrected for interferences as prescribed by the instrument manufacturers instructions. Calibration gases are checked by ORSAT analysis when received to verify suppliers analysis.

VI.B. TEST METHOD PROCEDURES

### VI.B.(1). LEAK CHECK PROCEDURES

Before and after each test, each sample train is tested for leaks. Leakage rates are measured and must not exceed 0.02 CFM or 4% of the sampling rate. Leak checks are performed checking the entire sampling train, not just the dry gas meters. Pre-test and post-test leak checks are conducted with a vacuum of 10 inches of mercury. Vacuum is monitored during each test and the highest vacuum reached is then used for the post test vacuum value. If leakage limits are not met, the test-run is rejected. During, these tests the vacuum was typically less than 2 inches of mercury. Thus, leakage rates reported are expected to be much higher than actual leakage during the tests.

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VI.B.(2).

TUNNEL VELOCITY/FLOW MEASUREMENT

The tunnel velocity is calculated from a center point pitot tube signal multiplied by an adjustment factor. This factor is determined by a traverse of the tunnel as prescribed in EPA Method 1. Final tunnel velocities and flow rates are calculated from EPA Method 2, Equation 6.9 and 6.10. (Tunnel cross sectional area is the average from both lines of traverse.)

Pitot tubes are cleaned before each test and leak checks are conducted after each test.

VI.B.(3). PM SAMPLING PROPORTIONALITY (5G-3)

Proportionality was calculated in accordance with EPA Method 5G-3. The data and results are included in Appendix C.

All tests were conducted, analyzed, and reported on by:

Bill Keen, Engineering Technician

Reviewed By:

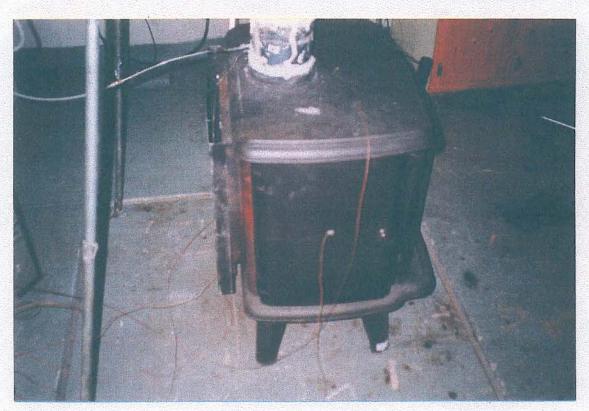
Edwin Hodgson, Project Manager

Richard Armstrong, Engineering Technician

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# APPENDIX A

	rana ratanta il rango	Probert of a const	Intertek Testing	Services	ganne er se sen	amendado propiasado ad al agra		**************************************	1 1 1
			SFBA EPA AD.	II IQTED EMI	ECION DI	CULTO			ļ
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	Date:		8/6/01	** * ****** * ****** ****** * ******	AVERAC	E ADJU	STED EN	ISSION F	5.728
	Run:		1						· · · · · · · · · · · · · · · · · · ·
of the large and the second of the second	roject #:		J20049092	r mark to the state of the stat	Louis comosas	Burn Rat	te (Dry kg	ı/hr):	1.239
A parent monday of a depart	Ouration:		270				i Promoja morano		
	minutes)			ent a ventra in arriva e attino e l'enver	ma emissiona	· ·	1 3000 ( 2000 ) 1000 )	Save dans to make be	
ar a receive receive a selfer				entre garer rema entre en	on reasons		1 		
	incerance contraga	PRESS	URE FACTOR:	0.97928	BARC	METRIC	man a sub-a obcor-	SHOW YOU WANTED A STREET A P.	
	TEMPER	ATLIDE	ACTORS		; {************************************			Average:	C 1 ***** A ***** * *****
	IEWPER	ATURE	FACTORS DGM #1:	0.96627	1 11110 ( 1010 + 1010 )	pareta ones careces	ļ	Start:	
veranvanava			DGM #1.	0.96881	i i vynavnanska i	******	[ ]elener er ein er ein e	End:	29.3
roma suncesid.		***************************************	BOW #2.	0.50001	DDV	SAS MET	ED VALL	!	
	VOLUME	SSAMD	IED	rumi t met nama kanse e s	DKI	JAO IVIL I	DGM #1	of white to be delicate an exercise	304.733
	VOLUME	O OAWI	DGM #1:	62.38804			DGIVI # I	Section is between it represent to	240.132
		***************************************	DGM #2:	63.05914				minda.	240.102
		estra a tra an est	and construction of the second second		ina venane acon I	**********	DGM #2	Final:	650.944
	TOTAL TI	UNNEL \	/OLUME (scf):	38146.929	i i i	************		drawn a service a construction	586.482
	SAMPLE	RATIOS			TEMP	FRATUR	ES (DEC	. RANKIN	
**************************************	**************************************		Train 1:	611.446		*********			546,429
			e Train 2:	604.939	фи г <del>ото</del> п конто кол 1	· · · · · · · · · · · · · · · · · · ·	A STREET P. STREET, S. P. PAGE		545.000
								1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	·
	TOTAL E	OWNERS MY OR SERV	an are no see on see an are an area.		CALIE	RATION	SANTON STANSON	where and an area	
·····		ole Train		18.0377	;		Service more names a	DGM #1:	1.0206
	Samp	ole Train	2 (g):	17.7852		(** )-*****		DGM #2:	1.0311
ина ; mm ; mm	EMISSIO	N RATES	5	nt from Crima Marca Lina	TUNN	EL FLOV	V RATE:		141.285
***************************************	Sample	Train 1	(g/hr):	4.0084	**********	*********		} = + - +	*****
	a state of the state of Attacher	Train 2		3.9523	PART	ICULATE	CATCH	(mg)	
							Sample Tr		29.5
ven vene ed	talk of the state of the state of the state of	Professional Asia Association States of	SION RATES	e to the second state of t		S	ample Tr	ain 2:	29.4
	record a partie of the state of the	Train 1	and a commit second commit contract on	5.7615			marameriana (	; } }	uo porte (20012 n
. : : :	Sample	Train 2	(g/hr):	5.6945	i Pa vona ciona con				erore ione richi
ana sumremma j			ATION:	4 4 3 7 7					
rees reasoning	· · · · · · · · · · · · · · · · · · ·	DE/	/IATION:	1.17%		enacemás intes		, ••••••••••••••	to any and may been appeal

nel mester service in a control in a control	1	Intertek Testing	Services				Transport of Commence of State	1
		SFBA EPA AD	ILISTED EMI	SSION DI	ECHITO	. 500000000 1 4 10-10	enn i timinimis estamaje i	
Commence of a commence of a contraction	<u> </u>	OI DA LI AAD	JOSTED EIVII	SSION KI	ESULIS	100000000000000000000000000000000000000		
Manufacturer:	india transment I	Morso	nin e i nomeno e e somono	i ramanin si mi		RESULT	• • • • • • • • • • • • • • • • • • •	: }
Model:	OWNERS TO SERVICE	3600	en 1444 ist einementer in inscholisisse		, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	INLOULI	O	Emmand parting
Date:	A comment can	8/8/01	***************************************	AVERAC	F AD.III	STED EM	ISSION RATE:	2.25
Run:	Ža nemone ka me E E	2	Alexander & Chipping Science	dament transport			IOOION TATE.	2.20
Project #:		J20049092	minorie vi Sillinos i e s		Burn Ra	te (Dry kg	/hr):	0.949
Test Duration:		370		\$40 = *****   \$4000	CONTRACTOR OF THE PARTY OF THE	, , , , ,	Promovers of a series	
(minutes)								
	enira e e manua.				unda ) kananan			
	PRESS	URE FACTOR:	0.97828	BARO	METRIC	PRESSU	RE	Windson visuojos
		i	- manual		y randidinia cau		Average:	29.2
TEMPER	RATURE	FACTORS				· · · · · · · · · · · · · · · · · · ·	Start:	attract of a debtertable .
~~~		DGM #1:	0.96804				End:	29.2
		DGM #2:	0.96862	k rowona nad	ordele è i diminisca	-		***********
		inne peranami er engang.		DRY	SAS MET	ER VALU	ES	
VOLUME	ES SAMP	reserve a commentant a a section of a be-			,	DGM #1	Final:	393.585
		DGM #1:	85.58870				Initial:	305.031
*	**********	DGM #2:	86.38268					
	unin kanganan					DGM #2	Final:	739.363
TOTAL	UNNEL	VOLUME (scf):	50747.168				Initial:	650.951
SAMPLE	RATIOS	***************************************	n • • • • • • • • • • • • • • • • • • •	TEMP	ERATUR	ES (DEG	RANKIN)	
	Sample	e Train 1:	592.919	V 421 /2 2000 V 40000	W	· · · · · · · · · · · · · · · · · · ·	DGM #1:	545.434
	Sample	e Train 2:	587.469				DGM #2:	***** * * ********* *
TOTAL E	MISSION	JS	andronia i s omorons is to	CALIB	RATION	FACTOR		
and the second of the second states and the second states are second states and the second states are second states and the second states are second states ar	ple Train	the second of the second section is a second section of the section of the second section of the section of the second section of the	7.6487			70101	DGM #1:	1.0206
	ple Train		8.3421	* * ********* * * ****	***************************************		DGM #2:	1.0311
	record ( samonare a		** ** ********* * * ********			rommory souds ; soumous comis		
EMISSIO	ACTION OF THE LAND OF THE PARTY.	THE ASSESSMENT OF THE PARTY OF	· ·	TUNNI	EL FLOW	RATE:		137.155
Sample	e Train 1	(g/hr):	1.2403	<u>.</u>	· magaza vi nin			
Sample	e Train 2	(g/nr):	1.3528	PARTI		CATCH (		
ADILIET	ED EMIC	CION DATES	orania de la composita de la c	ļ		ample Tra		12.9
Market agreement to the contract the	MAN HAND STREET WAS	SION RATES	2 4762	********	S	ample Tra	in 2:	14.2
	e Train 1 e Train 2		2.1762		: :	i. Janes comune	·····	
Sample	C Halli Z	(9/11).	2.3388	•••••••••••••••••••••••••••••••••••••••				
	DEV	/IATION:	7.20%	•••••••				
and francisco			1.2070	•		Jacevsen avenue	A 2 4 2 74 6 10 10 10 10 10 10 10 10 10 10 10 10 10	************

ERATURE MES SAM	SFBA EPA AD.  MORSO  3600 8/8/01 3 0 85  SSURE FACTOR:  FACTORS DGM #1: DGM #2:  IPLED DGM #2:  VOLUME (scf):		AVERA	GE ADJU Burn Ra	PRESSU	JRE Average: Start: End: JES Final:	4.103 29.035 29.04
e: n: #: n: s) PRES ERATURE	MORSO 3600 8/8/01 3 0 85 SSURE FACTOR: FACTORS DGM #1: DGM #2:  PLED DGM #2: DGM #2:	0.97042 0.97184 0.97489 19.65852 19.70168	AVERA	GE ADJU Burn Ra	STED ENte (Dry kg	JRE Average: Start: End: JES Final:	29.035 29.04 29.03
e: n: #: n: s) PRES ERATURE	3600 8/8/01 3 0 85 SSURE FACTOR: E FACTORS DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168	BARC	Burn Ra	STED ENte (Dry kg	JRE Average: Start: End: JES Final:	29.035 29.04 29.03
e: n: #: n: s) PRES ERATURE	3600 8/8/01 3 0 85 SSURE FACTOR: E FACTORS DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168	BARC	Burn Ra	STED ENte (Dry kg	JRE Average: Start: End: JES Final:	29.035 29.04 29.03
e: n: #: n: s) PRES ERATURE	8/8/01 3 0 85 SSURE FACTORS DGM #1: DGM #2: PLED DGM #2:	0.97184 0.97489 19.65852 19.70168	BARC	Burn Ra	PRESSU	J/hr): JRE Average: Start: End: JES Final:	29.035 29.04 29.03
n: #: n: s) PRES ERATURE	SSURE FACTOR: E FACTORS DGM #1: DGM #2: PLED DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168	BARC	Burn Ra	PRESSU	J/hr): JRE Average: Start: End: JES Final:	29.035 29.04 29.03
#: n: s) PRES ERATURE	SSURE FACTOR: FACTORS DGM #1: DGM #2:  PLED DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168		DMETRIC	PRESSU FER VALU DGM #1	JRE Average: Start: End: JES Final:	29.035 29.04 29.03
n: s) PRES ERATURE	SSURE FACTOR: E FACTORS DGM #1: DGM #2: PLED DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168		DMETRIC	PRESSU FER VALU DGM #1	JRE Average: Start: End: JES Final:	29.035 29.04 29.03
PRESERATURE	SSURE FACTOR:  FACTORS  DGM #1:  DGM #2:  PLED  DGM #1:  DGM #2:	0.97184 0.97489 19.65852 19.70168			ER VALL DGM #1	Average: Start: End: JES Final:	29.04 29.03 414.044
ERATURE MES SAM	E FACTORS DGM #1: DGM #2: PLED DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168			ER VALL DGM #1	Average: Start: End: JES Final:	29.04 29.03 414.044
ERATURE MES SAM	E FACTORS DGM #1: DGM #2: PLED DGM #1: DGM #2:	0.97184 0.97489 19.65852 19.70168			ER VALL DGM #1	Average: Start: End: JES Final:	29.04 29.03 414.044
MES SAM	DGM #1: DGM #2: PLED DGM #1: DGM #2:	0.97489 19.65852 19.70168	DRY	GAS MET	DGM #1	Start; End; JES Final;	29.04 29.03 414.044
MES SAM	DGM #1: DGM #2: PLED DGM #1: DGM #2:	0.97489 19.65852 19.70168	DRY	GAS MET	DGM #1	Start; End; JES Final;	29.04 29.03 414.044
	DGM #2: PLED DGM #1: DGM #2:	0.97489 19.65852 19.70168	DRY	GAS MET	DGM #1	JES Final:	414.044
	PLED DGM #1: DGM #2:	19.65852 19.70168	DRY	GAS MET	DGM #1	Final:	
	DGM #1: DGM #2:	19.70168	DRY	GAS MET	DGM #1	Final:	
	DGM #1: DGM #2:	19.70168				Carre - entere - reserve - a	
. TUNNEL	DGM #2:	19.70168	**************************************	***************************************		Initial:	393.620
TUNNEL				************	DOM 40		1
TUNNEL	VOLUME (scf):	12515 759		3	DOM #0		
TUNNEL	VOLUME (scf):	12515 759		James James Land	DGM #2	Final:	759.571
		12010.100				Initial:	739.374
on down , some t san-	4.		Í	· ·			
LE RATIO	A COMPANY OF THE REAL PROPERTY AND ADDRESS OF THE PARTY OF THE		TEMP	PERATUR		. RANKIN	
	ole Train 1:	636.658			the extensive a service between	DGM #1:	
Samp	ole Train 2:	635.264		š Žara sama sama .	Nere Simola mark	DGM #2:	541.600
FMICOLO				i Azamenna sa			
EMISSIC	STREET, SALES AND ASSESSMENT OF STREET AND ADDRESS.	0.0700	GALIE	BRATION	FACTOR	no wy an yy an yy a	are the above to be
mple Trai		8.9769		former men samera	Seren y reserve a series a	DGM #1:	1.0206
mple Trai	n 2 (g).	8.8302	: 	1 19. rann rann ran	ļ.,	DGM #2:	1.0311
ION RATE	ES		TUNN	IEL FLOV	V RATE:	\$ \$ }	147.244
ple Train	1 (g/hr):	6.3366	**********	A***********			· · ·
		6.2331	PART	ICULATE	CATCH	(ma)	errandra arbanuta, krandara a
			ramira mura mus.	C. PRESCRIPTION OF PROPERTY.		service of the the a reservice of the	14.1
TED EMI	SSION RATES	. 2000-1 1.0000		ters a setted a cheese breter		A CAMPAGE OF STREET, STREET, A	13.9
ple Train	1 (g/hr):	8.4258	*********	ganson navor en vo		akon na oo haluu.	
		8.3114		**************************************	**************************************	6-00 - 11-0-2 falls (	
1	VIATION:	1.37%		Sam Emplement	<u>.</u> 		
֡	iple Train iple Train STED EMI iple Train iple Train	ION RATES Iple Train 1 (g/hr): Iple Train 2 (g/hr): IPLED EMISSION RATES IPLE Train 1 (g/hr): IPLE Train 2 (g/hr): IPLE TRAIN 2 (g/hr):	pple Train 1 (g/hr): 6.3366 pple Train 2 (g/hr): 6.2331  STED EMISSION RATES pple Train 1 (g/hr): 8.4258 pple Train 2 (g/hr): 8.3114	pple Train 1 (g/hr): 6.3366  pple Train 2 (g/hr): 6.2331 PART  STED EMISSION RATES  pple Train 1 (g/hr): 8.4258  pple Train 2 (g/hr): 8.3114	iple Train 1 (g/hr): 6.3366 iple Train 2 (g/hr): 6.2331 PARTICULATE  STED EMISSION RATES iple Train 1 (g/hr): 8.4258 iple Train 2 (g/hr): 8.3114	iple Train 1 (g/hr): 6.3366 iple Train 2 (g/hr): 6.2331 PARTICULATE CATCH Sample Tr STED EMISSION RATES iple Train 1 (g/hr): 8.4258 iple Train 2 (g/hr): 8.3114	pple Train 1 (g/hr): 6.3366  pple Train 2 (g/hr): 6.2331 PARTICULATE CATCH (mg)

SFBA EPA ADJ Morso 3600 8/9/01 4 J20049092 193	JUSTED EMIS	AVERAG		RESULT	S	
Morso 3600 8/9/01 4 J20049092		AVERAG		AA 99 WASSAN	S	, , , , , , , , , , , , , , , , , , ,
3600 8/9/01 4 J20049092			E ADJUS	AA 99 WASSAN	S	
3600 8/9/01 4 J20049092			E ADJUS	AA 99 WASSAN		
8/9/01 4 J20049092			E ADJUS	STED EM		5
4 J20049092					ISSION F	7.489
J20049092				A LAMBERT HOLE I HAVE		
193	Canada a come and a company of the c	Same and a succession of the	Burn Rat	e (Dry kg/	/hr):	1.827
S I man hamma a man a man a family			*********	aren ar on anne	San Semalena	enavira secula-
					. dinné + 2000	
URE FACTOR:	0.96858	BARO	METRIC	PRESSU		
					Average:	(
FACTORS					Start:	
DGM #1:	0.96987		*****	 	End:	28.96
DGM #2:	0.97093		أسيجيم بسريا	i		
į		DRY G	AS MET	ER VALU		
LED	was a destrict a seekle to except a justice.			DGM #1	***** - ***** * ***** * *	460.600
DGM #1:	44.32674	n sama tancemi			Initial:	414.366
DGM #2:	44.79301	**********	egyy North House, was entroping North	ACTERNATION	and the second second to	
TOTAL TUNNEL VOLUME (scf):		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	mana agas surges	DGM #2		805.902
VOLUME (SCT):	26396.089				Initial:	759.708
SAMPLE RATIOS Sample Train 1:		TEMP	ERATUR	ES (DEG.	. RANKIN	J)
		***********	(vnnavnnavno	areas references	French and the feet of the second and the second	544.405
e Train 2:	589.290	5			DGM #2:	543.810
TOTAL EMISSIONS		CALIB	RATION	FACTOR	S	
Sample Train 1 (g):			.,	grand to the street of the	DGM #1:	1.0206
2 (g):	17.8647 17.5019		#1400   01400   0400   0	Anne 1 11110 2 1111 1 11	DGM #2:	Lane of State of absence a date
S	*** : **** : **** * **** * ****	TUNN	EL FLOW	/ RATE:	era trassitania ti	136.767
(g/hr):	5.5538	*** 00 ×**00 ***00	*********	2000 8404 25 no	· · · · · · · · · · · · · · · · · · ·	v v v
(g/hr):	5.4410	PARTI	CULATE	CATCH (	(ma)	CHANGE STREET STREET
		man Parket and A		ample Tra	described a second of the	30
SION RATES	Creation Branches & resolution enteres files			ample Tra		29.7
/a/br):	7.5523	***************************************	99 44 50 84 50 KM	and the state of the state of	14 5 6 44 6 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	
(9/111).	7.4248	**************************************			A sand tames same	
(g/hr):	117.3 Parest 1 100.00 1 Parest 1				en Core (more)	100, 1 1000 1 2 100 7 2 100 1
A 160	g/hr):	g/hr): 7.5523	g/hr): 7.5523	g/hr): 7.5523	g/hr): 7.5523 g/hr): 7.4248	g/hr): 7.5523

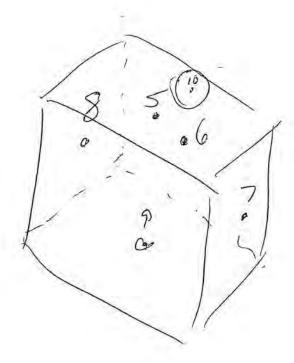
		Page of S
Manufacturer <u>Morso</u>	Model 3600 Wood Stove	Date 8/3/
Job# J20049092	Tech_	24
Emissions Test	ing Initial Stove Check Out	4
Date received: \$\langle 3/01	Carrier: /a	a Air
Shipping damage?Yes	Describe damage	
If damaged, repairable?NoYes		
Repairs affected by:	Date:	
Client notified about irreparable damage by:	Date:	
Disposition:		
Safety Certified by:	Safety Control#	
Overall Unit Dimensions: High 30"	Wide 2.9 /2 Deep 2	5"
Comments:		
Initialed: 13.4		

16	a y law also and in the		Page Z of S
Manufacturer Morso	Model 3600 Wood Sto	ve	Date 8/6/
Job#J20049092		Tech_	arc.
Unit description (check all that apply)	TESTING UNIT PREPARATIO		
Stove	⊆Top Vent Rear Vent		Manual Draft
	Kear vent		Bimetal Spring Remote Thermostar
Non-catalytic	Shale ≥Ashpan		Blower or Fans
Other;	<u>Crisipan</u>		Diower of Paris
Drawings: Yes Specifications: Yes Materials of construction: Ca Air introduction: controlled Control mechanism: handle in Unit net weight with all components:	No No No at rear trent trent 1967	Kg.	
Unit fire box volume: 2,19	Ft' (attach fire box volume calcu	ılations a	and drawings)
Ideal Load Weight: 14,98			
Load Weight Range: (±10% of ideal weight	ght) 13.48 lbs. to 16,48	lbs.	
Ideal piece length specification: 2 ( Thermocouples attached: 8/3/0/	inches. (5/6 of longest fire b	ox dimer	ision)
Thermocoupies attached. 0/0/0/	_Attached by	(attach 1	(/C map)
Unit	t conditioned prior to test		
10 hours at medium	50 ho	urs at me	dissa
burn rate (non-catalytic)			ach burn log)
(attach burn log)	buin	raic (aid	acii ourii iog)
Date started: \$\frac{3}{0}\] Catalyst manufacturer: \( \)	Date comp	leted:	8/4/01
	nensions:Cell	size:	cells/in,2
Unit ready for testing (date): 8/6	/0/ Initialed:	0.1.2	

			Page 5 of 5
Manufa	cturer Morso	Model 3600 Wood Stove	Date 8/6/01
Job#	J20049092	Tech	3111

### Thermocouple Location

Thermocouples are placed centrally on the top, back, right and left sides and the bottom and numbered as shown below.

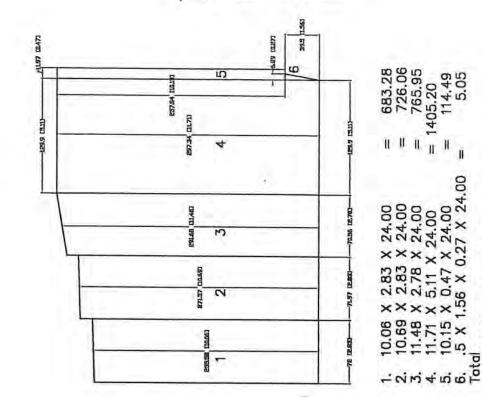


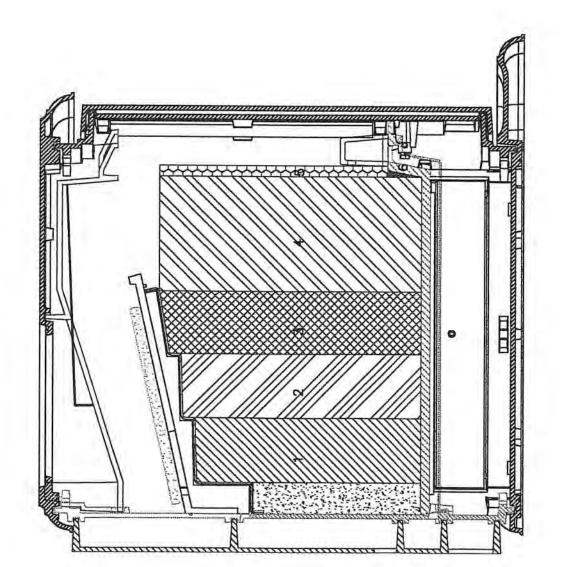
TC#	LOCATION
5	UNIT TOP
6	UNIT BACK
7	UNIT RIGHT
8	UNIT LEFT
9	UNIT BOTTOM

Manufa	acturer <u>Morso</u>	Model 3600 Wood Stove Date \$\( \) \( \) Date \( \) \( \) \( \) Date \( \)
Job#	J20049092	Tech
	Measurements By:	Checked By:
		FIRE BOX VOLUME CALCULATION
		See computer drawings

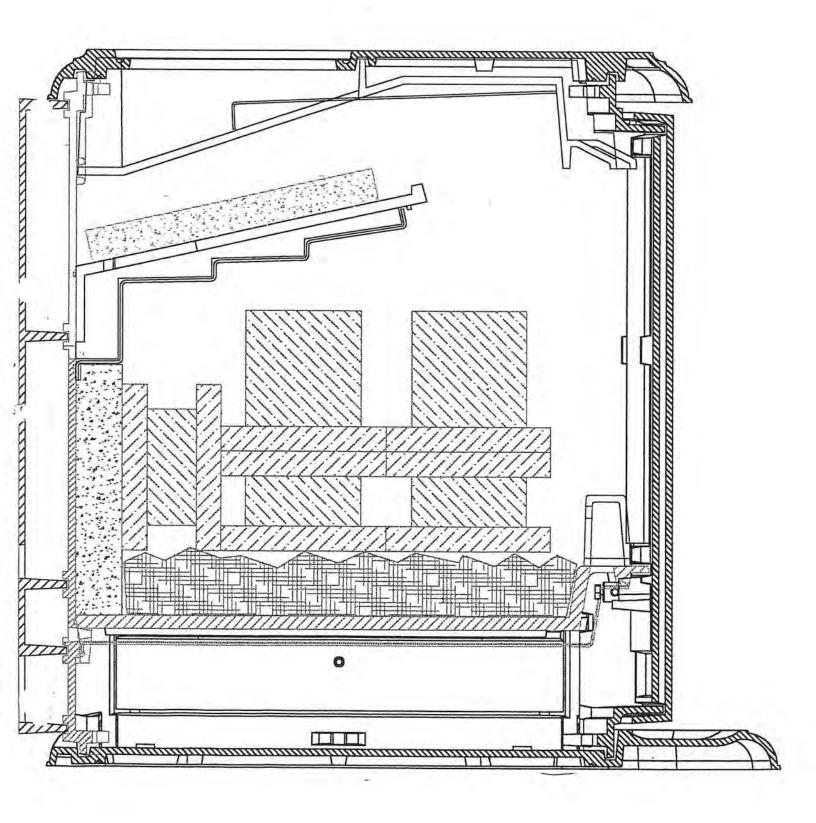
PAGE 5 OF 50

= 3700.03 cubic inches 3700.03 / 1728 = 2.141 cubic feet





PAGE - 0,=-



Manufacturer Morso		Model	3600	Page 7 of S
ob # J20049092		Run_	1	Date S/C
PRETEST DILUTION  Barometric pressure (  Inside diameter: Port .  Pitot tube type: Standa	P <sub>bar</sub> )2 <i>9.23</i> (inches A <u>6in.</u> Port B <u>6</u>	AVERSE RUN Hg.) Static pressure Sin. Tunnel cross so	(P <sub>q</sub> ) (inches ectional area: 0.196	w.c.) 3Ft
Traverse Point	Position (inches)	Velocity Head $\Delta_p$ (inches $H_2O$ )	Tunnel Temperature (°F)	$\sqrt{\Delta_2}$
A-Centroid	3.00	.04/	124	.2025
B-Centroid	3.00	1041	116	,2125
A-1	0.40	,046	122	1000
A-2	1.50	1041	124	12025
A-3	4.50	.041	124	12025
A-4	5.60	,037	122	,1924
B-1	0.40	,039	117	1975
B-2	1.50	04/	116	12025
B-3	4.50	041	116	2025
B-4	5.60	,039	118	1844
		AVERAGE	1199	11989
djustment factor applicati $V_s = K_p C_p F_p \left( \sqrt{\Delta_p} \right) A$		$S_s = K_p C_p \left( \sqrt{\Delta_p} \right) a v g . \sqrt{\frac{1}{2}}$	7,77,770	14
nere, = Pitot tube coefficient = 0.99 = manometer reading (inche = average absolute dilution tu	s H <sub>2</sub> O)	$F_{p}$	Pitot corre $= \frac{\left(\sqrt{\Delta_p}\right) avg}{\left(\sqrt{\Delta_p}\right) centroid}$	ction

P<sub>r</sub> = absolute dilution tunnel gas pressure or Pbar + P<sub>g</sub>

inchesH<sub>2</sub>O 13.6

P<sub>B</sub> = static pressure

 $M_{\star}=28.56$ , wet molecular weight of stack gas (alternatively, it may be measured)  $K_{p}=85.49$  Pitot tube constant, (conversion factor for English units)

Adjustment factor for alternative Pitot tube placement:

 $(\sqrt{\Delta_p})avg$ . = Average of the square roots of the velocity heads  $(0_p)$  measured at each traverse point.

 $(\sqrt{\Delta_P})$  centroid = Average of the square roots of the velocity heads measured at the tunnel centroid (inches of  $H_2O$ )

		Pag	e of of
Manufacturer Morso	Model 3600	Da	te 8/6/01
Job # J20049092	Run/	Tech_	N'C
Pre/Post Checks			
Moisture Meter Calibration Check:	Time: 6 30 X	: L Y: C	12: _ 22:
		Pre-Test	Post-Test
Facility Conditions:		A - 1	
Air Velocity		O fpm	<i>O</i> fpm
Smoke Capture Check	manimum manimum -		
Wood Heater Conditions:			
Date Wood Heater Stack Cleaned		2/4/01	
Date Dilution Funnel cleaned		\$ 19/11	
Induced Draft Check	G6000000000000000000000000000000000000	1/2	(2)
Tunnel Velocity		NEID	NUN
Flow Rate 140-cfm ±10%		.070	141, 285
Pitot Leak Check:			
Side A		0 - 1	
Side B			
Temperature System: Ambient (65°- 90°F)			90 °F
Wood Heater Surface (±125°F)	***************************************		-82.6 °F
Proportional Checks:		_	
CO Analyzer Drift Check		ommunionio 🗀	
CO <sub>2</sub> Analyzer Check			
O <sub>2</sub> Analyzer Check		mountaine .	
Thermocouple check			
Sampling Train ID Numbers:		Train 1	Train 2
Probe		1	2
Filter Front		41	11
Filter Back		Zn I	12
Filter Thermocouple.		19	22
Filter 5G-3 (<90°F)	And a few to have an a second of the first to the first t		_
Thermocounts Identification Non-Lo-			
Thermocouple Identification Number	Koom2	Dilution Tunnel Dry Bulb.	
Dilution Tunnel Wet Bulb       4         Unit Right Side       7         Catalyst/Combustion Chamber       10	Unit Top5 Unit Left Side8	Unit Back Unit Bottom	

		Page 9 of 3 b
Manufacturer Morso	Model 3600	Date 3/6/01
Job # J20049092	Run	Tech

### Pre-Test Scale Audit

Scale Type	Audit V	Audit Weight		-
Platform	1	) lbs., Class F	10.0	lbs.
Wood	10	lbs., Class F	10.00	lbs.
Analytical	100 Grams	mg, Class S	Grams /'00, 1	mg.

#### LIMITS OF WEIGHT RANGES

ANALYTICAL SCALE:	50%-150% of dry filter weight, ± 0.1 mg
PLATFORM SCALE.	20%-80% of ideal test load weight, ± 0.1 lbs. or 1%
	20%-80% of ideal test load weight, ± 0.1 lbs. or 1%

		Page/Oof Jo
Manufacturer Morso	Model 3600	Date # 16/01
Job # J20049092	Run/	Tech_3

## SAMPLING EQUIPMENT CHECK OUT

#### Leakage Checks Tunnel Samplers

		SYSTEM 1		SYSTEM 2			
Unplugged Flow Rate = .25cfm		Pre-Test	Post-Test	Pre-Test	Post-Test		
Vacuum (inc	ches Hg.)	104	10"	164	104		
Final	1 minute DGM (ft <sup>3</sup> )	240, 132	304741	586.482	650.948		
Initial	1 minute DGM (ft <sup>3</sup> )	240,132		586.482			
Change (C)	(ft³)	()	0	0	0		
Allowable le	akage .04 x Sample rate or .02cfm	0.0100	0.0100	0.0100	0.0100		
Check OK		V					

#### Leakage Checks Flue Gas Sampler

Plugged Probe	Pre Test	Post Test
Vacuum (inches Hg.)	10"	10"
Rotometer Reading (mm)	Ö	0
Flow Rate (CFM)	0	0
Allowable (.04 x Sample Rate)		
Check OK	V	

		Page 11 of 50
Manufacturer Morso	Model 3600	Date 8/6/11
Job # J20049092	Run/	Tech 200

### **CONTINUOUS ANALYZERS**

Pre-Test (Adjust and Record)

	ZERO		SPAN		CAL. (Record Only)	
со	00,00	00.00	9.96	9.96	00-96	.999
CO <sub>2</sub>	00.00	66.00	24.65	24.65	9.65	9.99
O <sub>2</sub>	00.00	00.00	20.93	20.93	10.27	10.2
	Actual	Should Be	Actual	Should Be	Actual	Should Be

#### Post Test (Record Only)

	Zero	Span	€al.	Zero Drift	Span Drift	Cal. Drift	OK?	Not OK*
со	00.00	10.05	06.96	-0-	.09	-0-	/	
CO <sub>2</sub>	06.00	24.80	9.70	-0-	.15	.05	/	
O <sub>2</sub>	00.01	20.83	10.27	-01	.10	-0-	/	

<sup>\*</sup> Greater than ± 5% of the range used.

		Page / 2 of 50
Manufacturer Morso	Model 3600	Date \$/6/07
Job # J20049092	Run/	Tech_ 72-1

#### TEST DATA LOG

#### RAW DRY GAS METER READINGS

	System 1	System 2
Final (ft³)	304,733	650, 944
Initial (ft³)	246, 132	586.482

#### AMBIENT CONDITIONS

	Start	End
Barometer. (inches Hg)	29,30	29.30
Wet Bulb (°F)		
Dry Bulb (°F)	74	79
Humidity (%)	84	63

Manufactur	er Morso							13 of 50	
lob # J2004	775				Model 3600			e 8/3/0/	
	.,				Kun	-	Tech_ s	W/	
		DILUTIO	N TUNNEL	PARTICU TER TYPE: Gelman	LATE SAM	PLER DATA	A		
		Sample	s in Desecrator.	Date TEM 1	8/6/01	Time: /47.			
		Probe and		Filter		Probe and Fr	SYSTI	20.7%	
Post To	est Weight:	Half Hou		Numbers		Half Housing	# 2	Filter Numbers /	1,12
-	950	91,9	40 grams	,246	3 grams	91,624	grams	, 2453	grams
	st Weight:	91.43	95 grams	2174	The second of the	91.624		.2/62	Grams
	Gain:	,00	06 grams	,0289		,0003	Wanted by	.0291	Grams
		10 7 30	al al		b1	a2		b2	
T	otal Gain:	-1 + h1 -	295	and a	55.00	200		4	
	otal Calli.	a1+01-	29.5 mg SYSTEM 1	rams	a2 + b2	2=29.4 m SYSTEM 2	grams	-1	
. W Re	e-test eight ecord	Probe & Housing Number	Front Filter Number	Back Filter Number	Probe & Housing Number	Front Filter Number	Back Filter Number	TEMP	HUMII
Date	Time	1	9	10	2	1/	/2	°F	%
8/3/01	1515	91.9395	11145	.1000	9/6247	1145	.1018	78	4/9
8/4/4	10:00	91.8395			91,6246	1144	1020	76	47
8/5/01	9:20	91,4395	.1144	.1031	91.6243	,1144	1018		48
8/6/01	6:10	91.4395	1144	1030	91.6242	1144	.1018		49
		Total	217	14	Total	,2/	62	170	1//
			SYSTEM 1			SYSTEM 2			
We	-test eight cord	Probe & Housing Number	Comb Filter V Num	Veight	Probe & Housing Number	Com Filter	ibined Weight mber	TEMP	HUMID
Date	Time	1	1	0	2	11	12	°F	%
\$/6/W	14:36	91.4411	,248	72	91,6279	.248		A5	46
8/7/01	5:45	91,4407	,247	0	91.6245	-243	53	75	48
3/8/01	6:58	91,4401	. 246-	5	91,6245	,245	5.3	74	45
1/8/01	7:11	964401	,246	3	91.6245	-245		73	88

		Page	Lof Sp
	_ Model 3600	Date	8/6/01
	Run/	Tech	12
FUEL DAT	A		
Consisting of: Scra	p and paper	Fire lit Time Time loaded:_i Vet:_/7,/2_%	6:55
full a	closed	Time:	2159
			per Limit
13.47 L	os. 14,58	lbs. 16,	48 Lbs.
14996 F	t.3 Loading Dens	ity: 6.9	9.0 Inches 199 lbs/ft³ 62 lbs/ft³
Weight	Meter Mois	ture Content /0/ d-//*	
			-
			18.1%
2-/2 lbs.		The state of the s	20.1%
4.28 lbs.			20.1%
			18.1%
lbs.	%	%	%
lbs.	%	%	%
	Consisting of: Scra Consisting of: 19.33 % Corre  TEST I  Lower Limit  2, / / F  4/14/6 F  // 3/4x1/2  Weight  2.30 Ibs.  2.42 Ibs.  2.42 Ibs.  4.28 Ibs.  1bs.  Ibs.	FUEL DATA  PRE-TEST LOAD  Consisting of: Scrap and paper Consisting of: 2X4X_\(\text{D}\), \(\text{P}\) inches \(\text{C_3}\) \( \text{Corrected Dry: \( \frac{1}{2}\) \( \frac{1}\) \( \frac{1}\) \( \frac{1}{2}\) \( \frac{1}\) \( \frac{1}{2}\) \( \frac{1}\) \( \	FUEL DATA  PRE-TEST LOAD  Consisting of: Scrap and paper

facturer <u>Morso</u> J20049092	Model 3600  Run	Date <u> </u>
COMMENTS		
2.7 16, krulle	+ the started	
7:00 12 3-	165 of kindling add	1
8:35 Stub		<u>eq</u>
1 3 NUE	cleanestout, scale	rezeroed
0,	11 01 11 11	
8:37 6.91	bs of kindling adds	d
8:42 - 7,77	1 (bs of preload adde	d
	/	
8:50 Rememble	- of preload added	
11 (11)	President statements	
11		
	Je.	
	TEST LOA	AD CONFIGURATION
	/-	
	71	
	back last	
	back 1	

Manufacturer Morso					_ Mo	odel 36	500			Date	8/	110	1		
Job # J20	049092						Run/				Tech on L				
			An	r cc.	nhol	1 /	1/	1	lase	1					
SWITCH	H NUMBE	ER	1	2	3	4	5	6	7	8	9	10			
READING#	REAL TIME ELAPSED TIME	WEIGHT	FLUE GAS TEMP	ROOM TEMP	TUNNEL DRY BULB	TUNNEL WET BULB	UNIT TOP	UNIT BACK	UNIT RIGHT SIDE	UNIT LEFT SIDE	UNIT BOTTOM	CATALYST DOWNSTREAM	TUNNEL	DRAFT	SMOKE
0 9:	00 0	9,00	77/	90	225	81	677	196	335	348	488	1227		1098	
1	10			90	/32	80	646	205	357	358	480	963	040	1084	6
2	20		485	90	128	8/	624	215	348	341	465	967	1641	.081	2
3	30		463	20	122	80	_	214	391	333	448	889	10 7/	1078	C
4	40		436	20	115	81	525	214	337	326	434	254	.040	154	2
5	50		424	20	113	80	555	2/4	332	323	429	841	.040	mI	C
6	60		375	90	108	81	521	215	326	322	429	732	,04/	.062	
7	70													.02	-(
8	80				i E i					7			-		
9	90	f							1				175		
10	100	)			- 11										
11	110	)							1 = 1						
12	120	)													
13	130	)			1										
14	140												1		
15	150														
16	160	(8)			Œ										
17	170		V										6.5		
18	180				1			- 4	1-						
19	190	U. O. S. A.													
20	200	1				1					6 - 14				
21	210											-	1117		
22	220	10 -							1	-	1				
23	230												- 17		
24	240	N E													
25	250														-

## Comment of the com		- 1
1,429   1,43   7,15   1,43   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45   7,45	SE DGM1	TUNN VELC
1, 10, 11, 11, 11, 11, 11, 11, 11, 11,	R G	RELECTIVE STREET
Column	12 18 34 196 2 13	76 76 30 .000 1065 C
Charles	1 20 79 89	1 79 77 100
8.5% 3.3 (20) (2) (2) (2) (2) (2) (2) (2) (2) (2) (2	81 80 90 593,5	J. 180. 06 77
1, 10, 10, 10, 10, 10, 10, 10, 10, 10,	82 81 90 595 9 1	90 .040
10	83 82 90 598, 2	82 80 90 ,090
\$\frac{1}{2}\text{Atol.} \text{  \$\frac{1}{2}\text{  \$\frac{1}{2	85 83 90	183 181 90 ,040, 079 58
Short   Shor	85 84 90 603.0	84 82 90 LOSO 090 LB
2.20 1.47 80.53 11.15 7.20 11.00 8.7 14.77 3.00 50.00 15.2 12.2 14.2 15.3 14.1.5 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.10 17.	86 85 90 605.3	1001 06 48 58
R. 20, 2.47, 1.47, 1.21.2	86 86 90 667.7 1	PS 23 90,040,006 C
Part	87 87 90	S6 25 90 100 1005 C
8.430 137 73.44 134.7 34.7 34.7 34.7 34.7 34.7 34.7 34.7	1 5.51 2 88 88 88	87 85 90 ,040 CE/C
8.2.0 137 (6.72) 13.5.6 10.0 12.7 13.6 13.5 13.5 13.5 13.5 13.5 13.5 13.5 13.5	1 6 619 58 88 88	187 186 189 1050
1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00   1.00	88 84 84 617.3	187 86 189 JONG 1057 C
1.20	29 84 84 619,7	040. 88 78 88
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COMMENTS: 1355 EC		

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Manufacturer_Morso	Model 3600	Date 8/7/09
Job # J20049092	Run_2	Tech 92

PRETEST DILUTION TUNNEL TRAVERSE RUN

Barometric pressure (Pbar) 2728 (inches Hg.)

Static pressure (Pg) 1/9 (inches w.c.) Inside diameter: Port A 6in. Port B 6in. Tunnel cross sectional area: 0.1963Ft

Pitot tube type: Standard

Traverse Point	Position (inches)	Velocity Head $\Delta_p$ (inches $H_2O$ )	Tunnel Temperature (°F)	$\sqrt{\Delta}$
A-Centroid	3.00	. 040	121	.2000
B-Centroid	3.00	,040	123	,2000
A-l	0.40	,036	123	1897
A-2	1.50	-040	123-	,2000
A-3	4.50	,040	121	,2000
A-4	5.60	,035	123	1.187/
B-1	0.40	,038	121	.1989
B-2	1.50	,040	122	,2000
B-3	4.50	,040	123	,2000
B-4	5.60	0035	120	1.1871
		AVERAGE	1218	.1959

Adjustment factor application

$$V_s = K_p C_p F_p \left( \sqrt{\Delta_p} \right) AVG \sqrt{\frac{T_s}{P_s M_s}} \qquad V_s = K_p C_p \left( \sqrt{\Delta_p} \right) avg. \sqrt{\frac{T_s}{P_s M_s}}$$

Pitot correction

Cp = Pitot tube coefficient = 0.99 for standard pitot

 $\Delta_p$  = manometer reading (inches H<sub>2</sub>O)  $T_s$  = average absolute dilution tunnel temperature (°F + 460)

Pr = absolute dilution tunnel gas pressure or

inchesH10 13.6

Phar + Pg

Ps = static pressure

M. = 28.56, wet molecular weight of stack gas (alternatively, it may be measured)

Adjustment factor for alternative Pitot tube placement:

Kp = 85.49 Pitot tube constant, (conversion factor for English units)

= Average of the square roots of the velocity heads ()p) measured at each traverse point.  $\sqrt{\Delta_P}$  centroid = Average of the square roots of the velocity heads measured at the tunnel centroid (inches of  $H_2O$ )

		I	Page / Pof 50
Manufacturer Morso	Model 360	0 1	Date
Job # J20049092	Run	Tech	21
Pre/Post Checks		and the second	
Moisture Meter Calibration Check:	Time: 6:50	X: Y:	12: - 22:
Facility Conditions:		Pre-Test	Post-Test
Air Velocity		8 fpm	O fpm
Smoke Capture Check		~	
Wood Heater Conditions:		-	
Date Wood Heater Stack Cleaned		\$ 141.01	
Date Dilution Tunnel cleaned		8/4/01	
Induced Draft Check		6	0
Tunnel Velocity	.,	.040	.027
Flow Rate 140-cfm ±10% Pitot Leak Check:			137, 155
Side A		V	
Side B			_
Temperature System:			
Ambient (65°-90°F)			38,8 °F
Wood Heater Surface (±125°F)			-97,8 °F
Proportional Checks:			
CO Analyzer Drift Check			V
CO <sub>2</sub> Analyzer Check			
O <sub>2</sub> Analyzer Check			
Thermocouple check			V -
Sampling Train ID Numbers:		Train 1	Train 2
Probe		)	c/
Filter Front		13	15
Filter Back	A CONTRACTOR OF THE PROPERTY O	14	16
Filter Thermocouple.	The second secon	19	22
Filter 5G-3 (<90°F)		V	V
Thermocouple Identification Number			
Flue	Room2 Unit Top5	Dilution Tunnel Dry Bu Unit Back	
Unit Right Side'7 Catalyst/Combustion Chamber10	Unit Left Side8	Unit Bottom	

		Page 20 of Jo
Manufacturer_Morso	Model 3600	Date 8/7/07
Job # J20049092	Run 2	Tech B

### Pre-Test Scale Audit

Scale Type	Audit	Weight	Measured Weight	
Platform	10	) lbs., Class F	10,0	lbs.
Wood	10	lbs., Class F	10,00	lbs.
Analytical	100 Grams	mg, Class S	Grams 999	mg.

#### LIMITS OF WEIGHT RANGES

ANALYTICAL SCALE:	50%-150% of dry filter weight, $\pm 0.1 \text{ mg}$
PLATFORM SCALE	20%-80% of ideal test load weight, ± 0.1 lbs. or 1%
	20%-80% of ideal test load weight, ± 0.1 lbs. or 1%

		Pageof_So
Manufacturer Morso	Model 3600	Date 8/7/01
Job # J20049092	Run 2	Tech_ 2

### SAMPLING EQUIPMENT CHECK OUT

#### Leakage Checks Tunnel Samplers

		SYST	ГЕМ 1	SYSTEM 2			
Unplugged Flow Rate = .25cfm		Pre-Test	Post-Test	Pre-Test	Post-Test		
Vacuum (inches H	Ig.)	100	v 10"	10"	10 4		
Final 1	minute DGM (ft <sup>3</sup> )	305.001	293.592	650,951	739.373		
Initial 1	minute DGM (ft <sup>3</sup> )	305,031	THE CORPORATION AND ADDRESS.	650.951	739,37/		
Change (C) (	ft³)	0	2001	Ó	1002		
Allowable leakage	e .04 x Sample rate or .02cfm	0.0100	0.0100	0.0100	0.0100		
Check OK		L		V	()		

#### Leakage Checks Flue Gas Sampler

Plugged Probe	Pre Test	Post Test
Vacuum (inches Hg.)	10'	104
Rotometer Reading (mm)	0	0
Flow Rate (CFM)	0	Q'
Allowable (.04 x Sample Rate)	*	
Check OK		L

		Page 22 of So
Manufacturer_Morso	Model 3600	Date 8/7/0/
Job # J20049092	Run_2	Tech_ 3

#### **CONTINUOUS ANALYZERS**

Pre-Test (Adjust and Record)

	ZE	RO	SPAN		CAL. (Record Only)	
co	00.00	00.00	9-96	9.96	.95	.999
CO <sub>2</sub>	00.00	00:00	24.65	24.65	9.64	9.99
O <sub>2</sub>	00.01	00.00	20.93	2093	10.28	10.2
	Actual	Should Be	Actual	Should Be	Actual	Should Be

#### Post Test (Record Only)

	Zero	Span	Cal.	Zero Drift	Span Drift	Cal. Drift	OK?	Not OK*
со	0.06	10.04	4.16	0	1.08	e01		
CO2	0,00	24,88	9.72	0	,23	80.		
O <sub>2</sub>	104	20.PS	10,24	.04	.08	.09		

<sup>\*</sup> Greater than  $\pm$  5% of the range used.

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Manufacturer_Morso	Model :	3600	Date 8/7/0/
Job # J20049092	Run_	2	Tech 2

#### TEST DATA LOG

#### RAW DRY GAS METER READINGS

	System 1	System 2
Final (ft <sup>3</sup> )	393, 585	739, 363
Initial (ft <sup>3</sup> )	305.031	650,951

#### AMBIENT CONDITIONS

	Start	End
Barometer. (inches Hg)	29,28	29.26
Wet Bulb (°F)		
Dry Bulb (°F)	75	80
Humidity (%)	72	67

danii factii	rer_Morso				2.507 (10.70)		Page	24.50	
ob # J200					Model 3600 Run 2		Date Tech	3/4/01	/
			FI s in Desecrator	LTER TYPE: Gelman Date	The state of the s	PLER DAT			
		Dealthani		STEM 1			SYSTE	EM 2	
n	V	Half Hou	Probe and Front Half Housing # Filter Numbers			Probe and Fr Half Housing		Filter Numbers	15.1
Post I	est Weight:	93, 1153 ,20		1,241	) grains	89 06	grams	230	gram
Pre T	est Weight:	93,1136 grams		.230	grams	89.96	grams	-1/	Gram:
	Gain:	prams			prams		The Description	.210	Gram:
	0017		1 1		2	-000°	7	,0135	}
		1	181					02	
1	otal Gain:	a1 + b1 =	12.9m	grams	a2 + b2	2 = 14,2 m SYSTEM 2	grams		-
. W	e-test eight ecord	Probe & Housing Number	Front Filter Number	Back Filter Number	Probe & Housing Number	Front Filter Number	Back Filter Number	TEMP	HUM
Date	Time	3	13	14	4	15	16	°F	%
8/4/01	10:03	93,114	1151	1154	89.9651	.103/	1143	76	43
8/5/0/	9:25	93, 1139	.1151	1153	29,9651		. 1141	76	48
8/6/01	6:15	93,1139	1151	1154	89.9651	.1031	-1139	76	49
8/2/01	5:50	93,1136	-1151	1154	89.9651		.1139	76	45
		Total	, 236		Total	12/6	29	100	10
	-		SYSTEM 1			SYSTEM 2			
Pre-test Probe & Weight Housing Record Number		Filter	bined Weight nber	Probe & Housing Number	Con Filter	nbined Weight	TEMP	ним	
Date	Time	3	13,	14	9	15	mber //	°F	%
11/5/8	1607	93/1/62	,242	6	89,9678	.233	1	87	87
8/8/01	7:05	93,1154	291		89.9674	2308		74	45
9/9/01	7:15	93,1153	. 2418	,	89,9663	230		74	98
3/10/01	7:25	93.1153	,24/7	7	81,9660	230	4	72	146
8/13/01	P:15	93,1153	,2417		89,9660	.2307		75	88

			Page 2	5 of 50
Manufacturer Morso		Model 3600	Date	8/7/01
Job # J20049092		Run 2	Tech_	n/
	FUEL DATA	A		
	PR	E-TEST LOAD		
FUEL DESCRIPTION: Kindling weight: 109 lbs. Pre-test load weight: 16.56 Pre-test moisture content: Uncorre	Consisting of: Scrap  Ibs. Consisting of:	N. COLONIA PROCESS	Fire lit Time Time loaded:  Vet: /6/50 %	
Test Air Control Settings: Test Unit Fan Settings:	full close	ed .	Time: <b>{</b>	9131
-	TEST L	OAD		
di Grence De	Lower Limit	Ideal	Up	per Limit
Test Load Weight:	13,48 Lb	s. 14-98	lbs. (6)	, E Lbs.
Fire Box Volume:  Load Volume:  Number of Spacers  Piece Size	2,/9 Fi -9986 Fi -/6 3/4x11/2x	Loading Densit	ity: 7,2	), () Inches (62 lbs/ft <sup>3</sup> 4/6 lbs/ft <sup>3</sup>
2 x y x /9 in.	2-25 lbs.	20.5 %	192%	18.6 %
2 x 4 x 19 in	2.19 lbs.	19.6 %	18.6 %	18.5 %
2 x 4 x 19 in.	2.50 lbs.	20.5 %	19.0 %	18.7 %
4 x 9 x 19 in.	4.55 lbs.	18.8 %	18.5%	18.0 %
9 x 9 x 19 in.	4.05 lbs.	19.6 %	18.3 %	26.2 %
x x in	lbs.	%	%	%
X X in.	lbs,	%	%	%
*Uncorrected range = 17.9% to 23  TEST LOAD WEIGHT: \( \sum_{\subseteq} \sum_{\subseteq} \sup_{\subseteq} \sup_{\subseteq} \)  AVERAGE MOISTURE CONTEN' (DRY) \( \sup_{\subseteq} \sup_{\subseteq	Libs.  CORRECTED TO TWO bs. to 3,8 lbs.	to a transfer of the second se	4,10,42,52	rg. <u>96</u> % veight

0049092		Run 2	Date of 7
COMMENTS			
6:43	2 7 /6	. LS.1/5. 24	lanted
1140	160-1	- 4(1()	1/1
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7.51	2,1165	kindly add	el
	0 1 /		
8:00	Stove cle	anellent	
8196	1,8 /65	Kridling Stav	41
8109	8,74 /6s e	of some Took and	lded
8124	Restat prelo	ad added	Men
0-27	ROFA Preio	RA CHINELL	
		D+**	
		TEST LO	AD CONFIGURATION
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		New L	1 + 1

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38CONDS . GOBY GREY 46 St. 200 LO St. CO. L. CO. L. C.	38CONDS JOBE 7.48 15.73 202 88 96 87 258 169 220 354 169 ED POR 125 381, 1 125 381, 1 120 86 87 736, 3 120 86 87 207 2040 C	135 354, 120 36 34 36 37 358 169 329 343 135 354, 120 36 36 36 37 334, 9 120 35 354, 120 35 355 355 355 355 355 355 355 355 355	1.20 1.89 13.47	40 10C	Т	+	100	707	1	/	_	15	200	C	0	10	1	2000
SECONDS GOOV GREYN GO SEC. ON CONTRACT OF THE SECONDS GOOV GREYN GOV GOV	3ECONUS . door apen 90 Sec. air coutral tull apen for 3 4 12 4 11 5 air	2	00 5 721 NO	200	100	4	7	1389	5		_	-	10	-	***	500	1	3 020
SECONDS . door apen 90 Sec. air runh, P. I and B.	SECONDS GOOD OPEN 90 SEC. ON CONTRACT THE SOUL Chood HILL SAILS		2000 1000	0.0	X.7	-	229	30 344	440	1	, 6	3	000		150	3/2		-
SECONDS GOOF OPEN 90 Sec. Dir contal Dilang. C. 36 1 1111	SECONDS door apen 90 Sec air contral to [lagen for 3 /2 m/2 then soul, chood till 5 m/2		200							1	7	4	9	7 73%		2	1	2000
SECONDS . door apen 90 Sec. Dir condul and a dir	SECONDS . door apen 90 Sec. air contral Pullagen for 3 3 mil then		390				1	1							100		-	
SECONDS . door apen 90 Sec. Dir routed Plane. D. 7 4	SECONDS . door apen 90 Sec. air contral Pullagen Por 3 /2 m/2 then		400		-												1	1
SECONDS . door apen 90 Sec. air condul ano. D. 36	SECONDS . door open 90 Sec air contral Pullogen for 3 4 min then		410											1				
SECONDS . door apen 90 Sec. Dir condul and a dir seconds	SECONDS . door open 90 Sec. air contral Pullogen for 3 3 mil then							2	-	1								
SECONDS . door apen 90 Sec. Dir roudal Pollano. D. 36	SECONDS . door apen 90 Sec. air contral Pullagen Por 3 /2 mile then		420				-		1									
SECONDS . door apen 90 Sec. Dir condul (2) 1970 . 4	SECONDS . door apen 90 Sec air contral Pallagen Por 3 % mils then		430					A year	0 11 0									
SECONDS . door apen 90 Sec. Dir routed Pollano. D. 26	SECONDS . door open 90 Sec air contral Pullogen for 3 /2 m/s then		410			1	-	/ () /	1661									
SECONDS . door apen 90 sec.	SECONDS . door open 90 Sec air contral Pullogen for 3 /2 mil then		450				>		1611									
SECONDS GOOD OPEN 90 Sec. Dis Conda Minor D. 36 4	SECONDS . door open 90 sec air contral Pullogen for 3 /2 min then		750				7	5									1	
SECONDS . door apen 90 Sec as condulation 0.36 ) 4	SECONDS . door apen 90 Sec air contral Pallagen Por 3 /2 mils then		OD.					1		-								
SECONDS . door apen 90 sec air condul allanou a. A.	SECONDS door open 90 sec air contra/ Pallegen for 3 /2 mil then		470						1									
SECONDS . door apen 90 sec air condul allanon as Is	SECONDS door open 90 sec air contra/ Pallogen for 3 /2 mily then		430				-	3	1									
SECONDS . door apen 90 Sec air conda Manon D. 7 4	SECONDS door open 90 sec air contra/ Pallogen for 3 /2 mil then		MENTS.														-	1
SECONDS door open 90 Sec as rounds Ollange D. 3/2 ) A	seconds door open 90 sec air contral tullopen for 3 4 min then	100						0.40										
Ser 1900 1. 1000 1. 1000 1.	are open to see ast could by lopen for 3 2 my then	Seconds	SECONDS		,		5	111	111	11-0	-							
	100 Maria 100 Ma	aver open 10 300 air control til 10000 sec. 10.	200.00		266		3	the land	1000	100	1	1	1	11-1-1				

		Page 27 of 50
Manufacturer Morso	Model 3600	Date 8/8/0/
Job # J20049092	Run 3	Tech AL/

PRETEST DILUTION TUNNEL TRAVERSE RUN

Barometric pressure (Pbar) 29,04 (inches Hg.) Inside diameter: Port A 6in. Port B 6in.

Static pressure (P<sub>q</sub>) <u>105</u> (inches w.c.) Tunnel cross sectional area: 0.1963Ft

Pitot tube type: Standard

Traverse Point	Position (inches)	Velocity Head $\Delta_p$ (inches H <sub>2</sub> O)	Tunnel Temperature (°F)	$\sqrt{\Delta p}$
A-Centroid	3.00	.059	209	0.2429
B-Centroid	3.00	-060	195	0. 2449
A-1	0.40	.054	202	0.2324
A-2	1.50	.059	206	0.2429
A-3	4.50	-059	205	0-2429
A-4	5.60	.055	204	0.2345
B-1	0.40	.056	196	0.2360
B-2 .	1.50	.060	196	0.2449
B-3	4.50	-060	199	0.2449
B-4	5.60	1054	196	0.2324
		AVERAGE	200.8	0.2399

Adjustment factor application

$$V_{s} = K_{p}C_{p}F_{p}\left(\sqrt{\Delta_{p}}\right)AVG\sqrt{\frac{T_{s}}{P_{s}M_{s}}} \qquad V_{s} = K_{p}C_{p}\left(\sqrt{\Delta_{p}}\right)avg.\sqrt{\frac{T_{s}}{P_{s}M_{s}}}$$

Pitot correction

Cp = Pitot tube coefficient = 0.99 for standard pitot

= manometer reading (inches H2O)

T. = average absolute dilution tunnel temperature (°F + 460)

$$F_p = \frac{\left(\sqrt{\Delta_p}\right) a v g}{\left(\sqrt{\Delta_p}\right) centroid}$$

P. = absolute dilution tunnel gas pressure or Pbar + Pg

P. = static pressure

M. = 28.56, wet molecular weight of stack gas (alternatively, it may be measured) Kp = 85.49 Pitot tube constant, (conversion factor for English units)

Adjustment factor for alternative Pitot tube placement:

= Average of the square roots of the velocity heads ()p) measured at each traverse point.

 $\sqrt{\Delta_p}$  centroid = Average of the square roots of the velocity heads measured at the tunnel centroid (inches of

		Page	30of 50
Manufacturer Morso	Model 3600	Date	8/8/01
Job # J20049092	Run	Tech	32
Pre/Post Checks	н		
Moisture Meter Calibration Check:	ime: 7:50 X: -	Y: - 1:	2: -   22: -
_		TALL I	
Facility Conditions:	P	re-Test	Post-Test
Air Velocity	and the second s	O fpm	O fpm
Smoke Capture Check		~ `	V
Wood Heater Conditions:			
Date Wood Heater Stack Cleaned	8/	14/11	
Date Dilution Tunnel cleaned		4/11	
Induced Draft Check		8	^
- Tunnel Velocity		253	0
		10 2	11/12 2001
Flow Rate 140-cfm ±10%  Pitot Leak Check:	***************************************		147,244
Side A	***************************************	V	L
Side B			
Temperature System:			
Ambient (65°-90°F)			89 F °F
Wood Heater Surface (±125°F)		-	-14/ °F
,			-1110
Proportional Checks:			,
CO Analyzer Drift Check			
CO <sub>2</sub> Analyzer Check	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		
O <sub>2</sub> Analyzer Check			
Thermocouple check			
Sampling Train ID Numbers:		Train 1	Train 2
Probe	The state of the s	5	/
Filter Front		13	19
Filter Back		15	20
Filter Thermocouple.		19	22
Filter 5G-3 (<90°F)		17	24
· · · · · · · · · · · · · · · · · · ·			
Thermocouple Identification Number	5 50	laber to the	- 2
Dilution Tunnel Wet Bulb4 Unit Top		lution Tunnel Dry Bulb	
		uit Bottom	

		Page of
Manufacturer Morso	Model 3600	Date 0/8/07
Job # J20049092	Run	Tech 3

### Pre-Test Scale Audit

Scale Type	Audit Weigh		Measured Weight
Platform	10	lbs., Class F	10, 8 lbs.
Wood	10	lbs., Class F	10.00 lbs.
Analytical	100 Grams	mg, Class S	Grams 100. 0 mg.

#### LIMITS OF WEIGHT RANGES

ANALYTICAL SCALE:	50%-150% of dry filter weight, ± 0.1 mg
PLATFORM SCALE	
WOOD SCALE	

		Page 3 Z of 5
Manufacturer Morso	Model 3600	Date 8/8/6/
Job # J20049092	Run	Tech 3/ /AL

## SAMPLING EQUIPMENT CHECK OUT

#### Leakage Checks Tunnel Samplers

		SYS	ГЕМ 1	SYST	EM 2
Unplugged F	low Rate = .25cfin	Pre-Test	Post-Test	Pre-Test	Post-Test
Vacuum (incl	hes Hg.)	101	10"	10"	104
Final	1 minute DGM (ft <sup>3</sup> )	393.620	414.063	739.379	759,583
Initial	1 minute DGM (ft <sup>3</sup> )	393,620	414,0 63		
Change (C)	(ft³)	0	0	Ö	0
Allowable lea	akage .04 x Sample rate or .02cfm	0.0100	0.0100	0.0100	0.0100
Check OK				~	

#### Leakage Checks Flue Gas Sampler

Plugged Probe	Pre Test	Post Test
Vacuum (inches Hg.)	10 "	10"
Rotometer Reading (mm)	0	0
Flow Rate (CFM)	U	0
Allowable (.04 x Sample Rate)		
Check OK	$\mathcal{L}$	

		Page 33 of J
Manufacturer Morso	Model 3600	Date 8/8/01
Job # J20049092	Run	Tech_AL/

### **CONTINUOUS ANALYZERS**

Pre-Test (Adjust and Record)

	ZI	ERO	SPA	AN	CAL. (Reco	CAL. (Record Only)		
CO	00.00	00.00	9-96	9-96	.95	.999		
CO <sub>2</sub>	00.00	00.00 -	24.65	24.65	9.64	9-99		
O <sub>2</sub>	00.01	00.00	20.92	20.93	10.20	10.2		
	Actual	Should Be	Actual	Should Be	Actual	Should Be		

#### Post Test (Record Only)

	Zero	Span	Cal.	Zero Drift	Span Drift	Cal. Drift	OK?	Not OK*
со	00.00	10.08	-97	Ŏ	,/2	,02	·V	
CO <sub>2</sub>	00.02	25.04	9.78	500	,39	, (3		
O <sub>2</sub>	00.02	20.62	10.16	,02	,30	,04		

<sup>\*</sup> Greater than  $\pm$  5% of the range used.

		Page 3 7 of 3
Manufacturer Morso	Model 3600	Date 8 18/0/
Job # J20049092	Run	Tech_ 2

#### TEST DATA LOG

#### RAW DRY GAS METER READINGS

	System 1	System 2
Final (ft³)	414.044	759,571
Initial (ft <sup>3</sup> )	393,620	739.374

#### AMBIENT CONDITIONS

	Start	End
Barometer. (inches Hg)	29,04	29.03
Wet Bulb (°F)	The Yard	
Dry Bulb (°F)	74	86.2
Humidity (%)	79	61.7

		Pag 35 of So
Manufacturer Morso	Model 3600	Date_8/5/0/
Job # J20049092	Run	Tech_3v(

### DILUTION TUNNEL PARTICULATE SAMPLER DATA FILTER TYPE: Gelman 47mm A/E

	SYS	TEM 1	Time: SYSTEM 2			
	Probe and Front 'S	Filter Numbers /7, /8	Probe and Front Half Housing #	Filter Numbers 19, 20		
Post Test Weight:	91.0576 grams	2415 grams	91. 5665 grams	2286 gram		
Pre Test Weight:	91.0566 grams	.2278 grams	91, 5661 grams	.2155 Gram		
Gain:	,0004 grams	,0137 grams	.0008 grams	.0131 Grams		
	ál	- b1	a2	b2		

To	otal Gain:	al + bl =	14,1m =	rams	= 13.9 m grams				
			SYSTEM 1			SYSTEM 2			
Pre-test Weight Record		Probe & Housing Number	Front Filter Number	Back Filter Number	Probe & Housing Number	Front Filter Number	Back Filter Number	TEMP	нимп
Date	Time	5	17	18	6	19	20	°F	%
8/5/01	9:30	91.0573	.150	.1132	91.5665	,1026	.1142	76	48
8/6/01	6:20	11.0570	-1151	.1130	945661	.1023	1139	76	49
8/7/01	5:55	91.0566	,1149	.1129	91.5661	,1022	.1137	75	48
8/8/01	72/0	91.0566	1149	1129	91.5661	.1020	11/35	74	45
		Total	.2	278	Total	.2/.	5 5		

			SYSTEM 1				
Pre-test Weight Record		Probe & Housing Number	Combined Filter Weight Number	Probe & Housing Number	Combined Filter Weight Number	TEMP	HUMID
Date	Time	5	17,18	6	19,30	°F.	%
8/8/01	11:48	91.2654	.2464	91,6279	,2301	85	49
8/9/01	7:18	91.0581	,2418	91.5672	,2300	73	88
5/10/61	7:30	91.0571	.2417	91,5670	. 2288	72	46
8/13/01	8:20	91.0570	.2415	91,5669	, 2786	75	48

			Page	6 of 50
Manufacturer Morso		Model 3600	Date	8/8/01
Job # J20049092		Run	Tech_ つ	me -
	FUEL DATA	<b>A</b>		
FUEL DESCRIPTION: Kindling weight: 4.4 lbs Pre-test load weight: 15.57 Pre-test moisture content: Uncor	Consisting of: Scrap	X4X// // inches	Fire lit Time 8 Time loaded: Vet: 18,06	
Test Air Control Settings: Test Unit Fan Settings:	Tull open		Time:	40
	TEST LO Lower Limit		0.00	
Test Load Weight:	13,48 Lb	Ideal 14,98	lbs. 16.	per Limit
Fire Box Volume: 2 / 4/ Load Volume: 0 . 49 9 6		Ideal Length Loading Dens Load Density	ity: 7	Inches   13 2   lbs/ft <sup>3</sup>   72   lbs/ft <sup>3</sup>
Piece Size	Weight	Meter Mois	ture Content (% dry)*	
2 x 4 x 19 in.	2.29 lbs.	20.5 %	21-5 %	199 %
2 x 4/x 19 in.	2-43 lbs.	23./ %	22.0 %	18.3 %
2 x 4/x 19 in.	2-38 lbs.	23./ %	20.0 %	18.8 %
4 x 4 x 19 in.	4.46 lbs.	22.2 %	22.0 %	23.1 %
4 x 4/x /9 in.	9-13 lbs.	19.7 %	19.4 %	19.9%
x x in.	Ibs.	%	%	%
X X in.	lbs.	%	%	%
COAL BED RANGE: 3.2 TEST CHARGE: Time loaded:	19 lbs. NT: CORRECTED TO TWO	(20% to 25% of test load)  Coal bed weight = $\frac{2}{\sqrt{2}}$	(WET) /8.	

COMMENTS				1_3	Tech_ 7	
	FKD	2 × Y )	× 10	6.52 185	AT 913	YAI
	ler	irst mers	TURE	6.52 1BS	OF 20-	3
					~	
				4		
				TEST LOAD	CONFIGURATIO	N
						1
			re			

ob#	J200490	092						F	Run	3_		T	ech_ ?	rk	<u>  8/8</u>   8/8 (	
				Air	Con	ful	fa	11	ppe	1						
SWI	TCHN	JMBER		1	2	3	4	5	T 6	7	8	9	10			
READING #	REAL TIME	ELAPSED TIME	WEIGHT	FLUE GAS TEMP	ROOM TEMP	TUNNEL DRY BULB	TUNNEL WET BULB	UNIT TOP	UNIT BACK	UNIT RIGHT SIDE	UNIT LEFT SIDE	UNIT BOTTOM	CATALYST DOWNSTREAM	TUNNEL	DRAFT	SMOKE
0	RE	0	17,70	162	73	208	69	172	73	76	78	74	694		1880	17
1		10	1420	743	75	202	71	316	8.5	113	125	95	1293		101	+
2		20	10276	836	77	235	74	517	1/12	155	201	133	13/7		10%	1
3	1	30	7.60	843	80	229	26	651	125	255	296	194	1320		1106	0
4		40	5,10	795	84	205	75	7/2	147.	301	376	286	1129		1/11	C
5		50	820	788	26	2019	80	659	167	360	411	427	1204		1/1/	0
6		60	6,40	735	88	202	82	665	182	384	423	486	1/62		099	0
7	UI	70	4.30	180	88	188	28	642	192	397	440	730	1099		196	-
8		80								1	171	20	100	DI TI	3 (6)	_
9	304	90												7		
10		100											1.1—1	14 1		
11		110	1 -1							- 1					J. T. C	
12		120														
13		130												1	GI	
14		140													-	
15	-;-	150										1771				
16		160														10.1
17		170														
18		180	-				2 = 4		36							
19		190		12 7 11				<b>-</b>							71	
20		200														
21		210		-47				V II								
22		220		- 11	1 179			E:71							1	
23		230					==:1									
24		240							1							V
25		250								[F=1]						
Com	ments:		En	63	5	0	F	RET	EST	AT	9:39	A. M	2	xxx	10	

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Manufacturer Morso	Model 3600	Date 8.9.01
Job # J20049092	Run	Tech_ 3

PRETEST DILUTION TUNNEL TRAVERSE RUN

Barometric pressure (P<sub>bar</sub>) 29,00 (inches Hg.)
Inside diameter: Port A 6in. Port B 6in.

Static pressure (P<sub>q</sub>) / (inches w.c.)
Tunnel cross sectional area: 0.1963Ft

Pitot tube type: Standard

Traverse Point	Position (inches)	Velocity Head $\Delta_p$ (inches $H_2O$ )	Tunnel Temperature (°F)	$\sqrt{\Delta p}$
A-Centroid	3.00	.040	121	,2000
B-Centroid	3.00	1040	123	2.000
A-1	0.40	,036	123	11897
A-2	1.50	-080	1211	.2000
A-3	4.50	-041)	721.	,2000
A-4	5.60	_035	123	1/891
B-1	0.40	800,	121	1949
B-2	1.50	,040	122	.2000
B-3	4.50	-046	123	12000
B-4	5.60	,035	126	1.1871
4.60		AVERAGE	1268	19.59

Adjustment factor application

$$V_s = K_p C_p F_p \left( \sqrt{\Delta_p} \right) A V G \sqrt{\frac{T_s}{P_s M_s}}$$

$$\frac{T_s}{P_s M_s} \qquad V_s = K_p C_p \left( \sqrt{\Delta_p} \right) avg. \sqrt{\frac{T_s}{P_s M_s}}$$

Pitot correction 9794

Where,

Cp = Pitot tube coefficient = 0.99 for standard pitot

 $\Delta_p = \text{manometer reading (inches H}_2\text{O})$ 

T, = average absolute dilution tunnel temperature (°F + 460)

$$F_p = \frac{\left(\sqrt{\Delta_p}\right) avg}{\left(\sqrt{\Delta_p}\right) centroid}$$

P<sub>s</sub> = absolute dilution tunnel gas pressure or inchesH<sub>1</sub>O

Pbar + Pg

Ps = static pressure

 $M_s$  = 28.56, wet molecular weight of stack gas (alternatively, it may be measured)  $K_\rho$  = 85.49 Pitot tube constant, (conversion factor for English units)

Adjustment factor for alternative Pitot tube placement:

 $(\sqrt{\Delta_p})avg$ . = Average of the square roots of the velocity heads  $()_p$ ) measured at each traverse point.

 $(\sqrt{\Delta_p})$  centroid = Average of the square roots of the velocity heads measured at the tunnel centroid (inches of  $H_2O$ )

Manufacturer_ Morso	Model 3	600		Page 9/ of J		
Job # J20049092	Run_	4	Tec	h 22		
Pre/Post Checks	(m)	Tu Le	T.		T <sub>2</sub>	
Moisture Meter Calibration Check:	Time:	X: U	Y: -	12: ~	22:	
<b>3</b>		Pre	-Test	Post	t-Test	
Facility Conditions:			-21	1	AV.	
Air Velocity			G fpm		() fpm	
Smoke Capture Check				2		
Wood Heater Conditions: Date Wood Heater Stack Cleaned		8/	1/01			
Date Dilution Tunnel cleaned	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	0/4	401			
Induced Draft Check		1	9	1	2	
Tunnel Velocity		.09	10	05	-040	
Flow Rate 140-cfm ±10%  Pitot Leak Check:				136		
Side A		4	/	1 1		
Side B			/			
Temperature System: Ambient (65°- 90°F) Wood Heater Surface (±125°F)				-18		
Proportional Checks:						
CO Analyzer Drift Check				-		
CO <sub>2</sub> Analyzer Check				-		
O <sub>2</sub> Analyzer Check						
Thermocouple check					_	
Sampling Train ID Numbers:		Tra	in 1	Tra	nin 2	
Probe			7		2	
Filter Front		2	1	33		
Filter Back			2	24	1	
Filter Thermocouple.		1		-	22	
Filter 5G-3 (<90°F)						
Thermocouple Identification Number	Room2	Diluti	on Tunnel Dev F	Bulb	.3	
Dilution Tunnel Wet Bulb4	Jnit Top5 Jnit Left Side8	Unit E	lack		6	

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Manufacturer_Morso	Model 3600	Date 8-9-01
Job # J20049092	Run_ 4	Tech

### Pre-Test Scale Audit

Scale Type	Audit	Audit Weight		Measured Weight		
Platform	10.	O lbs., Class F	10,0	lbs.		
Wood	10.	lbs., Class F	10.00	lbs.		
Analytical	100 Grams	mg, Class S	Grams /000	mg.		

#### LIMITS OF WEIGHT RANGES

ANALYTICAL SCALE:	50%-150% of dry filter weight, ± 0.1 mg
PLATFORM SCALE	
WOOD SCALE	

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Manufacturer Morso	Model 3600	Date 8-9-0/
Job # J20049092	Run_	Tech 3

# SAMPLING EQUIPMENT CHECK OUT

#### Leakage Checks Tunnel Samplers

		SYS	ГЕМ 1	SYST	EM 2		
Unplugged Fl	ow Rate = .25cfm	Pre-Test	Post-Test	Pre-Test	Post-Test		
Vacuum (inch	nes Hg.)	10"	101	1011	104		
Final	1 minute DGM (ft <sup>3</sup> )	414,366	460,608	259,708	805,918		
Initial	1minute DGM (ft <sup>3</sup> )	414,365	460.608	759.706	805.911		
Change (C)	(ft³)	1001	0	,002	-003		
Allowable lead	kage .04 x Sample rate or .02cfm	0.0100	0.0100	0.0100	0.0100		
Check OK							

#### Leakage Checks Flue Gas Sampler

Plugged Probe	Pre Test	Post Test
Vacuum (inches Hg.)	10"	10"
Rotometer Reading (mm)	O	0
Flow Rate (CFM)	O	d
Allowable (.04 x Sample Rate)		
Check OK		1/

		Page 44 of JO
Manufacturer_Morso	Model 3600	Date 8-9-0/
Job # J20049092	Run_ 4	Tech AL/

### **CONTINUOUS ANALYZERS**

Pre-Test (Adjust and Record)

	ZERO		ZERO SPAN			CAL-(Record Only)		
со	00.00	00.00	9.96	9.96	-96	.999		
CO <sub>2</sub>	00.00	00.00	24.65	24.65	9.61	9.99		
O <sub>2</sub>	00.01	00.00	20.93	20.93	10.23	10.2		
	Actual	Should Be	Actual	Should Be	Actual	Should Be		

#### Post Test (Record Only)

	Zero	Span	Cal.	Zero Drift	Span Drift	Cal. Drift	OK?	Not OK*
со	.02	10,04	,96	.02	80,	0	V	
CO <sub>2</sub>	,05	24.95	9.75	.05	130	. 24	V	
O <sub>2</sub>	.08	20.61	10.26	.08	-32	103	~	

<sup>\*</sup> Greater than ± 5% of the range used.

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Manufacturer Morso	Model 3600	Date 8 9-07
Job # J20049092	Run	Tech_ 3/L

#### TEST DATA LOG

#### RAW DRY GAS METER READINGS

	System 1	System 2
Final (ft <sup>3</sup> )	460,600	805.982
Initial (ft³)	414 366	759.708

#### AMBIENT CONDITIONS

	Start	End	
Barometer. (inches Hg)	29.00	28.96	
Wet Bulb (°F)			
Dry Bulb (°F)	73	7074	WA
Humidity (%)	63	70	

							Page	:46 of	50	
anufactur	er Morso			1	Model 3600		Dat	te 8	17/01	
ъ# J2004	9092				Run 4	_	Tech	n	1	
			N TUNNEL FILT s in Desecrator.	PARTICU: TER TYPE: Gelman 4 Date:	7mm A/E	PLER DATA	N September 1			
				ГЕМ 1	074767	inic.	SYST	EM 2		
		Probe and Half Hous		Filter Numbers	2122	Probe and Fro Half Housing			ilter umbers 23	3 20
	est Weight:		grame	.258	grams	92. 185	grame	2	450	grams
Pre Te	st Weight:	90,94	72 grams	.2296	grams	92, 1860	grams	,2	167	Grams
(	Jain:	.00	arama	.0285	grams	TA1	grams	.0:	0 2	Grams
			al		ol	a2		10-	b2	-
T	otal Gain:	al + bl =	30.0 mg	rams	a2 + b	2=29.7m SYSTEM 2	grams			
. W	e-test eight ecord	Probe & Housing Number	Front Filter Number	Back Filter Number	Probe & Housing Number	Front Filter Number	Back Filter Numbe		TEMP	HUMII
Date	Time	7	21	21	P	20	24		°F	%
8/7/01	6:00	90,9485	.1139	.1162	92.1867	.1026	11.4:	3	75	88
5/8/01	7:15	909479	,1136	TT 76 32 5	92.1867	11024	,114	4	74	45
8/9/01	7:20	96.9477	.1136		92.1866	.1024	114	3	73	48
	8 1				2	1				
		Total	,23	96	Total	,2	167			
			SYSTEM 1	*		SYSTEM 2				
W	e-test eight cord	Probe & Housing Number	Comb Filter V Nun	Weight	Probe & Housing Number	Filter	nbined Weight mber		TEMP	HUMID
Date	Time	7	21	25	8	23	24		°F	%
8/9/01	1410	90,9507	.26	11	92/898	.24	85		85	49
8/19/01	7:15	90, 9993	,258	12	92,1881	24	51		72	46
8/13/01	8:25	90.9492	,258	y	92.180	24	50		75	48
Qlulat	,240	20 6000	>50	1	12 1500	200	-1		5-	110

		Page 4	70 50
	Model 3600	Date	70f 50 8-9-01
	Run_ 4	Tech_	all
FUEL DATA			
PRE-	TEST LOAD		
os. Consisting of: Scrap a	and paper X4X <u>/0, /G</u> inches	Fire lit Time Time loaded: 1: /7, 46 %	9:02
1 % from 1'p	W	Time; _ 9	433
TEST LO	AD	Inne	
Lower Limit	Ideal	Up	per Limit
/3.48 Lbs.	14.98	lbs.	16.48 Lbs.
0,4946 Ft.3	Loading Density		9 Inches 294 Ibs/ft <sup>3</sup>
		2/-	578 lbs/ft <sup>3</sup>
		re Content (% dry)*	
		18.8 %	19-2 %
			18.2 %
			19.5 %
			19.6 %
			19.8 %
lbs.			%
/lbs. ENT: CORRECTED TO TWO	PIN: (DRY) 20.5/%	^	g.
	PRE- DS. Consisting of: Scrap a  A lbs. Consisting of: 22  Directed: 1% P Corrected  TEST LO  Lower Limit  13. 48 Lbs.  2-14 Ft.  0, 49 46 Ft.  76 34x1½x5  Weight  2. 57 lbs.  2. 49 lbs.  2. 49 lbs.  3. 98 lbs.  3. 72 lbs.  lbs.  lbs.  lbs.  Dis.  Dis.	FUEL DATA  PRE-TEST LOAD  OS. Consisting of: Scrap and paper  Loss Consisting of: 2X4X/0 / G inches prected: 19.79 % Corrected Dry: 21.6 % We  TEST LOAD  Lower Limit Ideal  13.78 Lbs. / 19.88  2.14 Ft.3 Loading Density  Load Density:  Weight Meter Moistur  2.57 lbs. / 19.0 %  2.49 lbs. / 19.0 %  2.99 lbs. / 19.0 %  3.98 lbs. / 19.9 %  3.72 lbs. / 19.9 %  3.72 lbs. / 19.9 %  lbs. / 19.9 %  10.23.1%  PRYWEIGHT:  DRYWEIGHT:  DRYWEIGHT:	FUEL DATA  PRE-TEST LOAD  S. Consisting of: Scrap and paper   Size of time loaded: Time loaded: Time loaded: 1/2/2/3/4/6/6/6   Time: 1/2/4/6/6/6   Time: 1/2/4/6/6/6/6   Time: 1/2/4/6/6/6/6   Time: 1/2/4/6/6/6/6   Time: 1/2/4/6/6/6/6   Time: 1/2/4/6/6/6/6   Time: 1/2/4/6/6/6/6/6/6/6/6/6/6/6/6/6/6/6/6/6/6

Manufacturer Morso	Model 3600	Page 48 of 50  Date 8 - 9~u/
Job # J20049092	Run	Tech Rec
9:10 Parke 9:31 Restot	of preload added ( preload added	(6.0 (bs)
74		
	TEST LOA	D CONFIGURATION
	rea-	

Manufacturer Morso Model 3600 Job # J20049092 SWITCH NUMBER UNIT LEFT SIDE CATALYST
DOWNSTREAM ELAPSED TIME TUNNEL DRY BULB UNIT BOTTOM WEIGHT READING # REAL TIME .089 10101 Fines Ahmed 1550C Comments: 10:46 Fire attracted door open Imin

THE STATE OF THE S		LAPSED 0 S	-				m	7		7 8	8 9	- Mess	High	DATE	de	10/61		RUN#: 4	1		TECHNICIAN:	AN: SE	1
	10   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150   150	97 0	CO WEIGHT REMAIN,	co <sub>i</sub>	O <sub>2</sub>	EODM TEMP	TURNEL TEMP	TUNIT TOP TUNNEL WET HULE	BACK.	UNITHT.	INIT	CAT	2	GAS SM ROTO	DGM #1	ROTO I	≥ (DGM T)	READI	ROTO	C DGM 7	FILTE		f PRES.
			1. 1	5.00	96		6		178	- 4	327	69		PL V	010	1	EMT .	NG	- 1	ET .	_		8.
			3.50 1.26	5.78	3	0			127		024	398	-	13	57				100	~	_		
	10   10   10   10   10   10   10   10	10	000	08301	37				(733		437	129			0	70 00		_	- 1		300		
19   19   19   19   19   19   19   19	13 (1978) 9-14 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (1978) 13 (		-	12,19	100		1		173		25	250		-		29		_			00	_	25
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# APPENDIX B

#### INTRODUCTION

This document provides a step by step guide for the technician conducting tests to EPA standard requirements. Procedures outlined here, when followed, will result in tests in conformance with EPA Methods 28 and 5G-3. This guide cannot cover every possible contingency that may develop during a particular test program. Many questions that may arise can be answered by a complete understanding of the test standards and their intent. When in doubt on any detail check with the laboratory manager and be sure you understand the procedures involved.

The primary measurements to be obtained are particulate emission data and efficiency data. The technician's duties include the following steps. It is critical that all spaces on the data forms be properly filled in. Each test must be represented by a complete record of what was done and when.

- I. APPLIANCE INSPECTION AND SET-UP
  - A. Incoming Inspection
  - B. Unit Set-Up
- II. SAMPLING SYSTEMS SET-UP
  - A. Gas Analysis
  - B. Dilution Tunnel
- III. TEST CONDUCT
  - A. Pre-Test Fuel Load
  - B. Test Fuel Load
  - C. Unit Start up
  - D. Test Run
- IV. POST TEST PROCEDURE
  - A. Leak Checks
  - B. Particulate Sample Recovery

The technician running this test must be familiar with the following EPA documents that are to be kept in the laboratory at all times.

- Method 28
- Method 28A
- Method 5G-3
- Method 5H

#### I. APPLIANCE INSPECTION AND SET-UP

#### A. Incoming Inspection

- Check for completeness of unit including parts, accessories, installation and operating instructions, drawings and specifications, etc. Note any discrepancies or missing parts.
- Check for shipping damage. If damage has occurred, notify the laboratory manager. In some cases repairs may be made, provided the manufacturer and laboratory manager concur that repairs will not affect the units performance. If damage is irreparable, a new unit will need to be obtained.
- 3. Note whether unit is catalytic or non-catalytic.
- Mark unit with manufacturer's name, model number, work order number and date received.
- If unit is safety listed, note label data including listing agency and serial number.

#### B. Unit Set-Up

- All units must be operated in-house for a break-in period as follows (the unit may be connected to a lab chimney). NOTE: Inserts are tested as if they are freestanding stoves.
  - a. Non-catalytic units: 10 hours minimum burn time with a stack temperature of at least 250<sup>0</sup> Fahrenheit (medium burn rate, Douglas Fir scrap or cordwood.) A stack thermocouple must be installed and stack temperature recorded at 1-hour intervals or on chart recorder.
  - b. Catalytic units: 50 hours minimum burn time with catalyst temperature in excess of 800<sup>0</sup> Fahrenheit (medium burn rate, Douglas Fir scraps or cordwood). Record catalyst temperature at 1-hour intervals or on chart recorder.
- 2. Once break-in is completed, allow unit to cool then clean unit thoroughly.
- 3. Thermocouples must be attached to surfaces of unit prior to testing. EPA requires a thermocouple on the outside bottom of the firebox. This must be installed prior to putting the unit on the scale. In some cases the required thermocouple locations will be inaccessible on finished units. Check with the laboratory manager if problems are encountered in proper thermocouple attachment.
- Prior to placing unit on scale, the scale must be turned on and allowed to warm up for 1-hour minimum.
- Place unit on scale and align so chimney will be centered in hood. Record the weight of the unit and all accessories. (Do not weight with chimney attached.)

- 6. Chimney and connector should be cleaned with a wire brush prior to mounting. Attach chimney and connector then seal all joints. Be sure single wall stove pipe terminates and insulated pipe starts at proper level above scale platform. Chimney must be supported from scale so that it does not touch test enclosure or hood walls.
- Measure firebox dimensions and record on appropriate data form. Make a
  three dimensional sketch of the firebox including firebrick, baffles, and
  obstructions. Calculate firebox volume in cubic feet. See Section 6.2.4 of
  EPA Method 28 for details.
- 8. If unit is equipped with a catalyst additional thermocouples must be installed downstream of, and inside catalyst (upstream optional).
- 9. Plug thermocouples into data acquisition system jacks and verify that all instrumentation is working properly.
- 10. Dilution tunnel must be cleaned prior to each certification test series, and at anytime a higher burn rate follows a lower burn rate.

#### II. SAMPLING SYSTEMS SET-UP

#### A. Gas Analysis

- All instruments should be turned on and allowed to warm up for 1-hour minimum.
- Prior to calibrating, make sure that the outlet pressure on each calibration gas bottle reads 10 PSI. Adjust flow meters at each gas analyzer to required flow.

All gas analyzers (CO<sub>2</sub>, CO, O<sub>2</sub>) are zeroed on nitrogen. The O<sub>2</sub> analyzer is spanned on air and set for 20.93%. CO<sub>2</sub> and CO analyzers are spanned with their respective gases.

#### Calibrate analyzers as follows:

- With calibration switch at "SPAN", adjust all span controls to values specified on span gas label.
- Switch to "ZERO" and adjust zero controls to provide 0.00 readout on all analyzers.
- c. Repeat a. and b. until no further adjustment is required.
- d. Record these values on the appropriate data sheet.
- e. Switch to "CAL." and record all analyzer values.

#### Response time synchronization check.

- a. With switch at "SAMPLE" and no fire in unit, allow readings to stabilize (O<sub>2</sub> analyzer should read 20.93, CO and CO<sub>2</sub> should read 0.00).
- b. Switch to "CAL" setting and start the stopwatch. Note the time required for each unit to reach the calibration gas bottle value. If all three analyzers reach this value within 5 seconds of each other, synchronization is adequate. If not, contact the laboratory manager. Synchronization is adjusted by either internal instrument setting or adjustment of sample line length.
- Use EPA Method 5H 6.7-6.9 procedures to check calibration of instruments.

#### 4. Sample clean-up train.

- a. Load a new filter in 4-inch glass filter holder.
- b. Load four Impingers as follows:
  - #1: 100 ml. distilled water and 5 ml. H<sub>2</sub>SO<sub>4</sub>
  - #2: 100 ml. distilled water and 5 ml. H<sub>2</sub>SO<sub>4</sub>
  - #3: Empty
  - #4: 200-300 grams Drierite.
- Place Impingers in container and connect with greased "U TUBES".
   (Grease carefully on bottom half of ball joint so that grease will not get into tubes.)
- d. Connect filter to impinger #1 and sample line to impinger #4.
- e. Connect stack probe to filter.
- f. Leak check system as follows:
  - 1) Plug probe.
  - Turn on sample system and increase flow rate slowly.
  - 3) Set vacuum adjust valve to obtain a vacuum of 10 inches mercury.
  - If sapphire float in rotometer does not stabilize below 10 on scale, system must be resealed.
  - 5) Repeat leak check procedure until satisfactory results are obtained.
  - Unplug probe slowly, then decrease flow rate slowly before shutting off system.
- g. Just prior to starting test, fill impinger container with ice.

#### B. Dilution Tunnel Sample Train Set-Up:

#### 1. Filters and holders.

- Clean probes and filter holder front housings carefully and desiccate to a constant weight prior to use.
- Filters and filter probe combinations should be numbered and labeled prior to use.
- c. Weigh desiccated filters and probe filter units on analytical balance. Record weights on appropriate form. Note that probe and front half of front filter holder is to be weighed as a unit.
- d. Carefully assemble filter holder units and connect to sampling systems.
- e. Check Silica gel columns for adequate dry absorbent (blue color).

#### Leak checking.

- Each sample system is to be checked for leakage prior to inserting probes in tunnel.
- b. Plug probes and start samplers. Adjust pump bypass valve to produce a vacuum reading of 10 inches mercury. NOTE: During test, highest vacuum recorded is required for posttest leak check.
- c. Allow vacuum indication to stabilize at 10" mercury, record dry gas meter readings, (DGM<sub>1</sub>, DGM<sub>2</sub>). At a convenient DGM value start stopwatch. Time for 1 minute then stop vacuum pumps. Record dry gas meter readings again, (DGM<sub>3</sub>, DGM<sub>4</sub>). NOTE: If rotometer ball is floating above the 5-mm mark, system is leaking too much and all seals should be checked.
- d. Calculate leakage rate as follows.

System 1:  $DGM_3-DGM_1 = CFM_1$ System 2:  $DGM_4-DGM_2 = CFM_2$ 

If CFM<sub>1</sub> or CFM<sub>2</sub> is greater than 0.02 cfm, or  $_1$ S greater than 0.04 x Sample Rate, leakage is unacceptable and system must be resealed. For most tests the sample rate will be 0.25 cfm, thus leakage rates in excess of 0.04 x 0.25 = 0.010 cfm are not acceptable.

e. To prevent contamination, do not insert probes in tunnel until the start of the test run.

#### III. TEST CONDUCT

#### A. Pre-Test Fuel Load

 Using 2x4 Douglas Fir cut enough pieces to approximate test load weight. (Piece length must be greater than 1/3 of the test load length.)

Measure percent moisture content using Delmhorst moisture meter. The average percent moisture must be within 19 to 25 percent.

#### B. Test Fuel Load

1. Determine optimum load weight by multiplying firebox volume (cubic feet) by 7. This is the ideal load weight.

2. Determine piece size mix i.e. <1.5 cubic feet volume use 2x4's only; 1.5 ft<sup>3</sup> to 3.0 ft<sup>3</sup> use a mix of 2.4's and 4x4's; >3.0 ft<sub>3</sub> use only 4x4's. Ideal length is 5/6 of the longest firebox dimension.

 Weigh out test load and appropriate number of spacers and adjust weight by shortening or lengthening all pieces equally if necessary.

4. Construct test loads by attaching spacers as shown in EPA Method 28.

5. Measure and record moisture content of each fuel piece (use three sides). Determine if fuel load moisture content is within required range (19-25%). If not, construct new fuel pieces using wood with required moisture content. All wood in the humidity chamber is Douglas Fir and should be within range. Contact laboratory manager if you cannot find suitable pieces.

#### C. Unit Start-Up

- With all doors and air controls closed, zero draft Magnehelic using screw located at bottom of meter.
- Before lighting a fire, turn on dilution tunnel and set flow rate to 140 scfm (approximately 715 fpm) if burn rate is to be less than 3 kg/hr. For higher burn rates set flow for a 150:1 air fuel ratio (see chart for approximate values).
- Check draft imposed on cold stove. All inlets must be closed and a draft gauge in the chimney. If draft is greater than 0.005 inches water column, adjust tunnel to stack gap until draft is less than 0.005 inches water column.
- 4. With hot wire anemometer check for ambient airflow around unit (must be less than 50 ft/min).
- 5. Zero scale and start fire with newspaper and Douglas Fir kindling. (Make sure stack sample probe is on the unit.)

- Once kindling is burning well, add preload fuel. Operate at high fire for sufficient time to get fuel load burning well. Then adjust settings to intended test run levels.
- Perform the dilution tunnel traverse as prescribed in Method 28, Section 6.3.
   (Pitot tube should be carefully cleaned prior to each test.)
- 8. Pretest load must burn for a minimum of 1 hour. Record stove surface, catalyst, room and flue temperatures.
- Stir fire often during preburn (after a reading) to get a good coal bed. Fire
  can only be raked once (door open 1 minute or less) during the 15 minutes
  prior to the start of the test.

#### D. Test Run

- 1. Stack gas analyzers should be on and in the sample mode.
- 2. When the fuel bed is between 20-25% of the test load weight the test is to be started.
  - a. Insert the sample probes into the tunnel being careful not to hit sides of tunnel with probe tip.
  - b. Check tunnel Pitot tube for proper position.
  - c. Record initial readings.
  - d. Turn on probe sample systems and start timing test.
  - e. Tare platform scale.
  - f. Open stove doors and load stove. Close door or follow manufacturer's start-up procedures. Five minutes is the maximum time before all doors and controls must be set to final positions for duration of test.
  - g. Record length of time door and bypass are open, include any air control setting adjustments.
  - h. Every 10 minutes record the following:
    - 1) Dry gas meter readings.
    - 2) Weight remaining.
    - 3) All thermocouple temperatures.
    - 4) Tunnel Pitot tube reading.
    - 5) Draft reading.
    - 6) Rotometer readings.
  - Filter temperatures shall not exceed 901F anytime during the test. If approaching 901F turn on cooling pump. Filters must be kept above the dilution tunnel wet bulb temperature in order to prevent condensation.
  - j. Regularly check impinger for ice level during test.
  - k. After 30 seconds of 0.00 lbs. weight, and on the minute, shut off sample trains and record last reading.
  - Record final dry gas meter values.

#### IV. POST TEST PROCEDURES

#### A. Leak Checks

#### 1. Dilution Tunnel

- a. Remove both sample probes from tunnel and plug with rubber stopper.
- b. Turn on sample system and set vacuum to 10" mercury or to the highest value reached during the test.
- c. At a convenient value start stop watch. Record DGM starting value.
- d. After 1 minute stop sample system and record ending DGM value.
- e. Calculate leakage rate per pre-test description (see II.B.2.c.).

#### Gas Analyzers

- a. Set stack sample flow to about 75 mm on the rotometer.
- b. Plug with rubber stopper.
- c. Adjust vacuum to 10" mercury.
- d. Let system stabilize then record rotometer readings.
- e. If rotometer readings do not equal zero check with laboratory manager.
- f. SLOWLY unplug probe and decrease flow rate to zero.
- g. Turn off stack sampling system.
- Zero, span and calibrate the analyzers (see Gas Analysis). RECORD ONLY these meter values.

#### B. Particulate Sample Recovery

- Disassemble filter holder and scrape gasket with scalpel. Collect all loose material on filters.
- Weigh and record probes and filters for each train. NOTE: 24 hours of desiccation must pass before final "no change" weight values can be recorded.
- Weigh and record probes and fillers at 2-hour intervals until weight change between weighing is less than 0.5 mg.

#### V. DISPOSITION OF TESTED UNIT.

In order to meet the requirements of section 60.535(g) of the EPA's 40CFR Part 60 Standards of Performance for New Stationary Sources; New Residential Wood Heaters, Intertek Testing Services seals certified wood heaters by strapping the unit to a pallet and covering the unit with stretch wrap. A copy of the EPA certificate is attached and our WHI logo stamped on the stretch wrap in various positions and then another layer of stretch wrap is used to cover the markings and copy of the certificate. Any breaking of the stretch wrap seal will be easily noticeable. The unit is then shipped back to the manufacturer.

# APPENDIX C

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210	290.3	89	90	636.5	88	88	97	19.86	20.12
220	292.7	89	89	638.9	88	89	97	19.88	20.10
230	295.1	88	89	641.3	88	88	97	19.90	20.12
240	297.5	88	88	643.7	88	88	97	19.92	20.12
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260	302.3	89	89	648.5	88	88	97	19.88	20.12
270	304.7	88	89	650.9	88	88	96	19.90	20.12

lessor f Solites in Louis	Proportio	nal Rate Cal	culations	100 f (1116) (200 a 2 444) ( + 262 a +	(EPA Formulas	s from PR5	G)	- 1000 - 1000 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 - 1400 -
T distribution (see	Stack are	a (ft2)	0.1963	oren e presión antico della escapa.	Manufacturer:	elasticat classical disputer with	Massa	
Wood	moisture (		17.36	***************************************	Model:	States de mante parce una	Morso	us range a anna a
esemble a marrie & without	Veight (lbs	APPROXIT PROPERTY AND APPROXICAL PROPERTY AND	14.87	Statement (see a mile)	Date:		3600	omos ésara san
ness of Assessed Printedly	ate (Dry k	erreig it errore it haven a destent at	1.239		Run:	unte e la indica partir de Sance	8/6/01	· · · · · · · · · · · · · · · · · · ·
		9/111/:	1.200	latinia a sabela slavetia — esceja iczywa	Kull	Plate chair makes	11	* 14 M ***** * 1 ****** * 4
Final Ter	nperature	(DGM #1) D	egrees Ranki	n:	546.429	Erfely samete more as		to the property and the control of
Final Ter	nperature	(DGM #2) D	egrees Ranki	n:	545.000	ent corer x arm a apaŭ	1 - 0 × - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 -	
			grees Rankin:		566.500		- Tropic Street House & Anna	
		city (feet per		(104)	13.6957793	Carrier & Company of Service & As-		eta erandeko ilabariaka
Sta	indardized	Tunnel Flov	v (dscfm):	er germe e anne genoù kionn k	141.284923	THE STREET COMMON COMMON		. 1001 ( 10054) 40
***** : ***** : *****		Average	Average		\$	encesmojesnos y pare		innerane, can
of Harris Alabasa e sa		Inlet +	Inlet +	Caperon emotion of apparatus of facts of a capero	ţ		<u> </u>	nermore squar
	1	Outlet	Outlet			#1	#2	ere Scheinerscheinen e
multiple summing passes	Tunnel	Temp.	Temp.	ter to travel a desiral e levere a session e	j j.	dDGM	dDGM	*********
Tunnel	Velocity	Meter 1	Meter 2	oreanes concessors and annual	2 4 5 mm 5 mm 7 mm 5 mm 6 mm \$1.	Vol.Std.	Vol.Std.	1010 3 1443 1 )44
Velocity	Ft/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.040	13.703	538.5	536.0	41. V C	Secretaria de la composição de la compos	*******		*********
0.040	13.942	538.5	536.5	103.84	99.78	2.351	2.285	0 10
0.039	13.755	539.5	538.0	104.88	105.07	2.347	2.377	20
0.040	13.942	540.5	538.5	99.14	103.74	2.245	2.375	30
0.040	13.954	541.5	540.0	103.35	103.54	2.338	2.369	40
0.040	13.918	542.5	541.0	102.90	98.79	2.334	2.266	50
0.040	13.847	543.5	542.0	102.18	102.36	2.329	2.360	60
0.040	13.775	544.5	543.0	101.46	101.64	2.325	2.355	70
0.040	13.727	545.5	544.5	96.72	96.80	2.224	2.251	80
0.040	13.703	546.0	544.0	100.65	100.93	2.319	2.351	90
0.041	13.849	547.0	545.5	99.06	99.24	2.314	2.345	100
0.040	13.667	548.0	546.0	100.02	100.29	2.310	2.343	110
0.040	13.630	548.0	546.5	99.76	99.93	2.310	2.340	120
0.040	13.618	548.0	546.5	99.67	99.84	2.310	2.340	130
0.040	13.618	549.0	547.5	99.49	99.66	2.306	2.336	140
0.040	13.594	549.5	547.5	99.22	99.48	2.304	2.336	150
0.039	13.423	550.0	548.0	100.39	100.66	2.302	2.334	160
0.040	13.594	550.0	548.0	99.13	99.39	2.302	2.334	170
0.040	13.582	549.5	548.0	99.13	99.30	2.304	2.334	180
0.040	13.582	549.5	548.5	99.13	99.21	2.304	2.332	190
0.041	er a Witnesse a deserte a passion	549.5	548.0	97.91	98.08	2.304	2.334	200
0.040	THE MY AND WALLAND	549.5	548.0	99.04	99.21	2.304	2.334	210
0.040	13.569	549.0	548.5	99.13	99.12	2.306	2.332	220
0.041	13.738	548.5	548.0	98.00	98.00	2.308	2.334	230
0.040	13.569	548.0	548.0	99.31	99.21	2.310	2.334	240
0.041	13,738	549.0	548.0	97.91	98.00	2.306	2.334	250
0.040	13.569	549.0	548.0	99.13	99.21	2.306	2.334	260
0.040	13.557	548.5	548.0	99.13	99.13	2.308	2.334	270

	uria communa 2 gi		Model:	i i	3600	**********	Georgia de Source de	Transfer a comme	
minion i s mini	nia oramini d	eristanden i e Pagadai	Date:	ļ	8/8/01	*** ******** * * *			
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	an succession is a	Project Test Dur			J20049092		[	• ::::::::::::::::::::::::::::::::::	Ammod crissians
		as Volum		41.	370	A A Are flidentenselje in e leks V		range, caramage,	stommer to browner
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OPPORT A A COMPANIO	Average				29.27	nicement (com	ionis i summi	- armonar i e armone	Company of the second
nemen a commo			ular Weig		28.56	- COMMON A KAN			+ a - to General a succession of
	to an ormanic ray		Correction		0.9794			c foremery a simumosi 2	Cirinocci a amangan
01/10/20 11/00/	Calibratio	n Factor	(DGM #1	):	1.0206			Llamarz ex Yamires	e nomenca a manona)
	Calibratio	n Factor	(DGM #2	):	1.0311				A MANAGEMENT OF A THEOREMS OF
	44 6 4 komantzo (h. k.			(1) VS:	0.0164913	** D*********			
i Junea emeren		mbrose + 5 kmm	o e a mentrena i con	(2) VS:	0.016333			Filter	Filter
		nestina e a sumad			* * ********			Face	Face
Elapsed		Commercial	A R C S LOCATED S S S S	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity
Time	Reading	Inlet T	Outlet T	Reading	Inlet T	Outlet T	Dry Bulb	DGM 1	DGM 2
0	305.0	79	79	650.9	77	77	- 106		
10	307.4	81	79	653.3	79	78	125	20.19	20.45
20	309.8	82	80	655.7	80	78	124	20.15	20.44
30	312.1	83	81	tie a steamarkeling in our	82	80	Se etentestiare britains	19.28	20.36
40	314.5	84	83	660.5	82	80	129	20.06	20.36
50 60	316.9	84	83	662.9	83	82	130	20.06	20.30
70	319.3 321.7	85	84	665.3	84	83	128	20.02	20,27
80	324.0	86 87	85 86	667.7 670.1	85 86	84	122	19.99	20.23
90	326.4	88	87		87	84 86	118 115	19.12	20.21
100	328.8	87	87	674.9	86	86	110	19.91 19.93	20.16 20.17
110	331.2	86	86	677.3	87	87	108	19.97	20.14
120	333.6	86	86	679.6	87	88	106	19.97	19.28
130	336.0	86	86	682.0	88	88	104	19.97	20.10
140	338.4	86	86	684.4	88	88	103	19.97	20.10
150	340.8	87	87	686.8	88	89	102	19.93	20.08
160	343.2	87	87	689.2	87	88	101	19.93	20.12
170	345.6	87	87	691.6	87	88	101	19.93	20.12
180	347.9	86	87	693.9	86	87	100	19.12	19.32
190	350.3 352.7	86	87	696.3	86	87	100	19.95	20.16
210	commerce e vinnos	86	87	and an expension of the last	85	87	100	19.95	20.17
220	355.1 357.5	86 86	86 86		85 85	86		19.97	19.35
230	359.9	86	AND ADDRESS OF A LABOUR.	THE PROPERTY OF TAKE	85	85 86	99 99	19.97 19.97	20.21 20.19
240	362.3	86	86		86	86	a historiannia i vidaria	19.97	20.19
250	364.7	86	mental a manager	a a successful a six	85	85		19.97	20.17
260	367.1	86	86	a b a la chester a a wie.	85	85	CALL STREET, S	19.97	20.21
270	369.5	86:	86	715.4	85	86		19.97	20.19
280	372.0	86	86	717.8	85	86	the experience of a course	20.80	20.19
290	374.4	85	86	720.2	86	86	97	19.99	20.17
300	376.8	86	86		86	87		19.97	20.16
310	379.2	86	86	THE PROPERTY OF S. P. LEW.	86	86	97.	19.97	20.17
320	381.6	86	86		86	86	96	19.97	20.17
330	383.9	86	86	a s equipment a w also	86	86	96	19.14	19.33
340	386.3	86	86		86	86	S. C.	19.97	20.17
350	388.7 391.1	86	86	I F CONTROLL CON	86	86	96	19.97	20.17
360		86	86	736.9	85	85	97	19.97	20.21

	Stack are		0.1963	TO SOLD TO STATE OF THE PARTY O	Manufacturer:	motes amada se -	Morso	
Wood	moisture (	% wet):	16.96		Model:	0.01 () 110/10/13 ()	3600	******
	Veight (lbs		15.54	.6.7 (summer of turne.	Date:	men 513 (0100) A.T. (1	8/8/01	beaute - + Program
Bum R	ate (Dry k	g/hr):	0.949	in ( ) ( ) ( ) ( ) ( ) ( ) ( ) ( ) ( ) (	Run:		2	10103 - ) 101010
Final Ter	nperature	(DGM #1) D	egrees Ranki	n:	545.434	men ex sussessions e e		meyst man
Final Ter	nperature	(DGM #2) D	egrees Ranki	n:	545.105	ing transposition		in a contraction
			grees Rankin:	en de comoné à mange	565.789	merce (romanica) (rec	denne - a thenene in a s !	
		city (feet per			13.2923224	mus ( compror) a a se	1	etanini — i morrepri
Sta	ındardized	Tunnel Flov	v (dscfm):	en Communications	137.154509	*****	francis e e energene a e e e e	
. rom, r . junio		Average	Average	Historia es distribute	i manazari manazari k	meta escario, com		
	en el Parkeron o e	Inlet +	Inlet +	eline i tratestata s'è destressor	ra monume ex summa se e da L	more excessions and	imes vonames sess	
		Outlet	Outlet	COLUMN COMPANIES DE MONOSES.	fi Permit -> commes tick	#1	#2	entente tra portugues
	Tunnel	Temp.	Temp.		1	dDGM	dDGM	name remain
Tunnel	Velocity	Meter 1	Meter 2		}	Vol.Std.	Vol.Std.	
Velocity	Ft/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.040	13.641	539.0	537.0	Contract of Continues 1 des	destruction street	· · · · · · · · · · · · · · · · · · ·	termine francis	- (
0.039	13.694	540.0	538.5	101.75	102.09	2.342	2.373	10
0.039	13.682	541.0	539.0	101.47	101.91	2.338	2.371	20
0.038	13.552	542.0	541.0	98.67	103.21	2.236	2.362	30
0.038	13.563	543.5	541.0	102.76	103.30	2.327	2.362	40
0.038	13.575	543.5	542.5	102.85	103.10	2.327	2.355	50
0.038	13.552	544.5	543.5	102.49	102.74	2.323	2.351	60
0.038	13.483	545.5	544.5	101.78	102.02	2.318	2.347	70
0.038	13.436	546.5	545.0	97.02	101.58	2.218	2.344	80
0.039	13.576	547.5	546.5	99.49	99.73	2.310	2.338	90
0.040	13.689	547.0	546.0	97.90	98.14	2,312	2.340	100
0.039	13.494 13.470	546.0 546.0	547.0	99.16	99.03	2.316	2.336	110
0.038	13.272	546.0	547.5 548.0	98.98	94.65	2.316	2.236	120
0.039	13.434	546.0	548.0	100.10 98.72	99.79 98.42	2,316 2,316	2.332 2.332	130
0.039	13.422	547.0	548.5	98.45	98.24	2.312	2.329	140 150
0.038	13.237	547.0	547.5	99.65	99.62	2.312	2.334	160
0.039	13.410	547.0	547.5	98.36	98.33	2.312	2.334	170
0.039	13.398	546.5	546.5	94.27	94.32	2.218	2.241	180
0.038	13.225	546.5	546.5	99.65	99.71	2.314	2.338	190
0.037	13.050	546.5	546.0	100.99	101.14	2.314	2.340	200
0.038	13.225	546.0	545.5	99.74	95.73	2.316	2.245	210
0.039	13.386	546.0	545.0	98.37	98.61	2.316	2.344	220
0.038	13.213	546.0	545.5	99.65	99.80	2.316	2.342	230
0.038	13.225	546.0	546.0	99.74	99.80	2.316	2.340	240
0.036		546.0	545.0	102.38	102.63	2.316	2.344	250
0.036	12.861	546.0	545.0 :	102.38	102.63	2.316	2.344	260
0.037	13.027	546.0	545.5	100.90	101.05	2.316	2,342	270
0.037	13.027	546.0	545.5 546.0	105.11	101.05	2.413	2.342	280
0.037	13.015	545.5 546.0	546.5	100.90	100.87	2.318	2.340	290
0.037	13,015	546.0	546.0	100.81 100.81	100.78 100.87	2.316	2.338 2.340	300 310
0.038	13.178	546.0	546.0	99.39	99.45	2.316	2.340	320
0.037	13.003	546.0	546.0	96.52	96.58	2.220	2.243	330
0.036	12.827	546.0	546.0	102.11	102.17	2.316	2.340	340
0.038	13.178	546.0	546.0	99.39	99.45	2.316	2.340	350
0.038	13.190	546.0	545.0	99.48	99.72	2.316	2.344	360
0.037	13.003	546.5	546.0	100.63	100.78	2.314	2.340	370
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W. M. Salley C. P. Carrier C. P. Carrier	Statuen Cumming annual	Manı	ıfacturer:	Office fillers boloom in :	MORSO				*****************
***********	************	www.eranteration.co.	Model:	Interest and terrestories	3600	************	***************************************		·
ercescono e e mano enc	in a management and	vistinas jaities recome ja suot	Date:	Service and the second second	8/8/01	Na electrica en este sono activo	ļ		indian markatan da da yan da anay ayaya
communication of the		eroomenija nemije i	Run:	Stern water ground pa	3	e e elmero domento com			***************************************
		Projec	of named protein family	r pener seema rusas	0	/8-14-14 MARKETT */			an sainte come come è
Caretonia di Servicio di	tana amana	Test Dura	CHARLES INCHES LA LABORATE &	DV SALVON MANORAL	85	hadasta da en Caspanean e (ej persona	·		***************************************
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that s rode agents.		as Volum			19.68314			ing Companies among the Companies of the	
	Average				29.035	er menor kasasa maa		One Commissioner was a	
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here of the second of the seco		the first of the second of the second	orrection	and Street, and the reserved the seconds.	0.9837	CONTRACTOR CONTRACTOR		o salvenenýhoméva	of them also any of the core
	Calibratio	********	CONTRACTOR OF STREET, ST		1.0206	er menerann am	r junio sumo, minoso	omes mune inches manes	neme minor instor son
mregazin esparato	Calibratio	FOR WHENEVER CLARESCO PLANS	T WHITE CHIEFLE CONCE		1.0311			- 14900 82000 0000 1	.,
		March 10 Mar	Aron waren property	(1) VS:	0.0777721	COMULABOR CAPO		erros arana arminimante. I	144 G. Windowsky downstrate (c. 183
		With the Mark of the Control	terry of Newson Common or N	(2) VS:	0.0775054	omand spanned		Filter	Filter
THE COMME SOURCE		,	in there are a real			(deter time) chemics i		Face	Face
Elapsed	DGM 1	DGM 1	DGM 1	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity
Time	Reading	Inlet T	Outlet T	Reading	Inlet T	Outlet T	Dry Bulb	DGM 1	DGM 2
0	393.6	78	78	739.3	76	76			romen arenten angenes, seas
10	396.0	80	78	741.7	78	76	266	20.07	20.3
20	398.4	81	79	744.0	79	77	258	20.03	19.40
30	400.8	82	81	746.4	81	78	237	19.97	20.2
40	403.2	84	82	748.7	83	80	210	19.92	19.34
50	405.6	85	83	751.1	84	81	190	19.88	20.14
60	408.0	86	85	753.5	85	83	178	19.83	20.09
. 70	410.4	87	86	755.9	86	84	168	19.79	20.0
80	412.8	88	87	758.3	87	85	161	19.75	20.0
85	414.0	88	88	759.5	87	86	158	19.74	19.99

Mario Who a Man	Proportio	nal Rate Cal	culations		(EPA Formula:	from PR5	G)	( 1000 - 1000 5 top
or Connections in	Stack are	a (ft2):	0.1963	Cample Cample and Control Cample	Manufacturer:	anne anni anni a	MORSO	and a mark office of
Wood	moisture (		18.32	2 1614 7. P. 2007 P.A. TITCHE T. THEORY. (1 4414)	Model:		3600	99°8 * 0000 * 9 80009 €
terate a retain a disting	Veight (lbs	water without the fire in to t-1 at	15.69	ere a rupur d'anno a ranno comme d	Date:	eter e premi e preside i general	8/8/01	* 10111 + 0.00 + 3.00
Bum R	ate (Dry k	g/hr):	4.103	100 X 100 F	Run:		3	,
Final Ter	nperature	(DGM #1) D	egrees Rank	in:	543,300	s approximate success		rest is there is a second
terms a want to a tentra	e exercis a trader a partie e.	miner + maner i verse e a disente a a	egrees Rank	DOTE & PRINCES PRINCE & BORDS & BORDS &	541,600	iday a mira 2 mira 2 fina 6	[ minut bare constraint	
been to a markety w property.	a martin in proper a section of	tribus a misser a minus a democratic	rees Rankin	er - a steady t with a market a trible	661.100	rdit namat Simila Niena	1 1101 2 1101 7 1101 10111	CHURCHO CE DOL
Final Tu	innel Velo	city (feet per	second):	* 1100 - Canada - 1100 - Carada - 1100 - Carada	16.8090142	e milje te trans i roje i mir	\$	Marie anni a anna 2
Sta	ndardized	Tunnel Flow	/ (dscfm):	**************************************	147.244229			Committees of the contract of
	mera 2000 2 2000	Average	Average	tota onto e vino i more a una : .		nin saun pana sana		
ar morrous co		Inlet +	Inlet +	eropore d'una d'administration d'ampire amp	i z mon samo a mea same e mijo L	× missiones kom sk		**** * ***** * ***** *
	1	Outlet	Outlet	TANTO BY OUR TOURS ALONG BUILD	13 marena 1 mar 1 min 1 min	#1	#2	ekső a tempa fi épsező a
Antico princi a sono	Tunnel	Temp.	Temp.	**************************************		dDGM	dDGM	
Tunnel	Velocity	Meter 1	Meter 2		1	Vol.Std.	Vol.Std.	,
Velocity	Ft/Sec	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.052	16.744	538.0	536.0	* ** ** ** ** * * * * * * * * * * * *		· · · · · · · · · · · · · · · · · · ·	;	0
0.050	17.419	539.0	537.0	106.88	108.01	2.328	2.360	10
0.049	17.149	540.0	538.0	107.17	103.79	2.323	2.258	20
0.050	17.068	541.5	539.5	104.24	105.34	2.317	2.349	30
0.052	17.065	543.0	541.5	99.94	96.70	2.310	2.243	40
0.053	16.969	544.0	542.5	97.33	98.26	2.306	2.336	50
0.053	16.812	545.5	544.0	96.16	97.08	2.300	2.330	60
0.051	16.362	546.5	545.0	97.08	98.01	2.296	2.326	70
0.051	16.271	547.5	546.0	96.36	97.28	2.291	2.321	80
0.051	16.231	548.0	546.5	96.04	96.96	1.145	1.160	85

g panerium ann		to take transpire substitute	Paratria estrente estretar e	5 E 2007		TE CHILD'S ALTONO L'ANGUL		OH - MARCO CHEST TOPOLO	Orodo otoro desar s
		Manu	ufacturer:		Morso				
NATIONAL AND AND AND AND AND ADDRESS OF THE PARTY OF THE			Model:		3600				
C MANUA SI MAS SI TAND			Date:		8/9/01				
D20X 0 11er 0 10310=3	Annamore or highway and	no summando dos	Run:	t Consideration	4				
O. AMERICA ASSESSED ROSEO	6,2005,000 1,000	Projec	t #:	i Omravum samusasa	J20049092				
v Vistoria v romano vistoria	Section of the second section of the second	Test Dura	CONTRACTOR STATE OF THE SECURITY OF		193		+ 1		
CONTRACTOR & STREET, A	Cottonia asserble president and	where or tracery, distribution should	e (DGM	or eventure or every bready of	44.341478	lating the state of the state of the			
t staret i modern mans	Total G	as Volum	e (DGM :	2):	44.744423				
~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	Average	Barometr	ic Pressu	ire:	28.98				
		Molecu	ılar Weig	ht:	28.56				
		Pitot C	orrection	•	0.9794				,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
	Calibratio	n Factor	(DGM #1	):	1.0206	**************************************	3		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
A Transcola, determinata decada	Calibratio	n Factor	(DGM #2	):	1.0311			240,2004,5000,5000	ening hand hand
	***********	wang Gupungan Are	A ALLON SO THE AT A PLANT OF THE	(1) VS:	0.0320172	Market Market	\$		
mer contractions		**************************************		(2) VS:	0.0317289		1	Filter	₋ Filter
Grander de maniera de marc							1	Face	Face
Elapsed	DGM 1	DGM 1	DGM 1	DGM 2	DGM 2	DGM 2	Tunnel	Velocity	Velocity
Time	Reading	Inlet T	Outlet T	Reading	Inlet T	Outlet T	Dry Bulb	DGM 1	DGM 2
0	414.3	74	74	759.7	73	72	129		
10	416.7	76	75	762.1	75	74	151	20.16	20.40
20	419.0	77	76	764.4	76	74	159	19.28	19.5
30	421.4	79	77	766.8	78	75	173	20.06	20.33
40	423.8	81	78	769.2	80	77	165	20.01	20.2
50	426.2	82	80	771.6	81	78	160	19.95	20.2
60	428.6	84	82	774.0	82	80	151	19.88	20.10
. 70	431.0	85	83	776.4	85	82	143	19.84	20.0
80	433.4	85	84	778.8	86	83	134	19.82	20.03
90	435.8	86	86	781.2	87	85	127	19.77	19.9
100	438.2	87	86	783.6	88	87	124	19.75	19.9
110	440.6	87	87	786.0	88	88	121	19.73	19.9
120	443.0	88	88	788.4	88	88	120	19.70	19.9
130	445.4	88	88	790.8	89	88	119	19.70	19.8
140	447.8	88	88	793.2	89	89	117	19.70	19.8
150	450.1	89	89	795.6	89	89	116	18.84	19.8
160	452.5	89	89	798.0	88	89	116	19.66	19.8
170	454.9	89	89	800.4	88	88	115	19.66	19.9
180	457.4	88	89	802.8	87	88	113	20.50	19.9
190	459.8	89	89	proble bedrate bedrate too	87	88	114	19.66	19.09
193	trans come marro no	88	89	805.9	87	87	buren muner france vohr	21.87	22.1

				e seinii v	、LCA Formula	s from PR5	G)	
				Control of March Control of Street Control	li			
o engage			0.1963	T 17712 ( 200) 1 (1410 - 3441) 1 144	Manufacturer:	× 100 × 2 200 × 2 200 × 2 200	Morso	
PERSONAL PROPERTY AND PROPERTY.	moisture (	Charles a registry in fraction in branch L'A	17.02		Model:		3600	10 1 200 10100
	Veight (lbs		15.61	ion s'aun è un é mise append	Date:		8/9/01	
Burn R	ate (Dry k	g/hr):	1.827	Service Countries about a Manie Countries	Run:		4	
Final Ter	nperature	(DGM #1) D	egrees Rank	in:	544.405	e seina de en		na semas misa
service of experience of the service.	a marrie o hearin il licelle al-	culture or agreed, a service of a page 14 of	egrees Rank	min a himm Pander's loves a second of	543.810	m) s (Some Some a min		FORES CHINA NAME
	A APPRIL OF AMERICAN POSSESS AND	tallice a sere traine - feetil t :	rees Rankin	teste a courte o preside or exercise or exercise to	592.381	000 ) 1000 (1300) Falls	and father street con-	. 100(0.1.1001.1.101
		city (feet per	e a saleta e salet a w chastle or court	Y MINE T YOUR A MINE TAKEN SHEE	14.0166304	raining raining rains a si		
A STATE OF STREET	THE RESIDENCE AND ADDRESS OF SERVICE	Tunnel Flow	e in medical in Property in Tensor in a configu		136.767302			
mere promite a name		Augree 2		mi) e sua e e indre e indre A agraza.		******************************		
* 1 ***** 1 ***** 1 ***		Average	Average		ļ	n estapa tradas tara tanta aperad		
	: *** *********************************	Inlet +	Inlet +	Ship time their same car	ļ. 1914 r. 1915 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 1914 1. 19	* ···· * · · · · · · · · · · · · · · ·		n) e e e e e e e e e e e e e e e e e
ene ciona ciona	Tunnal	Outlet	Outlet	roceans sand randra muita	ika vanne a anne venan a enne je	#1	#2	, description and a second
Tunnol	Tunnel	Temp.	Temp.	me canno som from cano cano s	ļu 2 m. ( m. 1 m. 1 m. 1 m. 1	dDGM	dDGM	i series ioni e un
Tunnel	Velocity	Meter 1	Meter 2			Vol.Std.	Vol.Std.	*** ****** * ***** **
Velocity	· wanevan wash	Deg. R	Deg. R	PR1	PR2	(ft3)	(ft3)	Time
0.040	13.987	534.0	532.5	Samuel Company of the	 	Charles and Charles and		0
0.040	14.246	535.5	534.5	103.28	103.60	2.338	2.367	10
0.040	14.339	536.5	535.0	99.44	99.84	2.237	2.266	20
0.039	14.318	538.0	536.5	105.97	106.40	2.327	2.358	30
0.040	14.408	539.5	538.5	103.69	104.00	2.321	2.349	40
0.040	14.351	541.0	539.5	102.99	103.39	2.315	2.345	50
0.040	14.246	543.0	541.0	101.86	102.36	2.306	2.338	60
0.040	14.153	544.0	543.5	101.00	101.22	2.302	2.328	70
0.040	14.047	544.5	544.5	100.15	100.27	2.300	2.323	80
0.040	13.964	546.0	546.0	99.29	99.41	2.293	2.317	90
0.040	13.928	546.5	547.5	98.94	98,88	2.291	2.311	100
0.040	13.892	547.0	548.0	98.60	98.54	2.289	2.308	110
0.040	13.880	548.0	548.0	98.34	98.45	2.285	2.308	120
0.040	13.868	548.0	548.5	98.25	98.28	2.285	2.306	130
0.041	14.016	548.0	549.0	96.88	96.82	2.285	2.304	140
0.041	14.004	549.0	549.0	92.59	96.73	2.186	2.304	150
0.038	13.482	549.0	548.5	100.36	100.57	2.281	2.306	160
0.040	13.820	549.0	548.0	97.73	98.03	2.281	2.308	170
0.040	13.796	548.5	547.5	101.72	97.95	2.378	2.311	180
0.040	13.808	549.0	547.5	97.65	93.95	2.281	2.214	190
0.040	13.796	548.5	547.0	108.50	108.93	0.761	0.771	193

# APPENDIX D

# Intertek Testing Services Warnock Hersey Middleton, Wisconsin

# Post Test Dry Gas Meter Calibration Data

Manufacturer: Morso	er: Morso		Model:	3600	l,	Job Number: J20049092		Date:	8/13/01 Tech:		WK	
Barometric Press:	Press:	29.13	29.13 Calibration Factors:	Factors:	DGM#1:	1.0206	1.0206 DGM#2:	1.0311	1.0311 Std.Meter DGM#3:		1.0523	
Trial No.	Std Meter Press Dro	Initial Ft. <sup>3</sup>	Final Ft <sup>3</sup>		Temp % Std. Ft <sup>3</sup>	Std. Ft <sup>3</sup>	System # 1 Initial Ft. <sup>3</sup>	Final Ft. <sup>3</sup>	Change Ft.3	Temp °F Std Ft.3		Cal Factor
	1.6	586.769	589.12	2.3510	02	2.3995	471.938	474.365	2.4270		100	1.0044
2	1.6	589.12	591.479	2.3590	0.2	2.4077	474.365	476.808	2.4430	73	2.4047	1.0012
3	1.6	591.479	593.821	2.3420	02	2.3904	476.808	479.228	2.4200	73.5	2.3798	1.0044
	Previous Cal Factor:	Minus	Avg. Cal. Factor	Avg. Cal. divided by Factor	Previous Cal Factor	Previous Times 100	equals	Precent Deviation			Average:	1.0034
	1.0206		1,0034		1.0206			1.6890				
Trial No.	Std Meter #3 Press Drop Initial Ft. <sup>3</sup> Final Ft <sup>3</sup> Change Ft. <sup>3</sup>	Initial Ft.3	Final Ft <sup>3</sup>	11	Temp °F Std. Ft <sup>3</sup>	Std. Ft <sup>3</sup>	System #2 Initial Ft.3	Final Ft.3	Change Ft.3	Temp % S	Std Ft.3	Cal Factor
-	1.6	579.466	581.835	2.3690	69.5	2.4202	810.118	812,539	2.4210	71	67	1.0015
2	1.6	1.6 581.835		2.4180	70	2.4679	812.539	815.009	2.4700	71	2.4656	1,0010
က	1.6	584.253	586.643	2.3900	70	2.4394	815.009	817.456	2.4470	71.5	2.4403	0.9996
	Previous Cal Factor:	Minus	Avg. Cal. Factor	Avg. Cal. divided by Factor	Previous Cal Factor	Previous Times 100 Sal Factor *	equals	Precent Deviation		4	Average:	1.0007
	1.0311		1.000679		1.0311			2.95030				

# APPENDIX E

Manufacturer:

Morso

Project No: Model:

J20049092, 3005306 3600

Date:

08/13/01

	(	20	C	02	19	02
	Actual	Should be	Actual	Should be	Actual	Should be
Zero Gas	0	0	0	0	0	0
Span Gas	9.96	9.96	24.65	24.65	20.93	20.93
Cal GAS #1 Deviation	0.94	0.99 5.05%	9.66	9.99 3.30%	10.24	10.2 0.39%
Cal GAS #2 Deviation	2.48	2.489 0.36%	5.83	6.086 4.21%	5.39	5.2 3.65%
Cal GAS #3 Deviation	7.74	7.68 0.78%	19.37	19.86 2.47%	17.44	17.16 1.63%
Average Deviation		2.06%		3.33%		1.89%

EQUIPMENT	MANUFACTURER	MODEL	INVEN #	MEASUREMENT UNCERTAINTY
CO analyzer	Horiba	PIR 2000	9	± 5 ppm, 95% CL
CO <sub>2</sub> analyzer	Horiba	PIR 2000	10	± 0.5%, 95% CL
O <sub>2</sub> analyzer	Beckman	755R	11	± 0.5%, 95% CL
Dry gas meter	Rockwell	T-110	12	$\pm 0.1 \text{ ft}^3/\text{hr}, 95\%$ CL
Dry gas meter	Rockwell	T-110	13	± 0.1 ft <sup>3</sup> /hr, 95% CL
Anemometer	Davis	1800	442	±2% of reading
Manometer Inclined 0-1 inch	Dwyer	125-AV	22	± 0.01-in
Manometer Inclined 0- 10inch	Dwyer	400	24	±0.02"
Barometer 35" Mercury	Princo	Nova 469	437	.01"
Magnehelic (draft indicator)	Dwyer	2000-00C	554	$\pm 2\%$ of FS = 0.005"
Scale	Toledo Masstron	ML222	25	±0.1 lbs.
Readout	WeighTronix	WI110	259	±0.1 lbs
Scale	NCI	3220	6	± 0.1-lb
Readout	GSE	450	8	± 0.1-lb
Analytical balance	Ohaus	G-110	28	±0.0005 grams
Audit weights	Ainsworth	4254S	29	Class S
Moisture Meter	Delmhorst	RC-1C	49	±1%-0-20 & ± 2% > 20
Type K T/C wire	Omega		500	± 2°F, 95% CL
Type K meter	Omega	199	54	±2°F
Temp/RH/DP indicator	Dickson	TH300	639	± 1.8 (F), +/- 2% (RH)

	, ITS EQUIPME	NT CA	LIBRATION	RECORD				
DESCRIPTION:_	Co, Co2	0	2 ana	lesers	#9,10,11			
MANUFACTURE	CO, CO2	4 /	Becknar	# 10	# 1/			
SERIAL #: <u>CO /</u>	PIR-2000 019	_	MODEL: CO	2 PIR-201	00 02 75.			
EQUIPMENT LO				07000	100 192			
PURPOSE & ACC	CURACY: 1/2/ 3	15	1					
CALIBRATION S	PECIFICATIONS/INTE	ERVAL	: le mos.	*				
CALIDDATION		T.S.A.						
CALIBRATION DATE	NEXT CALIBRATION	AGE	BRATION NCY	CAL. BY	RESULTS/ADJUST.			
1/16/99	1/16/00	In	house	RA				
1/17/00	7/17/00		11	RA				
7/6/00	1/06/01		ħ	RA	OK			
6/1/01	11/1/01		ji	BK				
		7		1				
IAINTENANCE AND	REPAIR:							
DATE OUT OF SERVICE	DATE BACK IN SER	RVICE	REPAIR AGENCY	DESCRIPTION	N OF REPAIR			

# ITS Intertek Testing Services NA Inc.

Middleton, Wisconsin

CALIBRATION DATE; REVIEWED BY:	6/1/01	CALIBRATED	BY: UK
DESCRIPTION: Gas An Located in EE			
SERIAL NUMBER: 6110	0019 CO	WHI INVENT	ORY #009
SERIAL NUMBER: 6070	023 CO <sub>2</sub>	WHI INVENT	ORY #010
SERIAL NUMBER: 100	WHI INVENT	ORY #011	
GAS ANALYZER RESPO CALIBRATION GAS US		$CO_2$	0,
	CO	CO <sub>2</sub>	$O_2$
Analysis:	,994	9.99	10,2
Meter Reading Direct Connection:	-98	9.63	10007
90% of Analysis:	88	8.67	9,15

- · Meters set with zero gas and span gas.
- · Calibration gas routed through impinger train.
- Zero gas was introduced after each time trial to return meter to zero.

ITS EQUIPMENT CALIBRATION RECORD

ITS#\_12, 13, 14

DESCRIPTION: Dry Gas Include Calibration

MANUFACTURER: Or Received T-110 # 26866 #12

PROCEDURE T-110 # 26873 # 13

SERIAL #: 3 Rockwall T-100 # 36832: # 14

EQUIPMENT LOCATION: EYE

PURPOSE & ACCURACY: ± .05 CFH

CALIBRATION SPECIFICATIONS/INTERVAL: 6 Months

CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST
7/06/00	1/06/00	In-house	RA	OK
1/31/01	7/31/01	11	AL	ok
7/30/01	1/30/01	1 *	WIL	ek
	7			
	+			
	+	+		
			-	
			11	

#### MAINTENANCE AND REPAIR:

ON OF REPAIR

				X		1.0495	1.0507	1.0503	1.0023	1.0407	1.0323	1.0509		>	•	1 0000	1.0232	1 0224	1.0206		1			1.0364	1.0292	1.02/8	1.0311	031100
			3,644	Ivieler	FINA	5/3.444	574.395	577.315	578 316	570 703	217.403	AVERAGE		Motor	Final	ACD 042	407.045	471.811	AVERAGE		Median	Melen	FIIIa	807.912	808.937	002.23	AVERAGE	
	14		Coiromotos	Volume	1 Oco 1	1.0881	1.0540	1,0030	11165	1 0767	200		12	Snirometer	Volumn	1 0881	1,0001	1.0540		13	Crisomotor	Tolumen	1 0000	1.0936	1,1103	1		
	Inventory Number		Meanitement	Inches	22 0275	72 1075	23.1875	24 0625	24.5625	23 6875			Inventory Numbe	Measurement	Inches	73 9375	73 1875	23.1875		Inventory Number	Messurement	Inches	204 0695	200.47	23 6875	0.000		
	13		Meter	Pressure	17	1.6	1.7	1.6	1.6	1.6			-	Meter	Pressure	1.7	1.6	1.5		2	Meter	Pressure	16	1.0	1.6			
	Meter Number		Meter	Теппретапте	71	7.2	71.5	71	71.5	72			Meter Number	Meter	Temperature	74	74	74		Meter Number	Meter	Тетрегарие	73	74	74			
SPIROMETER			Vapor Pressure	of H,O (Hg)	1.0220	1.0560	1.0560	1.0735	1.1270	1.0910			4	Vapor Pressure	of H <sub>2</sub> O (Hg)	1.0220	1.0560	1.0560		2	Vapor Pressure	of H,O (Hg)	1.0735	1.1270	1.0910			A
	29.38		Spirometer	0	80	81	81	81.5	83	82				Spirometer	Temperature	80	81	81			Spirometer	1.	81.5	83	82			M Po
	Baro:		Barometric	Pressure	29.38	29.38	29.38	29.38	29.38	29.38				Barometric	Pressure	29.38	29.38	29.38			Barometric	Pressure	28.76	28.76	28.76			revision
	07/30/01	Y	Meter	Initial	572.46	573.444	574.395	576.333	577.315	578.316				Meter	Initial	468.828	469.843	470.83			Meter	Initial	806.912	807.912	808.937			
	Date:	By:	Run	Number	1	2	3	4	2	9				Run	Number	1	2	3			Run	Number	1	2	3			



### **Certificate of Calibration**

1000055507

Page 2 of 2

#### Calibration Standards

NIST Traceable #	Instrument ID#	<u>Description</u>	Model	Calibration Date	Date Due
1000026619	01-0098	Stopwatch	810033	20 APR 2000	20 APR 2001
1000027795	01-0287	Resonant Sensor Barometer	DPI 141	27 APR 2000	27 APR 2001
1000051990	01-0818	Humidity & Temperature Meter	HM34C	01 MAR 2001	01 MAR 2002
1000052381	01-0178	Thermistor Thermometer	600-8525	22 MAR 2001	22 MAR 2002
1000055291	01-0103	Electronic Manometer	Medm 500	05 APR 2001	05 APR 2002

### ITS EQUIPMENT CALIBRATION RECORD

DESCRIPTION: <u>Manager</u>	ter 0-1" Inclined
MANUFACTURER:	· · · · · · · · · · · · · · · · · · ·
SERIAL #: 882	MODEL: 125 AV
EQUIPMENT LOCATION: 6	missions Lab - E+E
PURPOSE & ACCURACY: ± /%	6 g F5 (0.01 in)
CALIBRATION SPECIFICATIONS/II	NTERVAL: 6 mos. ( jearly

CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST.
3/17/94	9/17/94	Inhouse	WK	
10/1/94	4/1/95	11	WK	
4/11/95	10/11/95	"	RA	
10/16/95	4/16/96	11	RA	
4/19/96	10/19/96	"	WK	
10/9/96	4/9/97	4	RB	
5/14/97	11/14/97	~,	RA	
12/16/97	6/16/98	2	RA	
8/12/98	2/12/99	"	RA	
1-22-99	7-22-99	u	RA	
7/16/99	1/16/00	9	RA	
1/14/08	1/14/06	Ze .	RA	
2/13/01	2/13/02	- //	AL	0.0015-in

DATE OUT OF SERVICE	DATE BACK IN SERVICE	REPAIR AGENCY	DESCRIPTION OF REPAIR

Middleton, Wisconsin

CALIBRATION DATE:

CALIBRATED BY:

DESCRIPTION: Manometer Inclined 0-1"

Located in EE lab

**SERIAL NEMBER: 882** 

MODEL: 125 AV

WHI INVENTORY #022

MICROTECTOR	MANOMETER	DEVIATION IN.
,379	, 7.5 7	0.001
.287	. 576	0,002
, 225	.454	0.004
.,3/	,260	0.002
1054	,105	0.003
1021	.042	0
,004	008	0
.44.2	786	0.002
1335	,670	0

AVERAGE DEVIATION = 0.0015 INCHES

Note: Microtector reading is exactly 1/2 of the manaometer reading



- A				
	ITS EQUIPMEN	T CALIBRATION RI	ECORD ITS N	To. 024
DESCRIPTION:	Manometer	0-10"		
MANUFACTURER:	Dwyer			
SERIAL No: 400		MODEL:		
EQUIPMENT LOCA	TION:			
PURPOSE & ACCUF	RACY: ± .01	in from 0-1"	± . 1 for	- 1-10 "
		RVAL: 6 mo		
CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST
5/15/00	5/15/01	in-house	WK	ok
8/20/01	2/20/01	r, 4	AL	ole
M				

DATE OUT OF SERVICE	DATE BACK IN SERVICE	REPAIR AGENCY	DESCRIPTION OF REPAIR

Middleton, Wisconsin

CALIBRATION DATE: 8/20/0/ REVIEWED BY: marthage

DESCRIPTION: Manometer Inclined 0-10"

O / CALIBRATED BY:

MODEL: Dwyer

**SERIAL NUMBER: 400** 

WHI INVENTORY #024

Item used to calibrate: Microtector WHI No. 103

MICROTECTOR	MICROTECTOR MANOMETER (* w.v)	ACTUAL	Difference
0.138	0.276	0.270	-:00/0
0.277	6.554	0.540	014
0.313	6.626	0.620	006
0.428	0.856	6.840	-,016
0.626	1.252	1.250	-,002
0.939	1-878	1.870	-,008

AVERAGE DEVIATION = 1009 W.C.

$$STD = \sqrt{n \sum_{x}^{2} - (\sum_{x})^{2}} = .005 \text{ in. w.c.}$$



#### TRACEABILITY TO

#### NATIONAL INSTITUTE OF STANDARDS & TECHNOLOGY

All PRINCO Barometers, Model Series 453 and 469, have been tested in comparison with the Fortin type mercurial barometer, serial no. W12655, which was calibrated on May 3rd 1994 against a Hass primary standard Type MS-3 Micrometer Standard Barometer, serial number 2510, certified by the National Institute of Standards & Technology (NIST Identification No. P-7485).

Barometer scales are positioned to read correctly with no correction for capillary depression. Compensation has been made for the average condition of capillary by tapping the instrument slightly before each reading to bring the meniscus height to its average value. The length of the scale of this barometer has a zero correction at 62°F on the English side and 0°C on the metric side. The density of the mercury is standard at 0°C. To correct for temperature of both density and scale length, use the combination temperature correction table as published in National Weather Service, Circular F. (See PRINCO Instruction Manual). To correct for gravity use the gravity correction tables in the same publication. No gravity correction is needed at 45° latitude.

This barometer is accurate to  $\pm 0.3$  mb, 0.2 mm, or 0.01 inch of mercury when carefully set and read, and after temperature and gravity corrections have been applied. The thermometer on the barometer is accurate to  $\pm 0.5$ °C.

The National Institute of Standards & Technology does not state any recommendations for a barometer to be re-certified.

If the barometer is not abused in any way it should never go out of calibration.

Princo Instruments, Inc. recommends that you return the barometer every 3 to 5 years.

ITS EQUIPMENT CALIBRATION RECORD  ITS# 534
DESCRIPTION: Magnehelic
MANUFACTURER: Dwyer 2000-00
SERIAL #: R990430 mP21 MODEL: 2000-00
EQUIPMENT LOCATION: $\mathcal{E} \neq \mathcal{E}$
PURPOSE & ACCURACY: ± 0, 005 in. WL

CALIBRATION SPECIFICATIONS/INTERVAL: 6 MO.

CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST.
8-10-99	2-10-00	In-house	RA	
8-10-99	7-14-00	//	12	
5/15/00	11/15/00	11	RA	
2/2/01	8/2/01	11	AL	0.0028"
7/29/11	1/29/02	10	WK	ave .003 STDEU .002
1 1/01	/ /			

DATE OUT OF SERVICE	DATE BACK IN SERVICE	REPAIR AGENCY	DESCRIPTION OF REPAIR

Middleton, Wisconsin

1/2

CALIBRATION DATE: 7/29/0/
REVIEWED BY: provide Example

CALIBRATED BY: \_\_\_\_\_\_

**DESCRIPTION: Magnehelic** 

MODEL: Dwyer 2000-00

SERIAL NUMBER: R990430MP21

WHI INVENTORY #554

Located in E&E Console

**USING: MICROTECTOR #103** 

MICROTECTOR	MICROTECTOR ACTUAL	MAGNEHELIC	N/L DEVIATION
111	,222	.222	0 8
.08/	,172	1175	2121
077	,142	.144	39 70/11
,039	1068	,072	1.000 5.
,054	.108	,1/2	1.53/2 3.5
,048	,096	.101	2.157 4.9
150:	1042	1046	3 132 8

AVERAGE DEVIATION = 7

See page 2/2 For correct std. deviation È differences.

WP DOCS\CALSHEET.WPDP.40

Middleton, Wisconsin

CALIBRATION DATE:_ REVIEWED BY:	CA	LIBRATED BY:	=
DESCRIPTION: Magnel	helic	MODEL: Dwyer 2000-	00
SERIAL NUMBER: R990 Located in E&E Console	0430MP21	WHI INVENTORY #5	54
USING: MICROTECTO	PR #103		MP 8/20/01
MICROTECTOR (in.)	MICROTECTOR ACTUAL (in. W.C.)	MAGNEHELIC (in. W.C.)	Difference (in. W.C.)
			,000
			. 003
		+	. 002
		V	2004
, A			,004
			,005
			.004
			,001

DESCRIPTION:	Weigh			
MANUFACŢŲRER	: Tronix			
SERIAL #:(8)68	00082 (25)	3082MODEL: <u>NC.</u>	(8) T 5780	(259)
SERIAL #:(0) 00	(42.)0	2002 ANIODEL. 11C.	2 3700	WI 110
EQUIPMENT LOCA	ATION:			
PURPOSE & ACCU	JRACY: 1/6			
	ECIFICATIONS/INTE	DVAI. /. P	2. 41-	
CALIBRATION SP	ECIFICATIONS/INTE	RVAL.	1007/195	
			1 202 030	Ta-su-su-su-su-su-su-su-su-su-su-su-su-su-
CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUS
8-11-98	2-11-99	In-house	RA	
5-19-98	11-19-98	Cream City	-	
11-98	5-99	CREAM CIT	1 JEFF	
5/21/99	11/21/99	" "	cc	
11/99	5/00	Cream City	741	
3/00	9/00		100	Biz State
9/27/00	3/27/01			
4/12/01	10/12/01			OK
1				
1				
		1		

)

#### Certificate of Calibration CREAM CITY SCALE, CO INC.

		Stoughton Rd.,	Madison, WI 5	3716 (608	s) 222-9427 c	or (888) 934-4	9/1	1
CUSTOMER _	ITS			<u></u>		D	ATE 9/12	401
ADDRESS			_	_				
CITY, STATE &								
NDICATOR MI	G. C-SE		CAPAC	ITY _	1004	CL	ASS	
MODEL	950		DIVISIO	ONS _	,01		CURACY _	
ERIAL NO.	1017	75	_ LOCATION		re Dan tes	TO	LERANCES U	JSED_
BASE MFG.	NI		I.D. #		6,8		11544	
MODEL	3770				INTERVA		Jami Annu	1
SERIAL NO.	7901	43	NEXT C	CALIBRA	ATION DU	JE/	10/01	
			SHIF	TEST				
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			INCREASING	G LOAD	TEST			
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	5	2	-	2			!!	
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			COTUMEN I	COMP	5770 F.433	T / NAT		
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COMMENTS:						-		
COMMENTS.								
TEST WEIGHT C								
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White - Customer Copy Canary - Office Copy

#### Certificate of Calibration CREAM CITY SCALE, CO INC.

CUSTOMER _	2009 S. S	Stoughton Rd.,	Madison, WI 53	3716 (6	08) 222	2-9427 (	or (888) 9.		TE 9/10	4
ADDRESS CITY, STATE &	ZIP in a	alelon is	И	_						
INDICATOR M MODEL SERIAL NO. BASE MFG. MODEL		itronix 1	CAPACI DIVISIO LOCATI I.D. # CALIBR	ONS ON 25+	25		_ A v) 1	CC	URACY _ URACY _ ERANÇES ( 14894 mi Annua)	1%
SERIAL NO.	NIV		NEXT C	ALIB	RATIO	DN DU	JE _	101	UI	
FLOOR S	SCALE	BE	SHIFT ENCH SCALE	TEST			*			
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S SHIFT TEST	WITHIN TOL		) YES ( INCREASING			T	DJUSTEI D TEST		ER ADJUSTI	MENT
SUBSTITUTION WEIGHT	TEST WEIGHT	READING	ERROR	1	STITUT WEIGH		TEST WEIGH		READING	ERROR
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	2W	نىلا					200		3w	-
	300	3641	ナー				300		7ai	_
	9W	9W1	*·I	-			900 VW		Jw FW	2
	3"	24.7	3-1				J			
IS SCALE WITHIN I (if no, see final load t	'est)							CE TO	DLERANCE (O	ACIN
WAS SCALE W COMMENTS:	TTHIN CUS	TOMERS RI	EQUIRED AC	CCURA	ACY?	(A)	Y ( ) I	V		
TEST WEIGHT ( NIST TRACEAB LIST TEST WEIG	ILITY CERT	FICATE NO		<sub>0</sub> U						
SCALES WERE C FAIN THE ACCUI INSTITUTE OF ST	RACY OF THE	E SCALE CON	NFORM TO TH	E TOL	ERANG	CES ES	TABLISH	O RE	STORE AND/ BY THE NATI	OR MAIN ONAL

DESCRIPTION: analytes	al Balane	e	
DESCRIPTION: <u>Inalyter</u> MANUFACTURER: <u>OK</u>	ULLS		
SERIAL#: 5336	MOI	DEL: 6/10	
EQUIPMENT LOCATION:	* E		
PURPOSE & ACCURACY:	.0005 g		
CALIBRATION SPECIFICATIONS	S/INTERVAL:	6 month	

CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST.
6-2-97	12-2-97	An-house	RA	
6/25/98	12-25-98	LI	WK	
12/11/98	6/11/98	i,	RA	
6/1/99	12/1/99	11	RA	
1/14/00	7/14/00	4 "	RA	
7/6/00	1/6/01	ii	RA	OK
2/1/01	8/1/01	11	AL	0.00019
7/30/01	1/30/01	14	WK	,000 18 are det
-				
		4-		

DATE OUT OF SERVICE	DATE BACK IN SERVICE	REPAIR AGENCY	DESCRIPTION OF REPAIR

Middleton, Wisconsin

CALIBRATION DATE: 7/

CALIBRATED BY:

REVIEWED BY: MARKED

**DESCRIPTION: Analytical Balance** 

MODEL: (Ohaus) Galaxy 110

SERIAL NUMBER: 5336

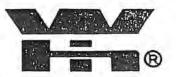
WHI INVENTORY #028

USING: Ainsworth Class S Weight WHI #29

WEIGHT	MEASURED	DIFFERENCE (g)
2 mg	BROKEN WE	16117
5 mg	0.00519	0.000/
10 mg	6.0104	0.0004
20 mg	0.0202	0,0002
50 mg	0.0499	0.0001
100 mg	0.1001	0.0001
1 g	0.9999	0.000/
20 g	20.0000	-0-
50 g	49.9996	00.0004
100 g	100.0002	000,0002

Average Difference = 0.060/778 grams

Standard Deviation = , 200 14 grams MP



# WARNOCK HERSEY INTERNATIONAL, INC. MIDDLETON WISCONSIN 53562

2050 South Pecos Street, Denver CO 80223 (303) 934-2276

CLASS	S	WEIGHT SET

	RANGE:	100	GRAMS TO _	1	GRAMS MILLIGRAMS
CATALOG NO	4254	- 5	SERIAL NO	393	92

	CONSTRUCTION	MATERIAL	DENSITY g/cm³ @ 20° C
GRAM WTS.	☐ 1-piece	Naval Brass, rhodium plated	8.40
	2-piece screwknob	☐Brunton* Metal	7.89
		☐ Stainless Steel	7.85
MILLIGRAM WTS. 30 mg & larger	☑ 1-piece	QTantalum	16.6
MILLIGRAM WTS. 20 mg & smaller	☑_I-piece	Aluminum .	2.7

Naval Brass average composition-60% copper, 39.25% zinc, .75% tin. ASM #4612B.

Brunton\* Metal average composition—25.5% chromium, 21% nickel, 2% manganese, 1.5% silicon, .25% sulphur, phosphorus, carbon.

Stainless Steel average composition—18% chromium, 9% nickel, 1% manganese .5% silicon, .1% carbon, AISI #303

Rhodium plated weights have an undercoat of electrolytic nickel plate.

All Ainsworth weights meet or exceed the National Bureau of Standards Handbook 77, Volume III, issued February I, 1966, Concerning: Matertial (hardness, corrosion resistance, magnetic properties, density, adjusting materials); Design (Shape, dimensions, number of pieces); Surface (irregularities, porosity, surface finish); Denominations; Markings; Constancy under variations of humidity; Packaging.

We can supply new class, S, and S-1 Sets with any range between 100g and 1 mg. New weights or weight sets and even those you are now using may be calibrated and certified by Ainsworth Products, Inc., Standards Laboratory to show traceability to National Bureau of Standards.

Made by AINSWORTH PRODUCTS, INC. 2050 South Pecos St., Denver, CO 80223

### ITS EQUIPMENT CALIBRATION RECORD

		ITS	5# 49		
DESCRIPTION: Maisture 1	neter				3
MANUFACTURER: Delmho	est				
SERIAL #: 1435C		RC-1C	AND	CAL.B.	lock
EQUIPMENT LOCATION: Eu &					. Y
PURPOSE & ACCURACY: ±1 % -0-	20 + 12%	6 > 20			
CALIBDATION SPECIFICATIONS/INTER	NAT.	13			

CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST
8/20/01	2/20/02	In-house	AL	OK

DATE OUT OF SERVICE	DATE BACK IN SERVICE	REPAIR AGENCY	DESCRIPTION OF REPAIR



#### LETTER OF CERTIFICATION

October 12, 2000

Intertek Testing Service 8431 Murphy Dr. Middleton, WI 53562

Gentlemen:

Subject: Moisture Content Standard Model MCS-1 Serial No. 101200

This is to certify that the primary calibration - electrical resistance - of the Delmhorst Moisture Meters has been tested on equipment whose accuracy is certified by the:

General Radio Model No. 1644-A S/N 2526 Keithley Model No. 97, S/N 283483.

The calibration of these instruments, certified by Ballantine Laboratories, Inc. with Report No. D19016 dated December 9, 1999, is traceable to the NIST.

The MCS-1 (Moisture Content Standard) is an external means to check the Delmhorst Moisture Meters for wood at two points -12 % and 22% on the Douglas Fir, 4 Pin mode; the two points will yield readings of 12.7% and 23.6% if the meters are set on the Douglas Fir, 70°F, 2 Pin mode. The analog meters in their standard form are always set at Douglas Fir 70°F 4 Pin mode. The resistance values at said points, i.e., 120 Megohms and 1.1 Megohms verified with the same equipment as above, are within  $\pm 10$ % of the above values.

The analog Moisture Meters, checked with the "MCS-1" Standard, should read within (±) one division on the dial at the point(s) checked; the digital Moisture Meters should read within ±0.5 M.C. of the indicated values.

Sincerely,

John C. Laurenzi

V.P. Manufacturing

JCL: dm

Middleton, Wisconsin

CALIBRATION DATE: 8/20/01

CALIBRATED BY:

DESCRIPTION: Delmhorst moisture meter cabibration block MODEL: MSC-1

**SERIAL No. 101200** 

REVIEWED BY:

WHI INVENTORY # 049

Calibrated using Fluke multimeter WHI No. 109

Calibration block position	Desired reading	Actual reading	Accepted range
12%	8.33 nS	8-72	7.50 - 9.16 nS
22%	1.1 Megohms	1.107	0.99 - 1.21 MΩ

ITS EQUIPMENT CALIBRATION RECORD

		106	
ITS#	TE	500	/
110#	1	_	

DESCRIPTION:	THERMO	coup	OLES		
MANUFACTURER:	OMEG4				
SERIAL#:			MODEL:		
EQUIPMENT LOCA	TION: E+E	CA	В		
PURPOSE & ACCUF	RACY:				6 mos.
CALIBRATION SPE	CIFICATIONS/INTER	RVAL:	BOILING WA	TER 10	E BATH 6
					2
CALIBRATION DATE	NEXT CALIBRATION	CALI	BRATION AGENCY	CAL. BY	RESULTS/ADJUST.
6-4-97	12-4-97		IN HOUSE	RA	
12-12-97	6-12-99		4	RA	
4-26/98	12-26-98		11	WK	
12-11-98	6-11-99		11	RA	
6/1/99	12/1/99		-11	RA	
5/30/00	11/30/00		11	AL	± 2°F
1/24/01	7/24/01		11	AL	1 2 Flwithn
7/29/01	1/29/02		1 x	WK	OK
				<u></u>	
				40	
MAINTENANCE AND RE	PAIR:				
DATE OUT OF SERVICE	DATE BACK IN SERV	VICE	REPAIR AGENCY	DESCRIPTION	N OF REPAIR

Middleton, Wisconsin

CALIBRATION DATE: 7/29/0	CALIBRATED BY:
REVIEWED BY: A>	

Description: Thermocouple wire

No. 500

WHI inventory

ROOM TEMPERATURE 70

Thermocouple number and location	Thermocouple immersed in boiling water	Thermocouple immersed in ice
1) Flue Gas	2/2	33
2) Room Temperature	2//	32
3) Dry Bulb (in tunnel)	2 (	32
4) Wet Bulb (in tunnel)	2//	3 2
5) Unit Top	2//	3 3
6) Unit Back	7//	33
7) Unit Right Side	2//	33
8) Unit Left Side	2//	32
9) Unit Bottom	2//	23
10) Catalyst Downstream	21/	32
11) Catalyst Center	9//	33
12)	5//	33
13)	9-11	23
14)	2/2	33
15)	2/1	33
16)	2//	73
17) DGM (in)	2 ( /	33
18) DGM (out)	2 / /	
19) Filter (1)	211	33
20) DGM (in)		22
21) DGM (out)	211	35
22) Filter (2)	2//	33

es.	ITS EQUIPME	NT CAI	LIBRATION I	RECORD ITS#	54
DESCRIPTION: <u></u> MANUFACTURE	Digital Ty, R: Omega	a k	Ther	ro Couple	Meter
SERIAL #:	21662		MODEL:_ <i>/9</i>	9-KF-H	1-X
EQUIPMENT LOC	CATION: EXC				
PURPOSE & ACC	URACY: 170 F	土	2°F (LH	1)	
	PECIFICATIONS/INTE				
CALIBRATION DATE	NEXT CALIBRATION	CALIF	BRATION ICY	CAL. BY	RESULTS/ADJUST.
12/11/98	6/11/99	Bi.	house	RA	
6/1/99	12/1/99		e,	RA	
1/14/00	7/14/00		4	RA	
5/24/00	11/24/00	Cal	2806		Cal Lab
11/21/00	54/21/00	Ca	l Lab		OK
5/8/01	\$ 11/8/01	(	al Lab		
	1.				
	4				
MAINTENANCE ANI	REPAIR:				
DATE OUT OF SERVICE	DATE BACK IN SE	RVICE	REPAIR AGENCY	DESCRIPTIO	ON OF REPAIR

3 5-K North 126th Street Brookfield, WI 53005 262-790-1916 262-790-1949 FAX @callabco.com





#### Customer

Intertek Testing Services 8431 Murphy Dr. Middleton, WI 53562

www.callabco.com

#### Instrument

Manufacturer: Omega Model: 199

Description: Digital Temp. Meter

Serial #: 21662 ID#: 000054

#### Calibration Information

Technician: Mark Adams Temperature: 71°F (21.7°C)

Humidity: 39%RH

Calibrated On-Site

Cal Interval: 6 months Cal Date: 05/08/2001 Due Date: 11/08/2001

Received Condition: Fully operational and within tolerance Work Performed: No adjustments required and calibrated to manufacturers specifications using manufacturers

procedure

#### Calibration Standards Used

Cal:10/18/2000 Due:10/18/2001 ID#1334 Fluke 5500A/3 Calibrator Serial#6535009



This instrument was calibrated with a minimum 4:1 TUR/TAR unless otherwise stated. These represent best uncertainties. Actual uncertainties are available upon request.

Best Measurement Uncertainty

Temperature ±0.2°C

Quality Team Member - Issue Date: 05/09/2001 Reviewed and approved by

All Functions/Ranges were checked unless otherwise stated. This Certificate may not be reproduced except in its entirety without the written approval of CAL LAB Co., Inc. This Report Certifies that all Calibration Standards used in the test is traceable to NIST, and the test was performed in accordance with ANSI/NCSL Z540-1-1994 (ISO/IEC 17025-1999).

Page 1 of 1 for Certificate # 1062557

		T CALIBRATION RI	ITS#	
DESCRIPTION:	Emp/Rel. He	unid/Dew to	Pint Te	ster
MANUFACTURER:	Dickson			*
SERIAL#: 000	150593	MODEL: 1	1300	
EQUIPMENT LOCA	TION: E-E			
PURPOSE & ACCUI	RACY: <u>£</u> 1.8	°F, 12%	RH	
CALIBRATION SPE	CIFICATIONS/INTER	RVAL: 6 mo.		
CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST

CALIBRATION DATE	NEXT CALIBRATION	CALIBRATION AGENCY	CAL. BY	RESULTS/ADJUST
5/8/01	5/21/00	Cal Lab		OK
5/8/01	11/8/01	11 11		ok
		1.		
¥ + 1				
			N .	

DATE OUT OF SERVICE	DATE BACK IN SERVICE	REPAIR AGENCY	DESCRIPTION OF REPAIR

95-K North 126th Street Brookfield, WI 53005 262-790-1916 262-790-1949 FAX @callabco.com





#### Customer

Intertek Testing Services 8431 Murphy Dr. Middleton, WI 53562

www.callabco.com

#### Instrument

Manufacturer: Dickson Model: TH300

Description: Temp/Humidity Indicator

Serial #: 00050593 ID#: 000639

#### Calibration Information

Technician: Mark Adams Temperature: 71°F (21.7°C)

Calibrated On-Site

Cal Interval: 6 months Cal Date: 05/08/2001 Due Date: 11/08/2001

Humidity: 39%RH

Received Condition: Fully operational and within tolerance

Work Performed: No adjustments required and calibrated to manufacturers specifications using CAL LAB

procedure #30

#### Calibration Standards Used

Cal:04/27/2001 Due:04/30/2003 ID#1385 Cole Parmer 3312-20 Psychrometer 'F Serial#NONE Cal:01/16/2001 Due:01/31/2002 ID#1390 Fluke 743B Process Calibrator Serial#7005629 Cal:09/28/2000 Due:09/30/2001 ID#1589 Thermocouple Prod. 400-T-12 T Thermocouple Probe Serial#NONE



This instrument was calibrated with a minimum 4:1 TUR/TAR unless otherwise stated. These represent best uncertainties. Actual uncertainties are available upon request.

Best Measurement Uncertainty

Humidity ±3%

Temperature ±0.2'C

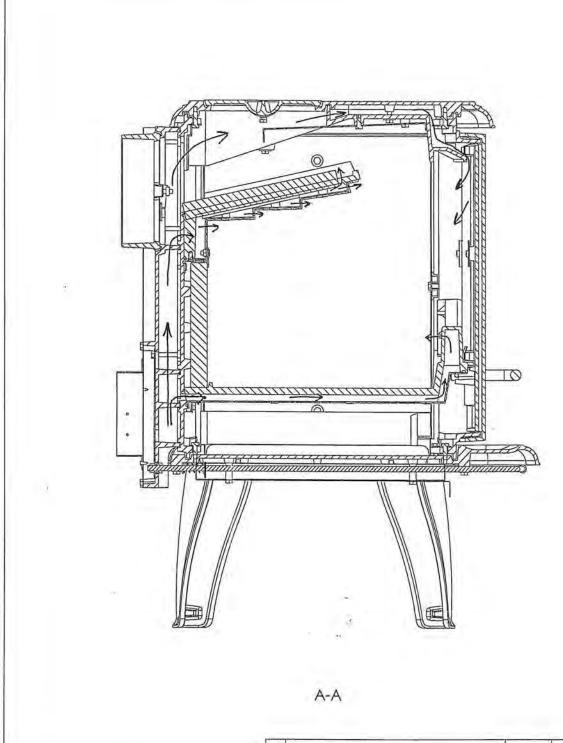
Quality Team Member - Issue Date: 05/09/2001 Reviewed and approved by

All Functions/Ranges were checked unless otherwise stated.

This Certificate may not be reproduced except in its entirety without the written approval of CAL LAB Co., Inc. This Report Certifies that all Calibration Standards used in the test is traceable to NIST, and the test was performed in accordance with ANSI/NCSL Z540-1-1994 (ISO/IEC 17025-1999).

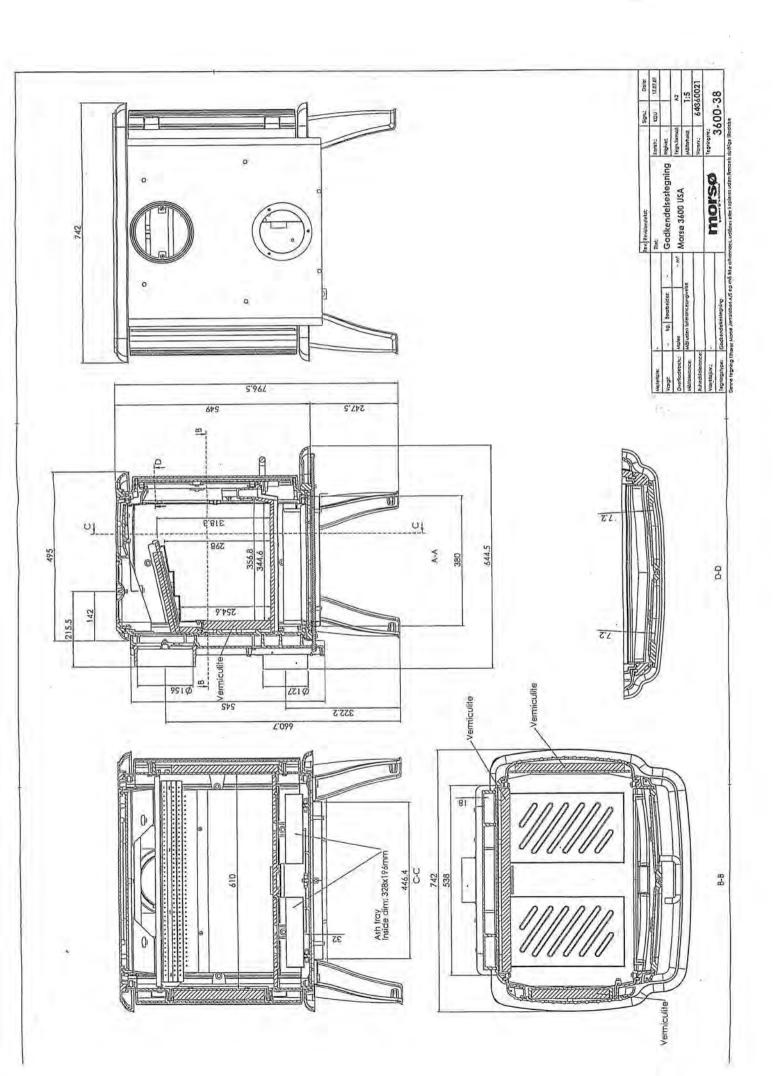
Page 1 of 1 for Certificate # 1062543

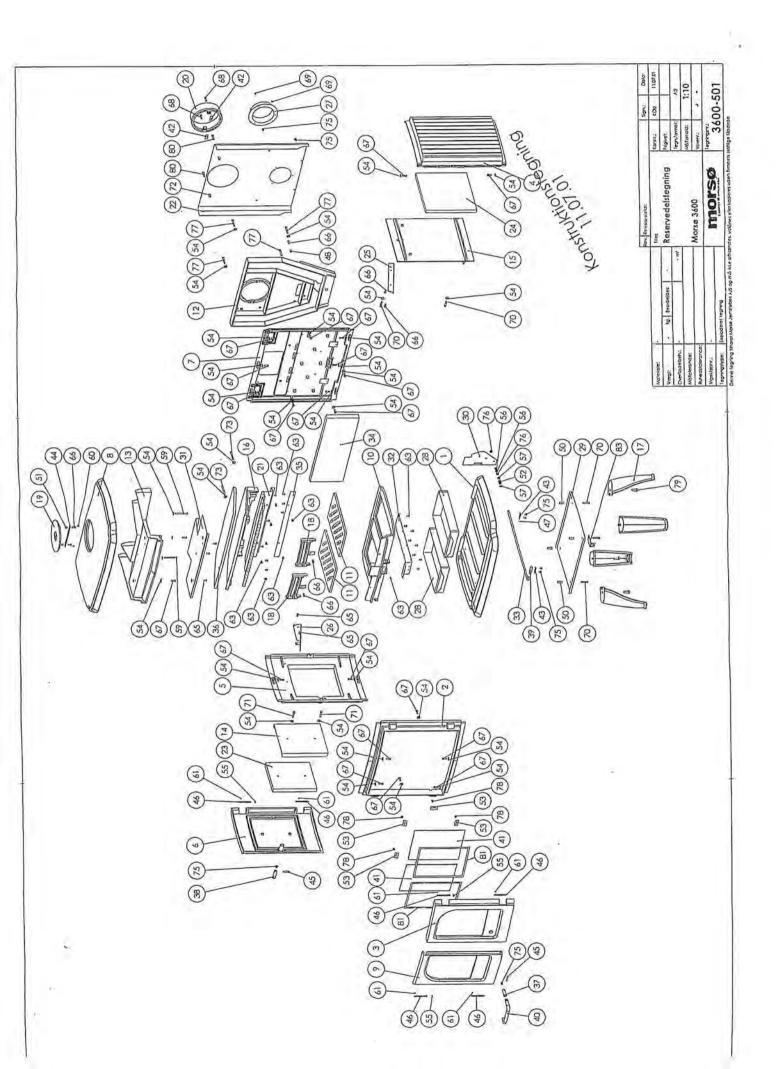
# APPENDIX F



				Rev. Revisionstekst:		Sign.:	Dato:
Materiale:			Titel:	Konstr.:	KDU	17.08.01	
Vægt:	- kg.	Bearbejdes:		Airflow diagram	Frigivet:	-67	- 5
Overfladebeh.:	./		- m²		Tegn.format:	A4	
Måltolerance:	Mål uden toleranceangivelse		ia and a single sign	Målforhold:		1:5	
Ruhedsfolerance:		Morsø 3600	Varenr.:				
Værktøjsnr.:			morsø	Tegningsnr.: 3600-39			
Tegningstype:			By againment in the Pays Darron Cost				

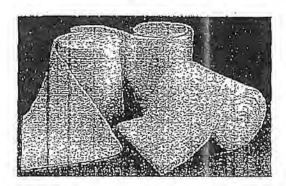
Denne tegning tilhører Morsø Jernstøberi A/S og må ikke afhændes, udlånes eller kopieres uden firmaets skriftlige tilladelse





### Technical Datasheet.

#### INSULFRAX@ BLANKET



KERAMAB's latest addition to its fibres product range, INSULFRAX®, is a revolutionary breakthrough in insulating materials technology.

This new product is based on a calcium-magnesium-silica chemistry, giving excellent thermal and physical stability up to its operational limit of 1100°C.

INSULFRAX® products can be used in a wide range of applications as thermal insulation, particularly in Fire Protection and in Domestic Appliances.

#### General Characteristics

INSULFRAX® Blanket offers users a number of important advantages over other man-made mineral fibres:

- Excellent thermal and physical stability up to 1100°C
- Light weight, flexibility and exceptional acoustic absorption properties
- Improved tensile strength of INSULFRAX® Blanket due to our specialist manufacturing technology
- INSULFRAX® needle felted Blanket contains no organic binders

Chemical Analysis (wt.%)				
SiO,		61.0 - 67.0		
CaO	-	27.0 - 33.0		
MgO	43	2.5 - 6.5		
AI,0,	1.6	< 1.0		
Fe.O.		< 0.6		

Effective: 29051998/MJH.mvo Supersedes: 0704 1592/MUFUTIVO All Rights Reserved Price List No.: III 016

Page 1 of 2

The information, recommendations and epinions set forth The information, resommendations and opinions set fortherion are offered solely for your consideration, inquiry and verification, and are not, in part or total, to be constructed as constituting a warranty or representation for which we also where legal responsibility. Nothing contained herein is to be interpreted as authorization to practice a paterned Invention without a license.





### Technical Datasheet.

#### Typical Applications

#### Domestic Appliances

- Boiler insulation
- Fire seals
- Storage heater insulation
- Wood-burning stove seals
- Domestic cooker insulation
- Chimney fill

#### Fire Protection

- Offshore rig accommodation modules
- Building expansion joints
- Column and beam wrap
- Fire door in fill

Typical Physical Properties					
Colour	- B	luish-white			1:
Classification Temperature	- 1	100°C			2
Melting Point	- >	1330°C			
Fibre Diameter		.2 microns (			
Tensile Strength .	- >	35 kPa (128	3 kg/m³)		
Thermal Conductivity Data, W/m (based on CEN draft method ASTM C-201)	ı°К б4 kg/m²	96 kg/m³	128 kg/m³	160 kg/m³	192 kg/m²
200°C Mean Temperature	0.07	0.06	0.05	-	- 1
400°C Mean Temperature	0.10	0.09	0.08	0.07	0.06
600°C Mean Temperature	0.18	0.14	0.12	0.11	0.10
800°C Mean Temperature	0.27	0.22	0.18	0.16	0.15
Permanent Linear Shrinkage	1000°C	1100°C			

Where appropriate Physical Properties and Thermal Conductivity Data measured according to ENV 1094-7:1994

#### Fire Test Data

INSULFRAX® Blanket is non-combustible in accordance with BS476:Pt4 and is approved for use against cellulosic and hydrocarbon fires and for dry wrapping of structural steel. Certification details can be supplied on request.

Farm:A1-050 Effective: 2905 1998/MUH/mvo Supersede: 070A1998/MUH/mvo All Rights Reserved

Page 1 of 2

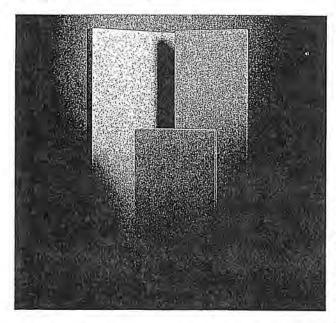
Price List No.: III 076

The information, recommendations and opinions set farth herein are offered solely for your consideration, inquiry and varification, and are not. In part or total, to be constructed as constituting a warranty or representation for which we assume legal responsibility. Nothing contained herein is so be interpreted as authorization to practice a parented invention without a license.





### SKAMOLEX VIP-12 Vermiculite Block Insulation



Packing Colour Code: GREEN/BLACK.

#### Grade: VIP-12 Temp. limit: 1150°C (2102°F)

The continuous efforts to improve energy efficiency of aluminium reduction cells have intensified demands for better heat insulation in pot cathodes.

Although a number of insulating products are available on the market, many smelters are still facing the problem of reducing the temperature of penetrating bath substances to solidifying point at a line between the carbon and the insulation layer, thus achieving a freezing of bath substances before they penetrate further into the more vulnerable bottom insulation.

With this end in view there is a need for a dense intermediate insulator, of a chemistry to resist bath attacks.

SKAMOLEX VIP-12 offers a perfect solution because it combines Vermiculite chemistry and good bath resistance with ample insulation and high strength.

Placed above the bottom insulation it will cause penetrating bath to stop and solidify, due to chemical reactions that transform the low-melting mixture of sodium fluoride and aluminium fluoride into a solid mixture of magnesium fluorides and silicates of sodium and aluminium (nephaline).

#### **Product Data**

SKAMOLEX VIP-12 is a Vermiculite based refractory block insulation of high bath resistance, characterized by good insulation value and very high mechanical strength.

Precision moulding ensures blocks of smooth, non-dusting surfaces and clean edges, and permits manufacture to close dimensional tolerances, i.e.  $\pm$  2.5 mm (0.10") on length and width, and  $\pm$  1.0 mm (0.04") on thickness.

#### **Block Sizes**

#### Metric:

1000 mm × 305 mm, Thicknesses: 30 - 40 - 50 mm 610 mm × 305 mm, Thicknesses: 25 - 30 - 40 - 50 - 60 - 75 mm

#### US/British:

are made to order

36" × 12",

Thicknesses:
1½" - 1½" - 2"
24" × 12",

Thicknesses:
1" - 1½" - 1½" - 2" - 2½" - 3"

Derivatives cut from standards



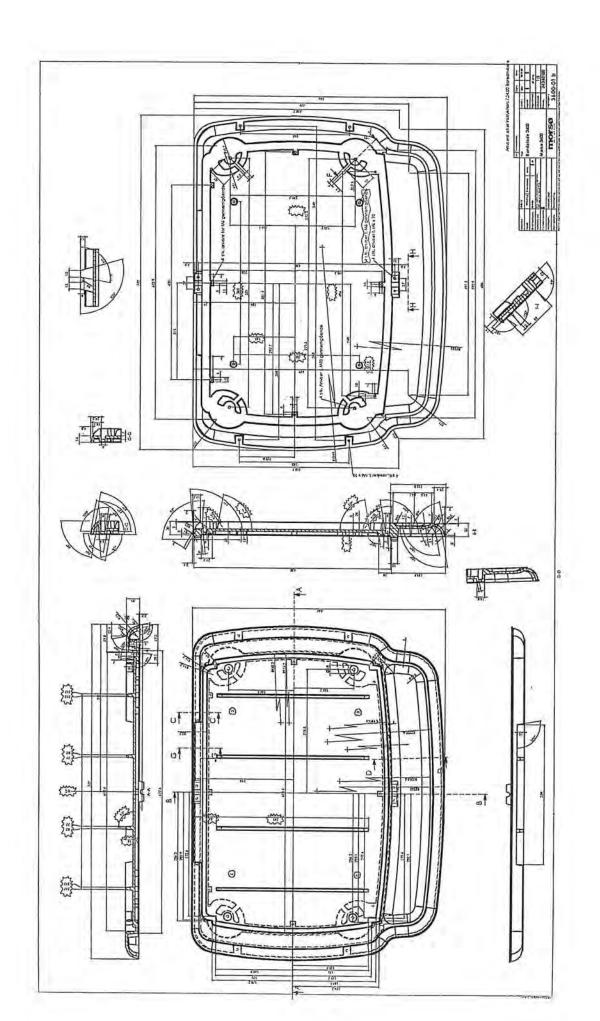
Skamol a/s · Ostergade 58-60 · DK-7900 Nykobing Mors · Tel.: +45 97 72 15 33 · Fax: +45 97 72 49 75
Technotherm GmbH & Co. KG. · Postfach 10 14 37 · D-41414 Neuss · Tel.: +49 2131 10 64 0 · Fax: +49 2131 10 64 64
Skamol a/s, UK Sales Office · Aden Mount · Thorrington · Essex CO7 8.J · Tel.: +44 1 (206) 302 330 · Fax: +44 1 (206) 304 576
Skamol Inc. · 2045 Niagara Falls Blvd. · Suite 16 · Niagara Falls · NY 14304 · Tel.: +1 (716) 298 4115 · Fax: +1 (716) 298 4118

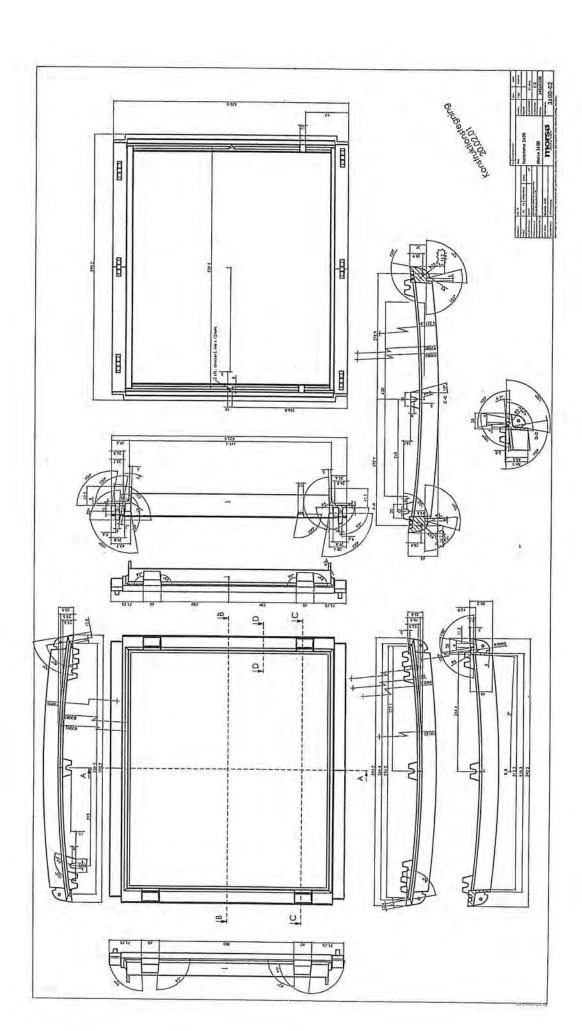
### SKAMOLEX VIP-12 Vermiculite Block Insulation

Chemical Analysis (typical)			
SiO <sub>2</sub>	48%	CaO	8%
Al <sub>2</sub> O <sub>3</sub> + TiO <sub>2</sub>	22%	Na <sub>2</sub> O	0.3%
Fe <sub>2</sub> O <sub>3</sub>	3.4%	K,ô	6%
MgO	9%	Loss on ignition (1025°C)	3.0%

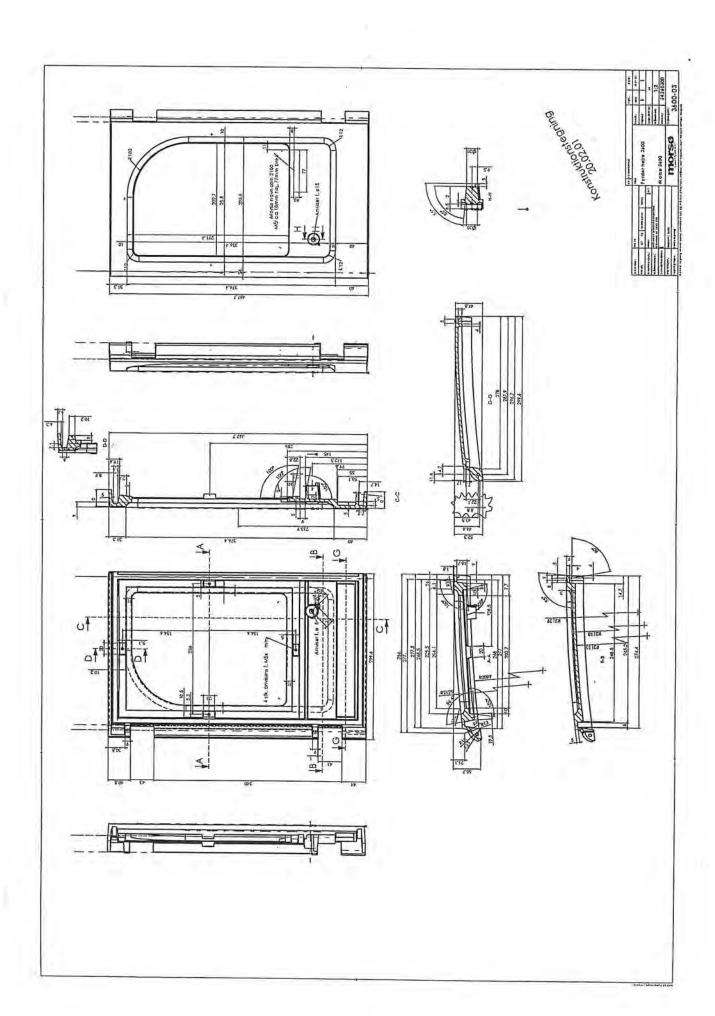
TECHNICAL PROPERTIES							
Max. service temp.	°C °F	1150 2102	Specific heat	kJ/(kg·K) BTU/(lb·°F)	0.9 0.22		
Bulk density, dry	kg/m³ lbs/cu.ft.	1200 75	Coefficient of reversible thermal expansion, 20°C-750°C (68°F-1382°F)	%F-1	14x10 <sup>-8</sup> 7.8x10 <sup>-8</sup>		
Compressive strength	MPa lbs/sq.in.	15.0 2175	Linear reheat shrinkage, 12 h at 1100°C (2012°F) (DIN 51067, Teil 2)	%	1.0		
Modulus of rupture	MPa lbs/sq.in.	3.0 435	Pyrometric cone equivalent	°C °F	1180 2156		
Total porosity Bath resistance (»Light Metals 1986«, pp. 501-514) Cryolite Attack Ratio (k Material Factor (m)	%	1.27 1.03	Thermal conductivity at mean temp. (ASTM C-201 supplemented by ASTM C-182)	200°C 400°C 600°C 800°C BTU/(si 392°F 752°F 1112°F 1472°F	W/(m·K) 0.23 0.26 0.29 0.32 q.ft.·h·°F/in 1.59 1.80 2.01 2.22		

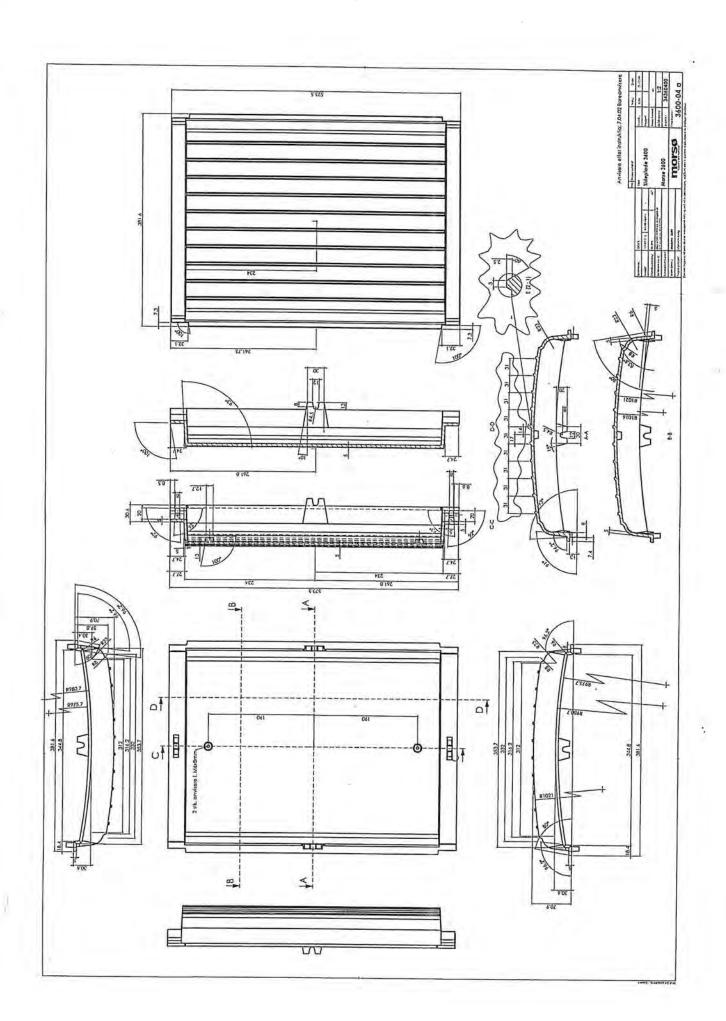
The physical and chemical properties represent typical average values obtained in accordance with accepted test methods and are 'subject to normal manufacturing variations. They are supplied as a technical service and are subject to change without notice.

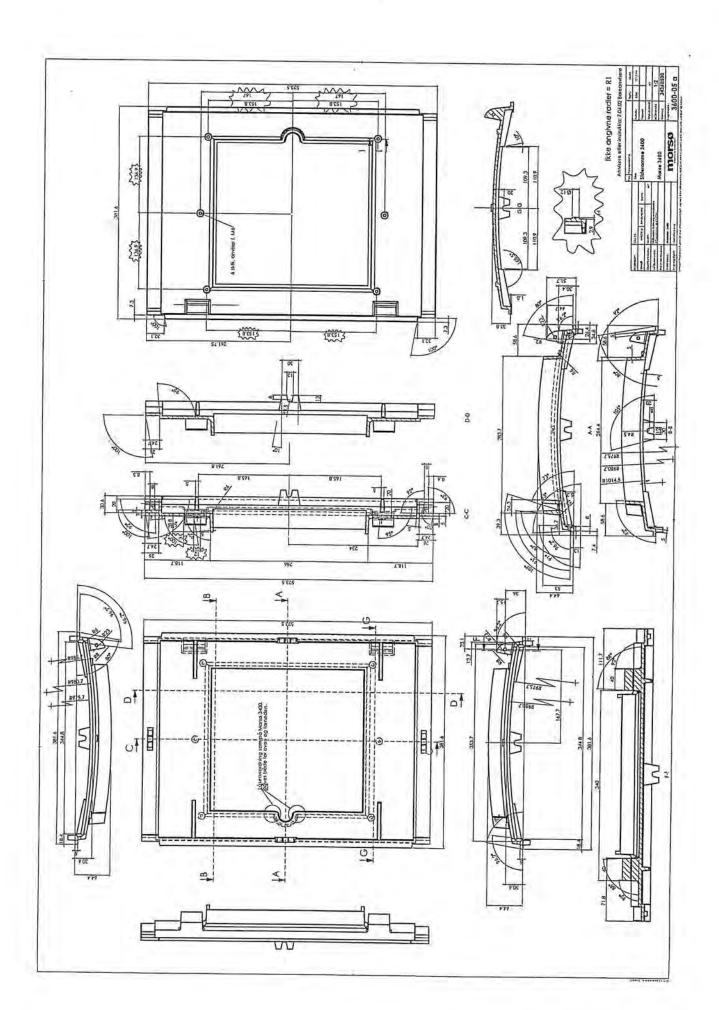


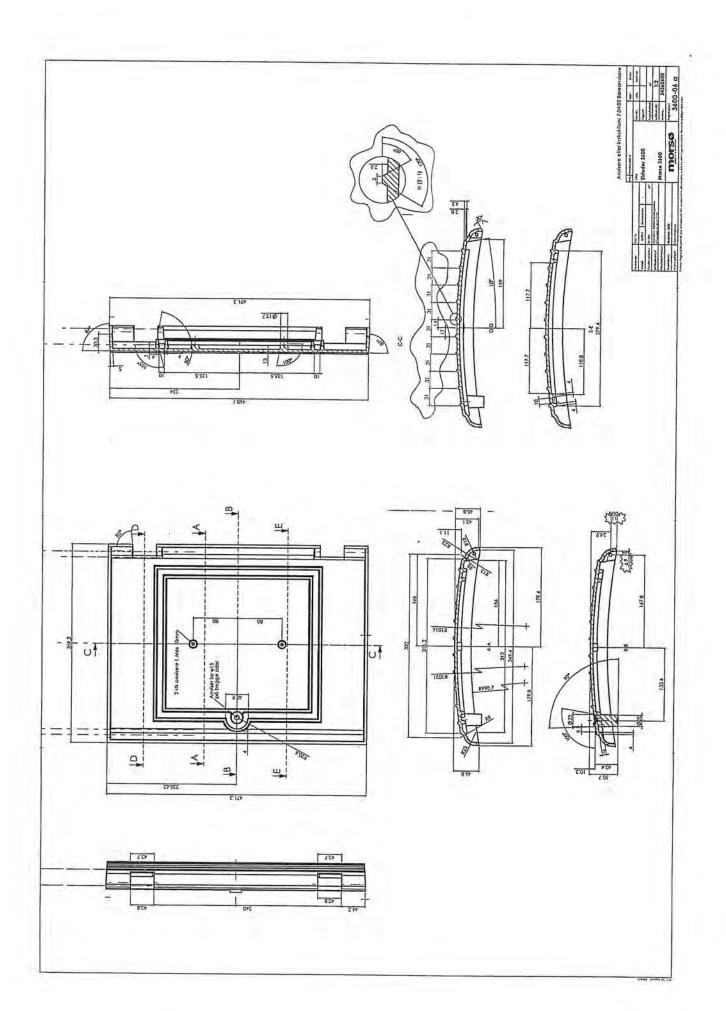


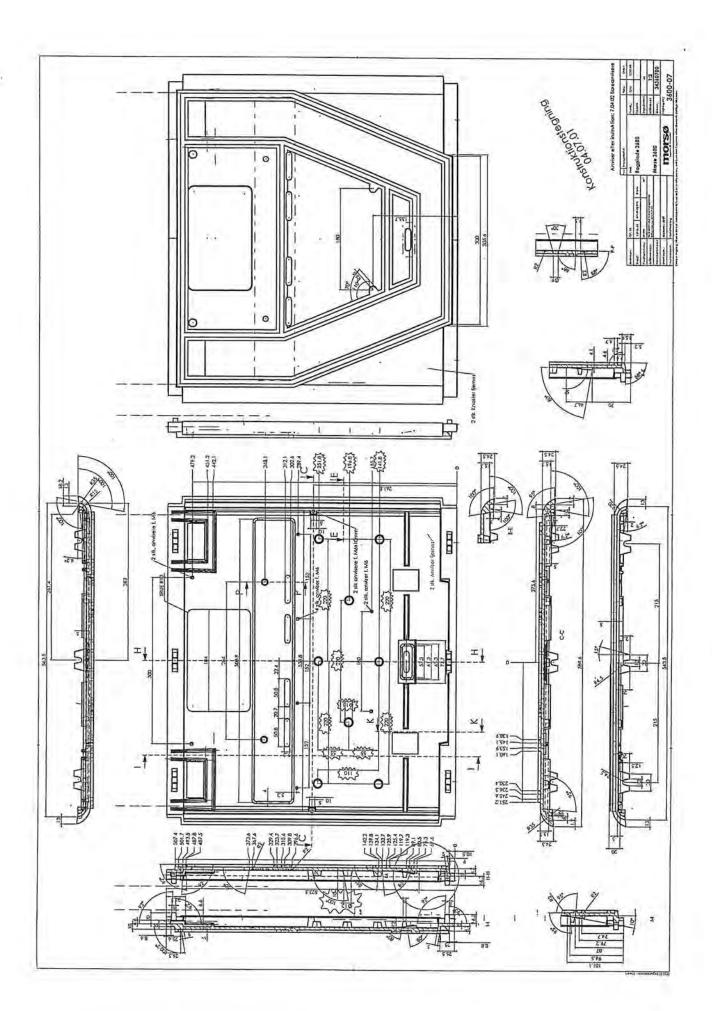
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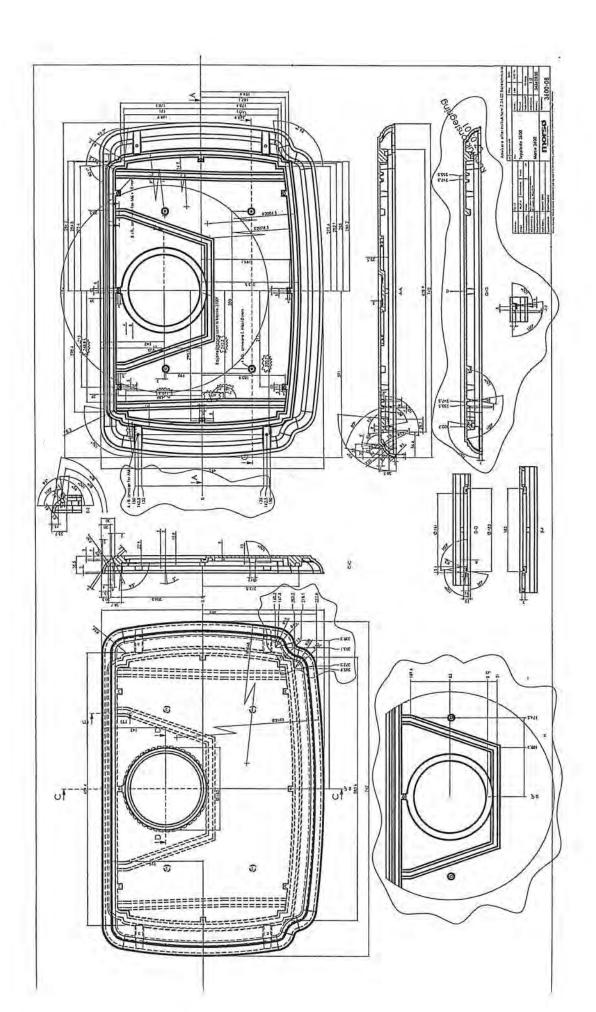




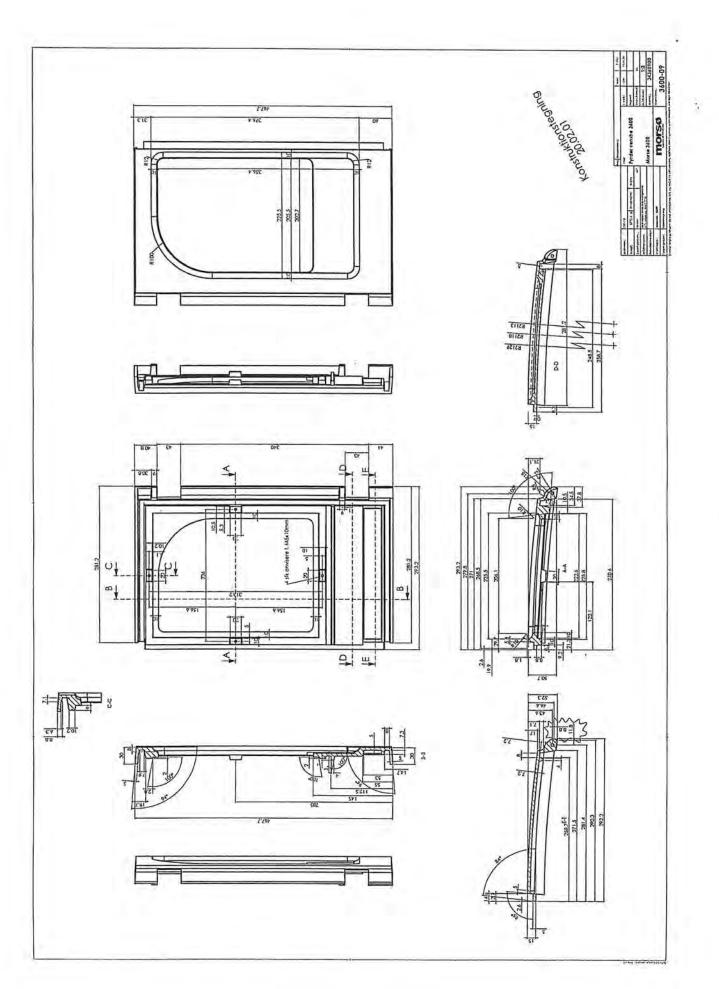


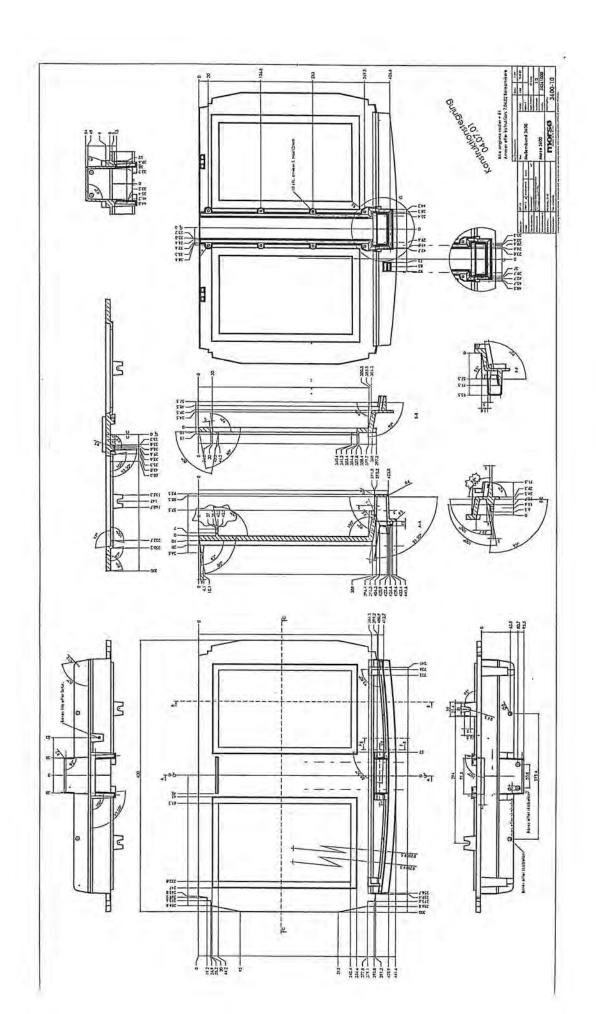




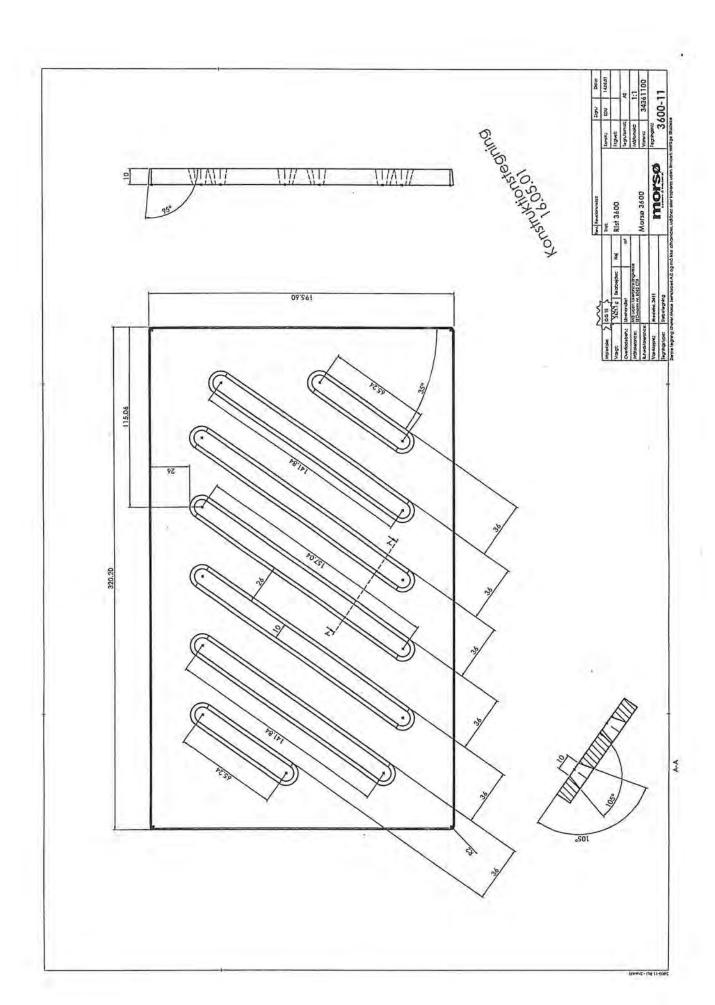


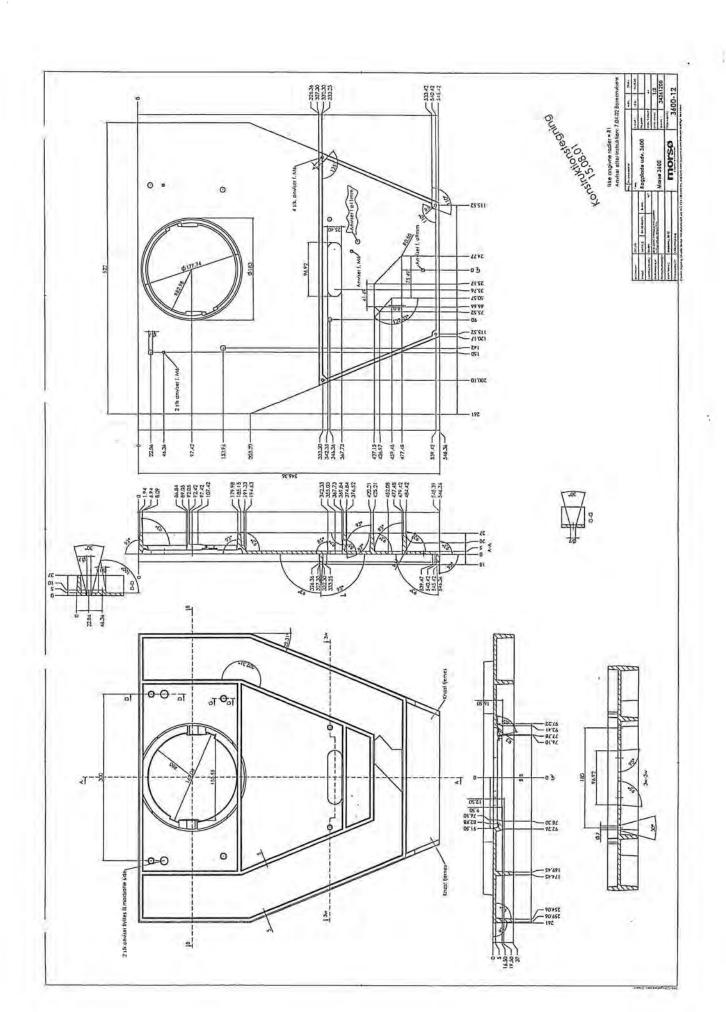
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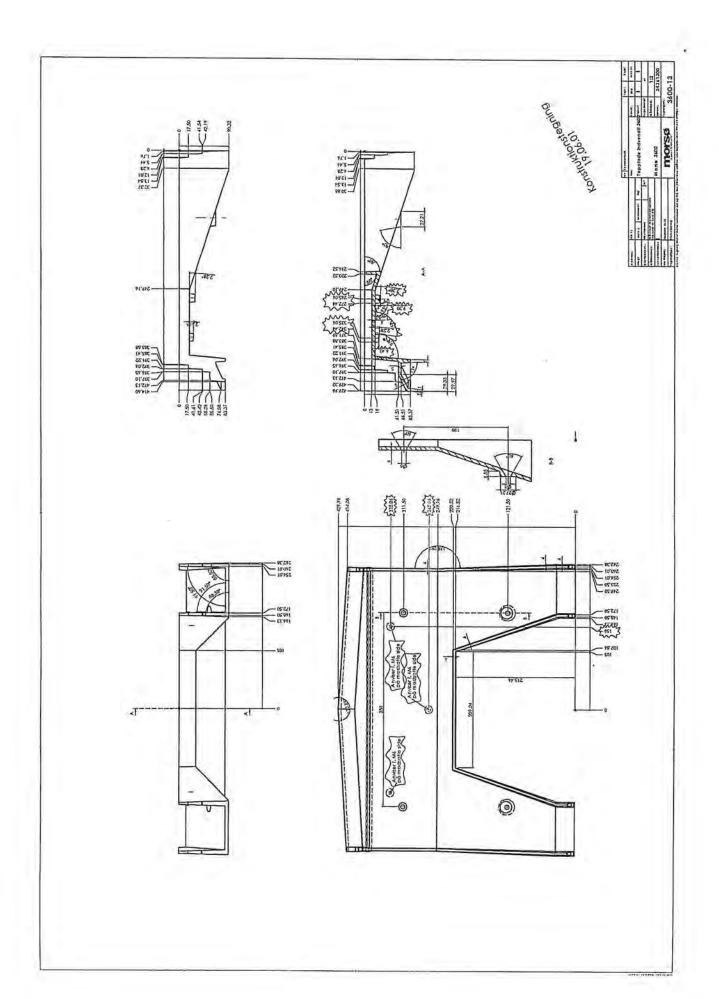


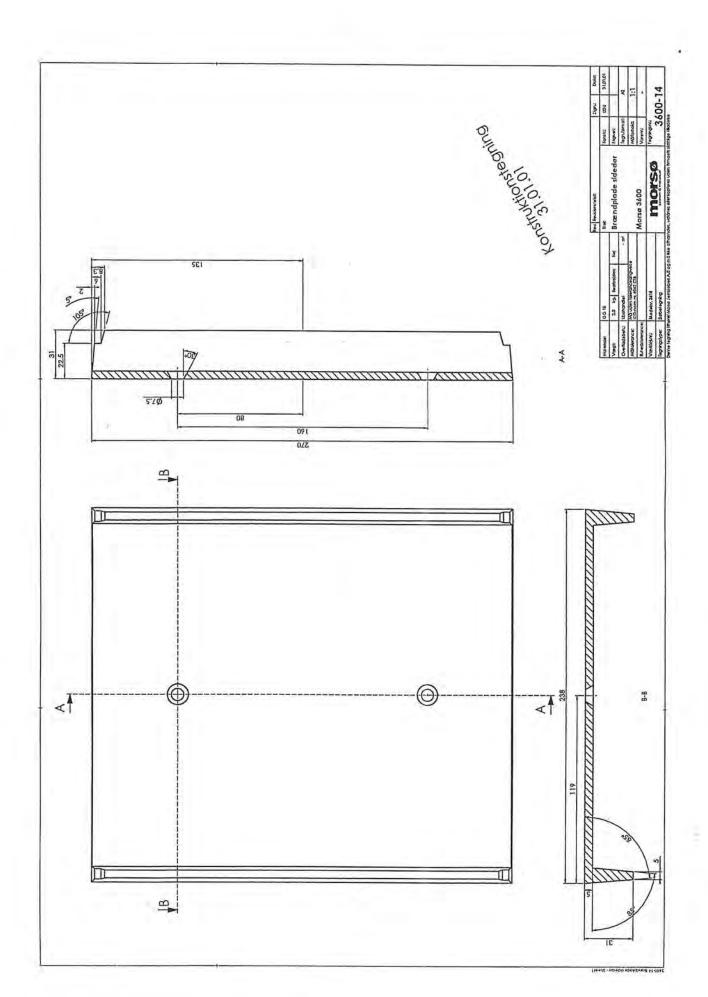


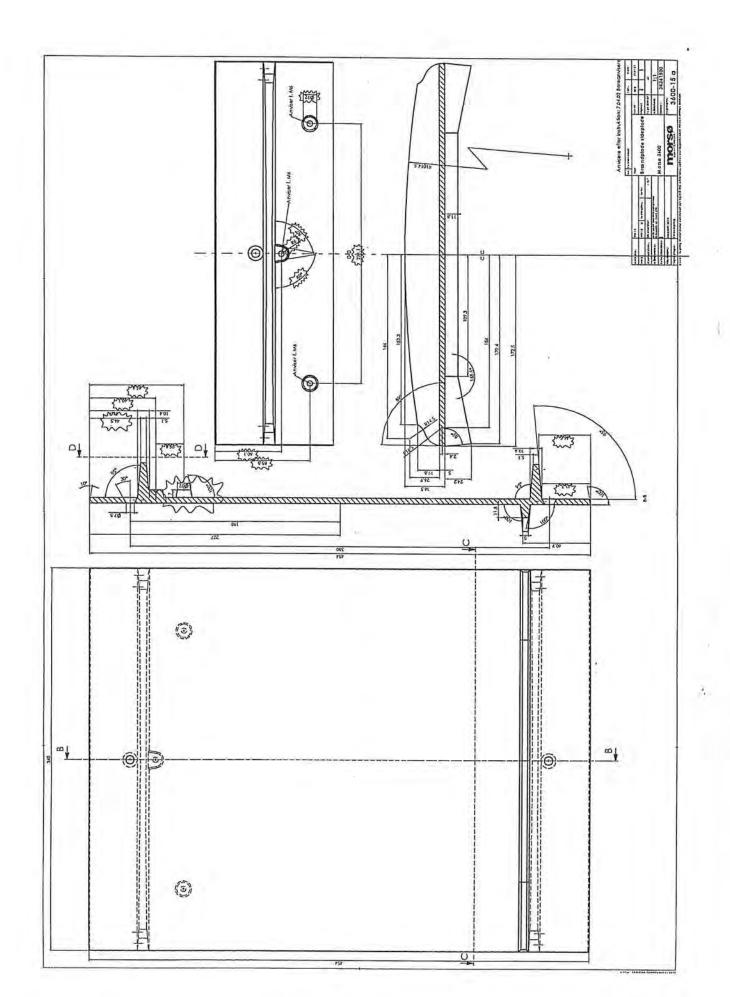
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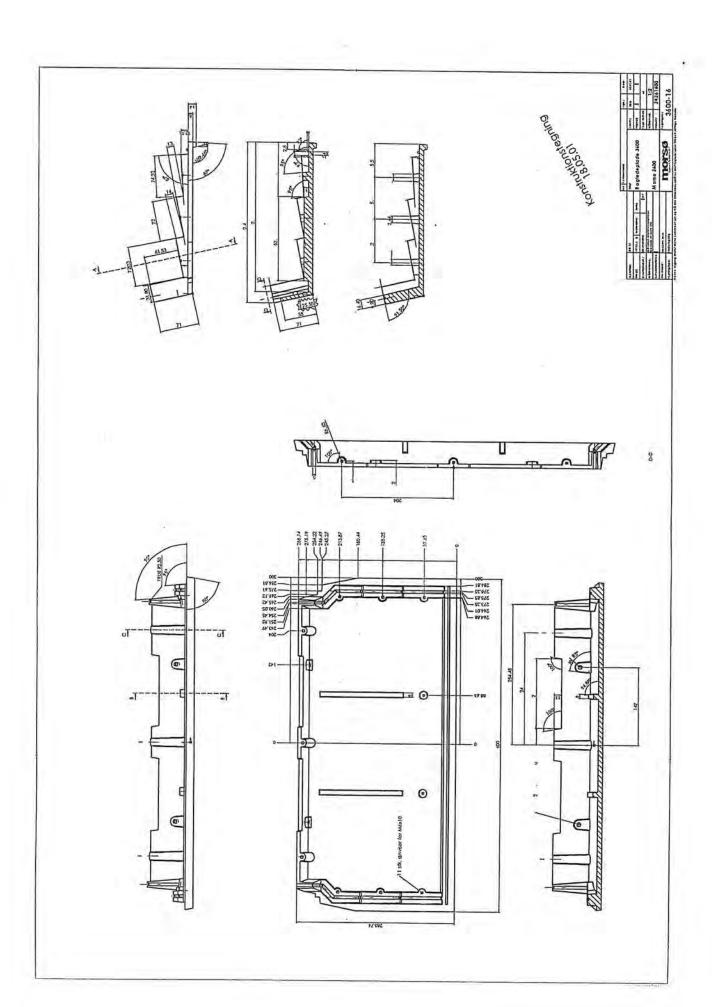


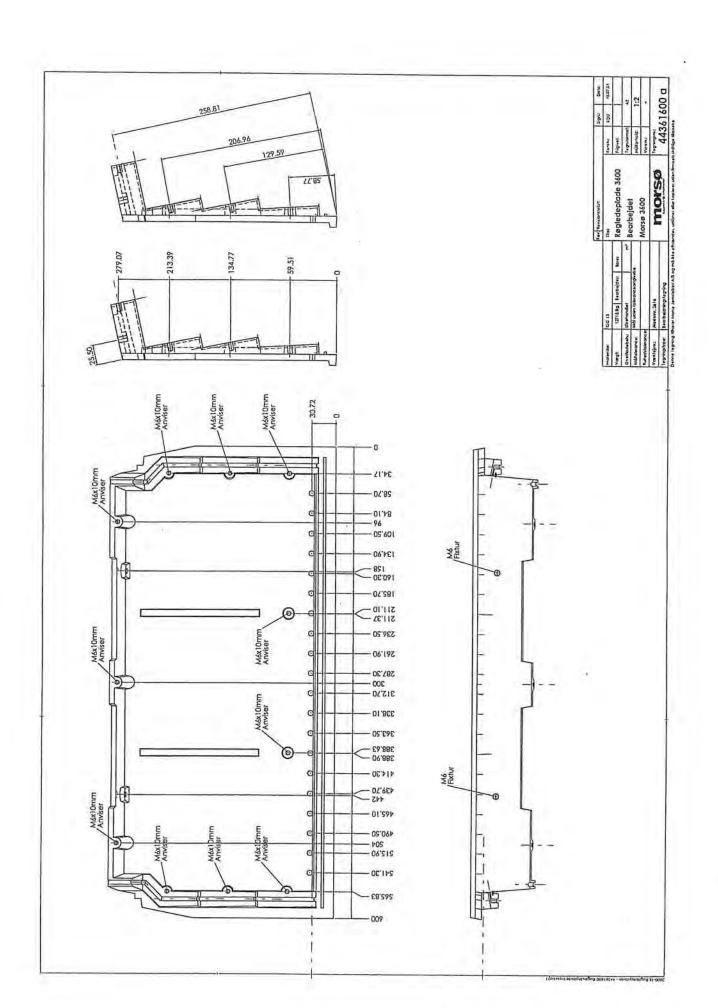


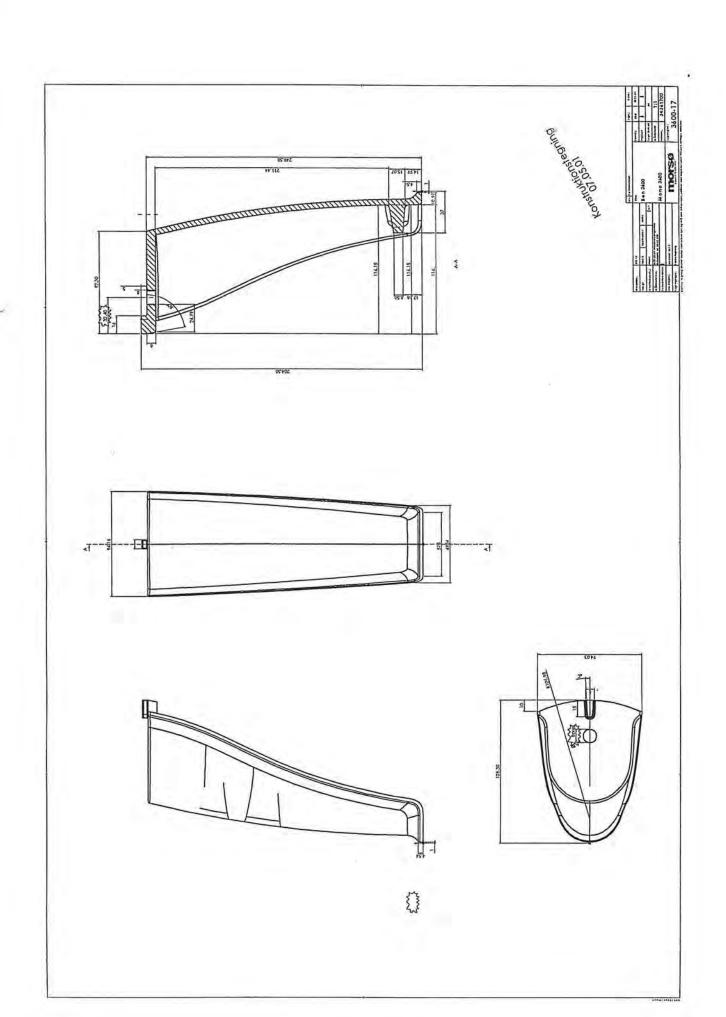


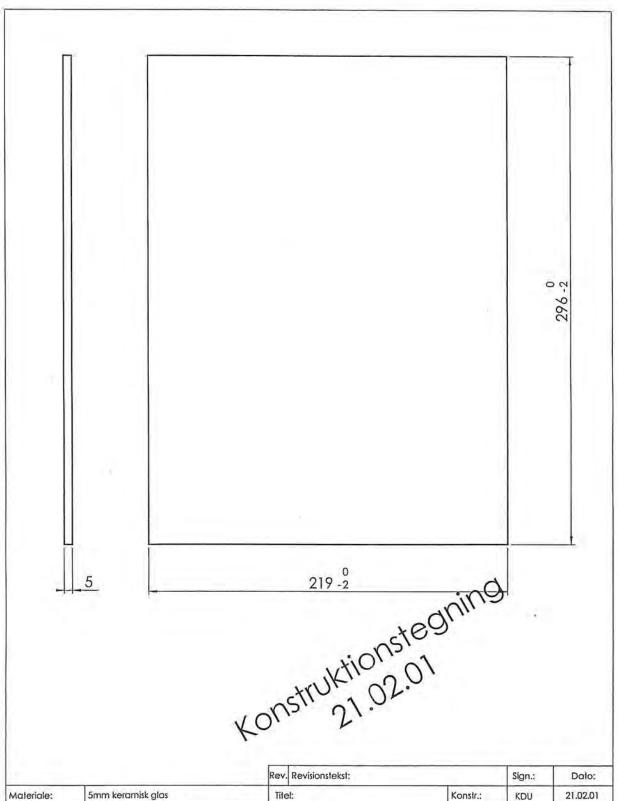




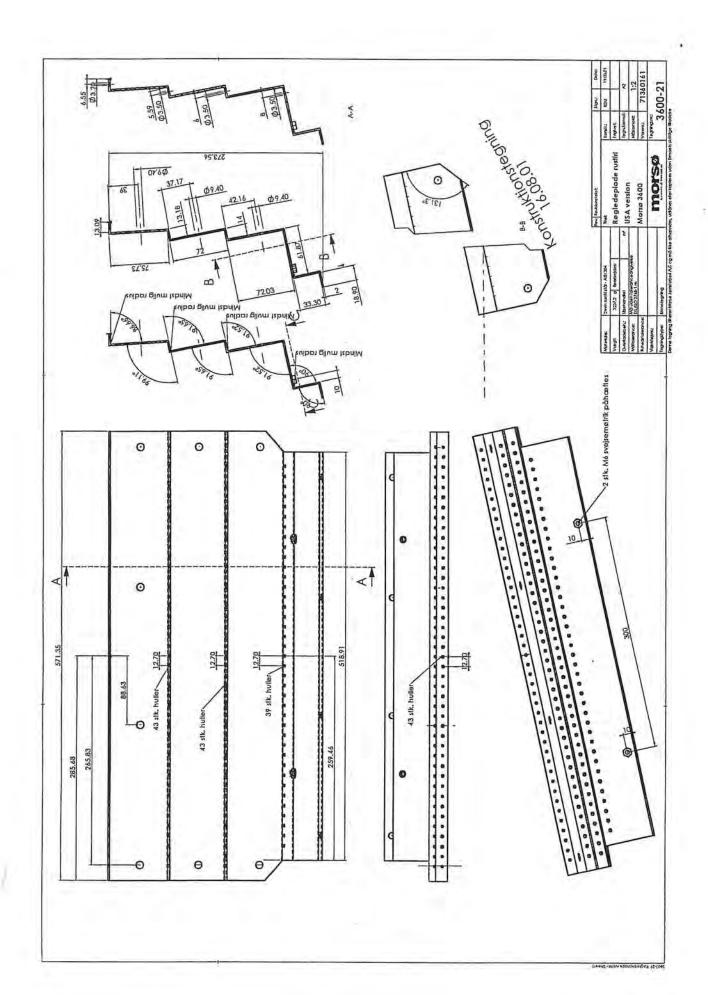


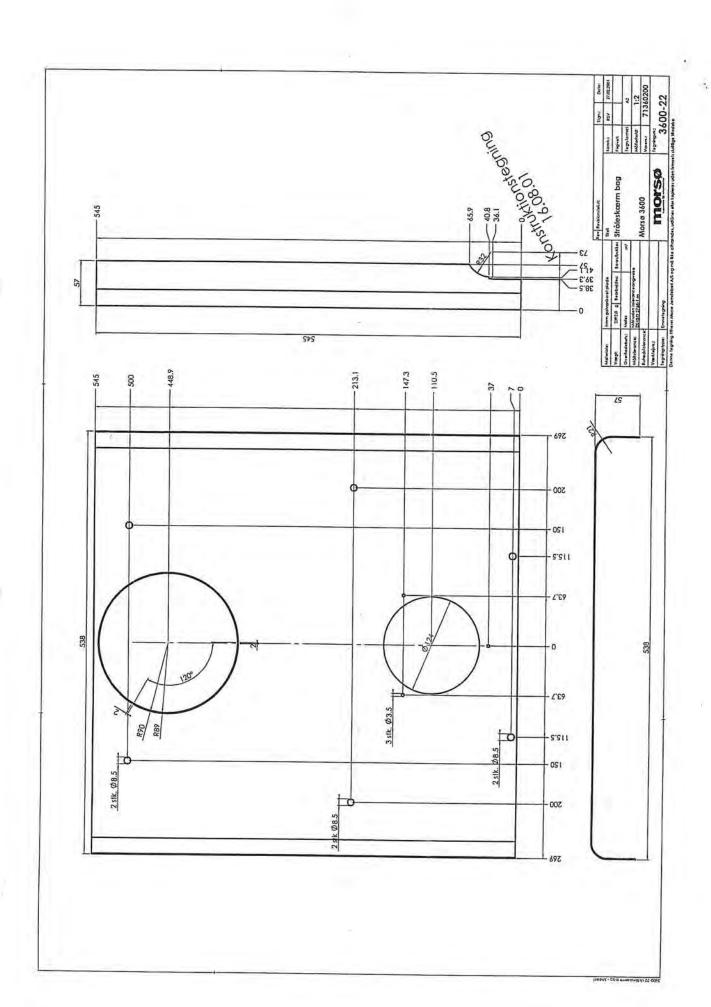


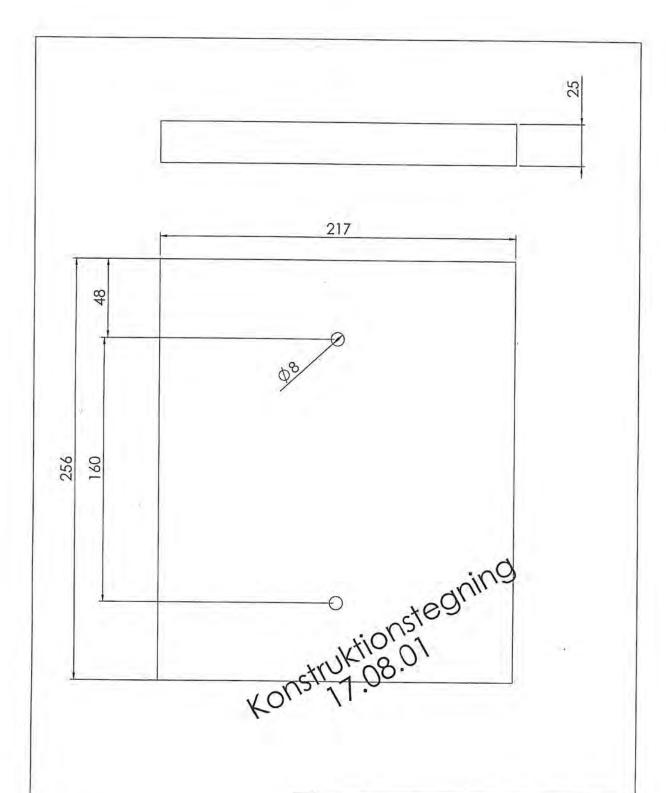




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Materiale:	eriale: 5mm keramisk glas			Titel:	Konstr.:	KDU	21.02.01
Vægt:	813.5 g	Bearbejdes:		Glas 3600	Frigivet:		
Overfladebeh.:			m²		Tegn.format:	A4	
Overfladebeh.: Måltolerance:	Se teaning				Målforhold:	Målforhold: 1:2  Varenr.: 79360000	
Ruhedstolerance:			Morsø 3600	Varenr.:			
Værktøjsnr.:	Emnelegning		morsø	Tegningsnr.:			
Tegningstype:			Diabaconto () seleta Data Cont	36	3600-20		

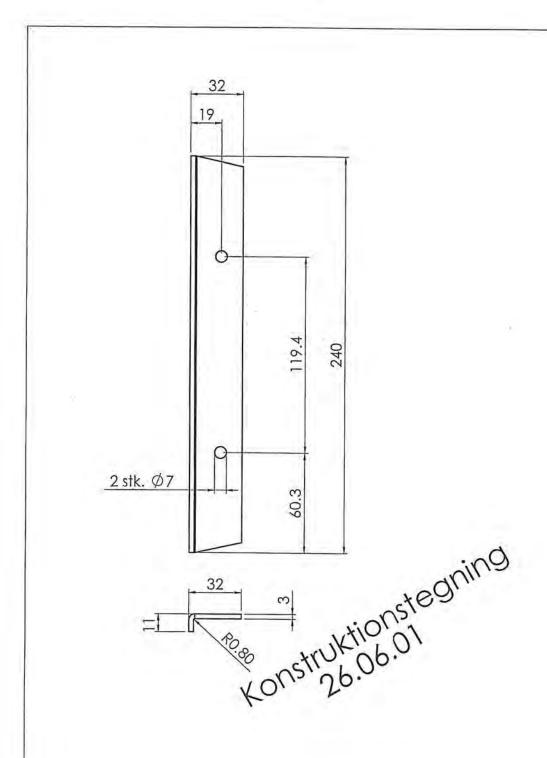




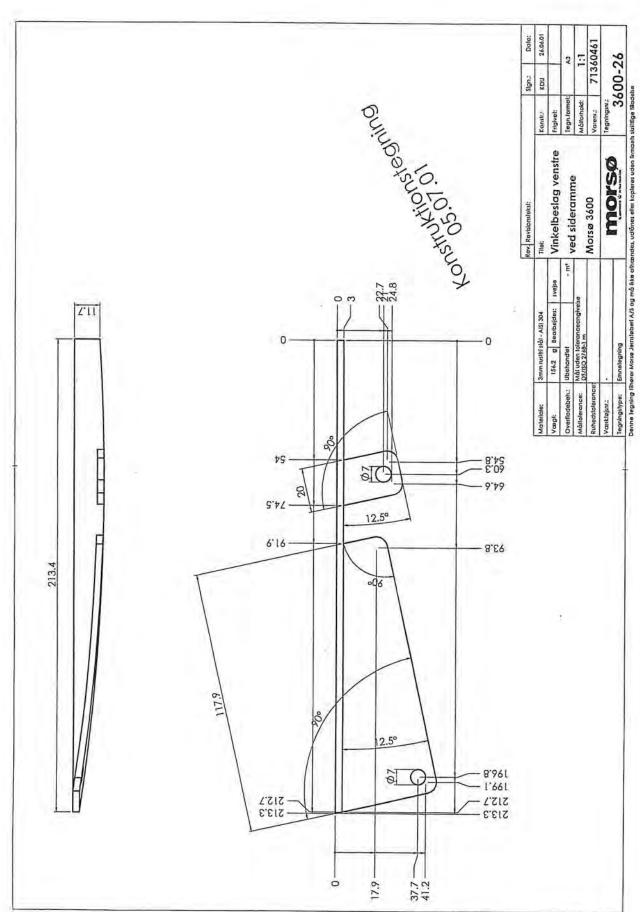


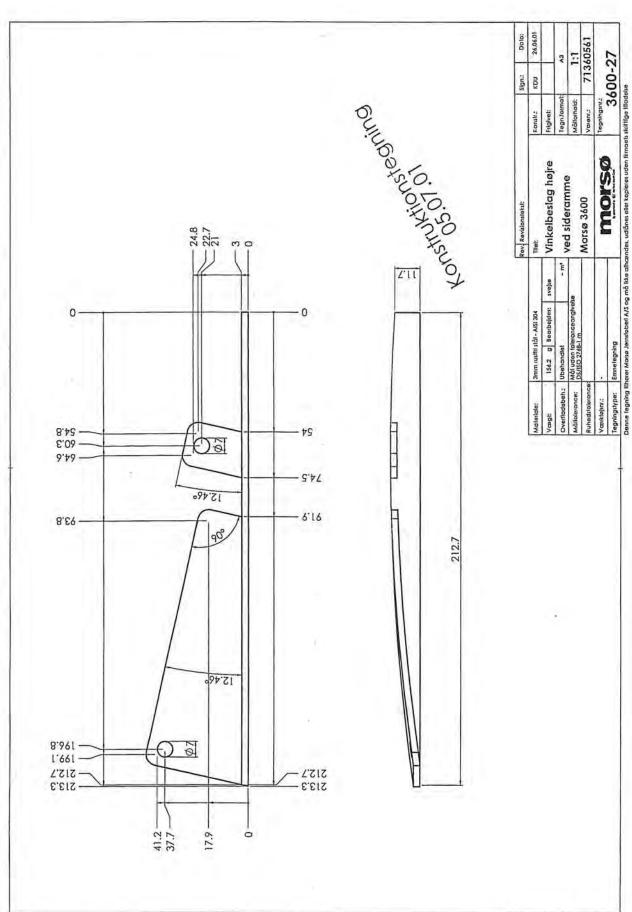
				Rev. Revisionstekst:		Sign.:	Dato:
Materiale:	ateriale: 25mm Isoleringsmåtte		Titel:	Konstr.:	KDU	05.07.01	
Vægt:	- 9	Bearbejdes:	Nej	Isoleringsmåtte sidedør	Frigivet:		
Overfladebeh.:	Ubehandlet		- m²		Tegn.format:	A4	
Måltolerance:	Se tegning				Målforhold:	1:2	
Ruhedstolerance:			Morsø 3600	Varenr.:	79074900		
Værktøjsnr.:	- Emnetegning			morsø	Tegningsnr.: 3600-23		
Tegningstype:				By accomment to the ne flow of seast Court			23

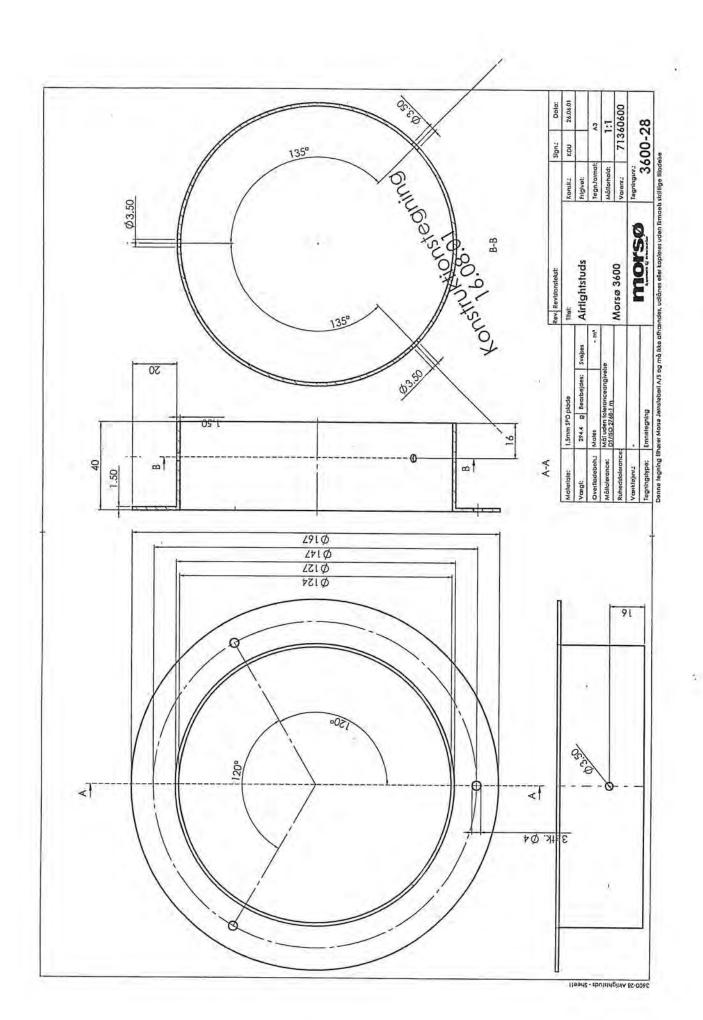
					25	107
			205			1
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		to	nstruktionstegn	ing		300
	I a constant		Rev. Revisionstekst:		Sign.:	Dato:
	25mm Isoleringsmåtte		Tifel:	Konstr.:	KDU	05.07.0
	The state of the s	No	lsoleringsmåtte sideplad	dicionivet:		
egt:	- g Bearbejdes:	Nej	isolelingsmalle sidepide			
egt: verfladebeh.:	Ubehandlet	- m²	isolenngsmalle slaeplad	Tegn.format:		A4
egt: verfladebeh.: bitolerance:	Ubehandlet Se tegning					:2.5
ateriale:  ægt:  verfladebeh,:  åltolerance:	Ubehandlet Se tegning		Morsø 3600	Tegn.format:		

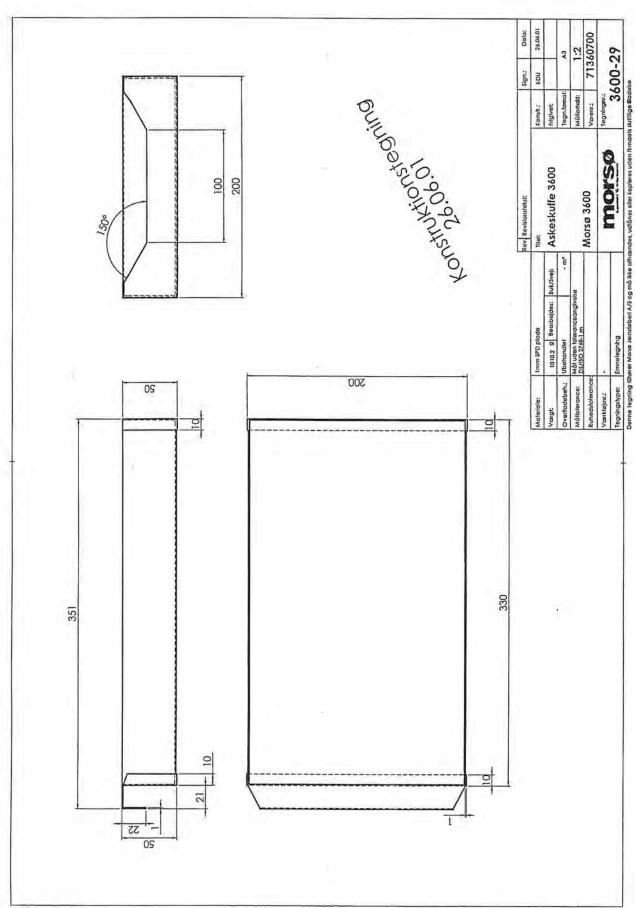


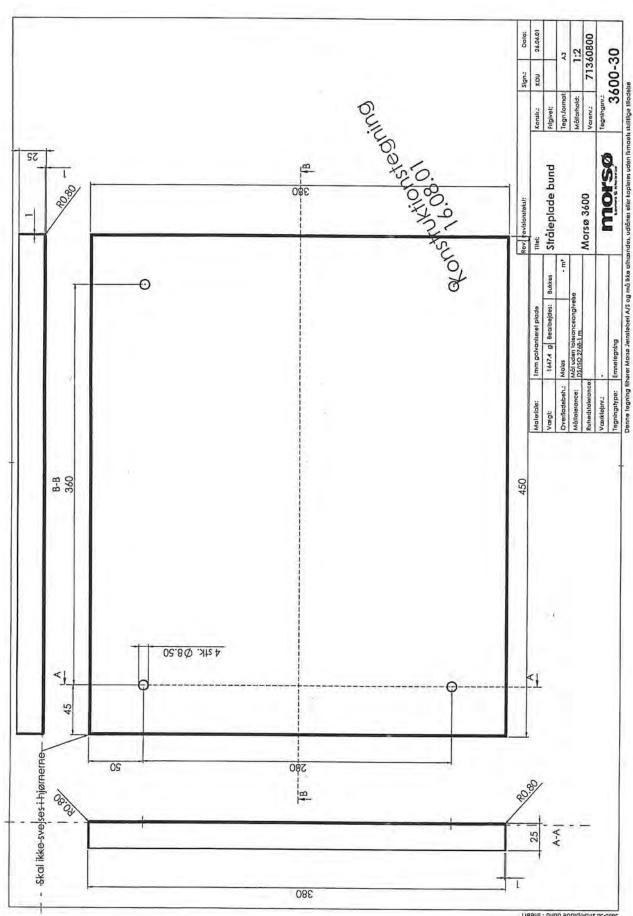
				Rev. Revisionstekst:		Sign.:	Dato:
Materiale:	3mm rustfri :	stál - AISI 304		Titel:	Konstr.:	KDU	26.06.01
Vægt:	214.8 g	Bearbejdes:	Buk/bor	Vinkelbeslag røgledepl.	Frigivet:		
Overfladebeh.:	Ubehandlet - m² Mål uden toleranceangivelse DS/ISO 2768-1 m		- m²	ved brændplade	Tegn.format:		
Måltolerance:			lse		Målforhold:		
Ruhedstolerance:				Morsø 3600	Varenr.:	713	60361
Værktøjsnr.:	- Emnetegning			morsø	Tegningsnr.:		775
Tegningstype:				By expansional to all the Polys Carab Coun	3600-25		



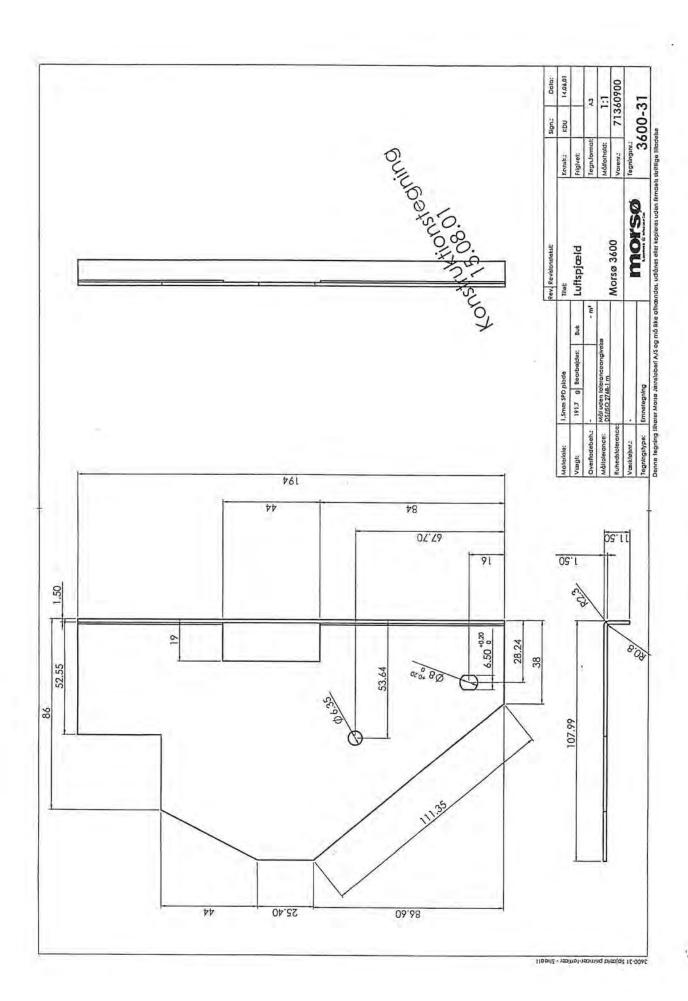


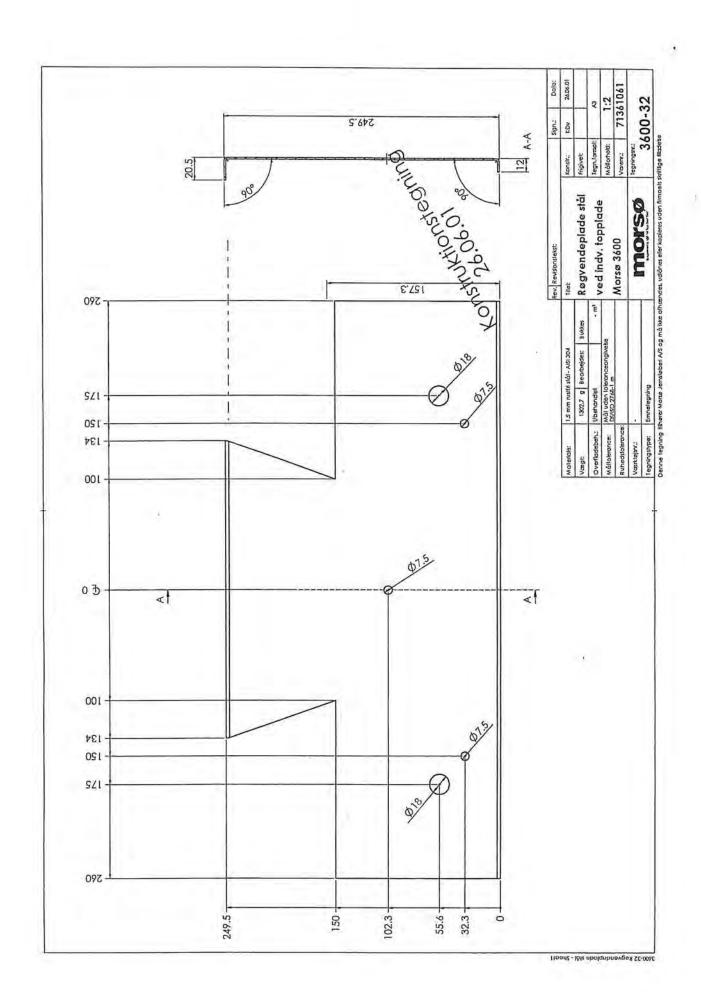


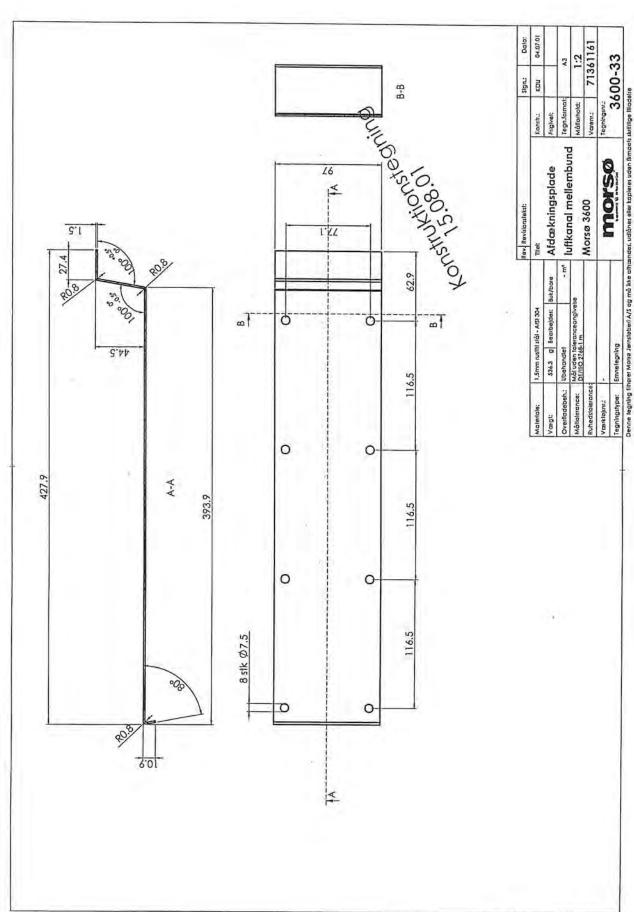


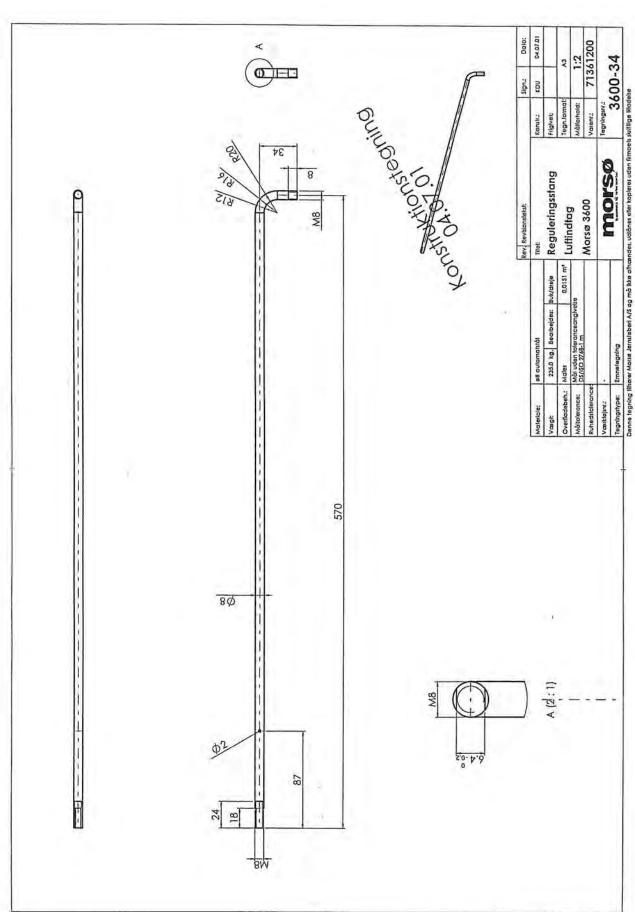


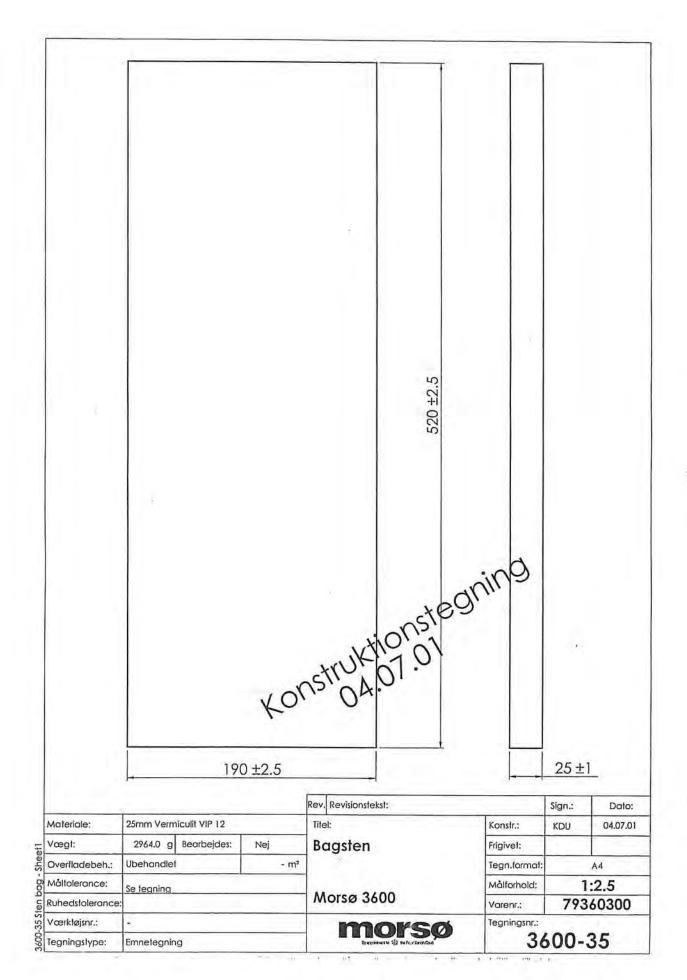
3600-30 Struleplade bund - Sheet I





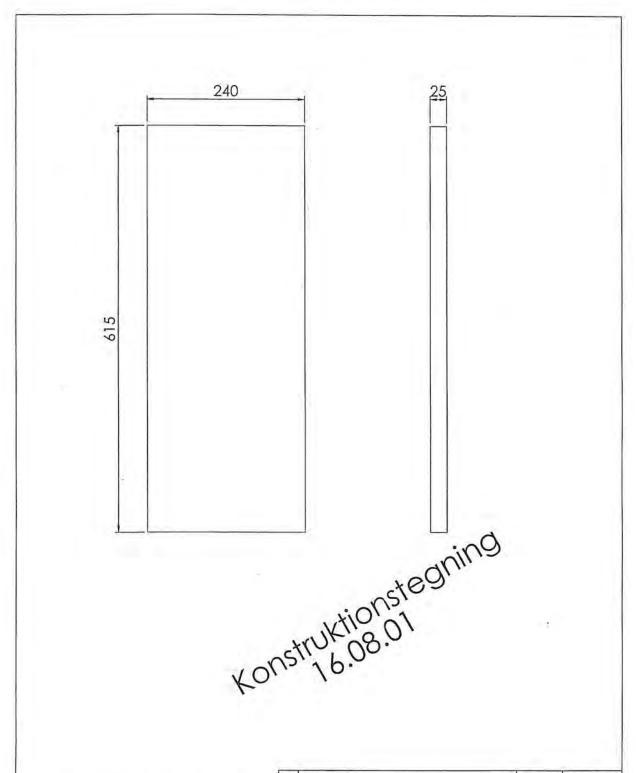




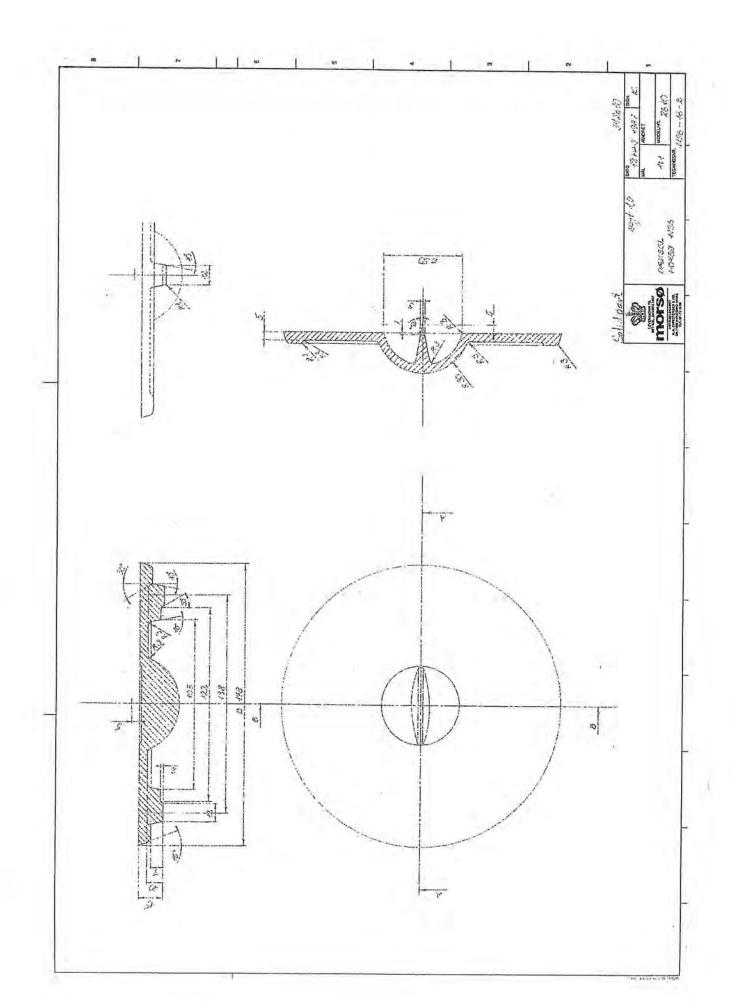


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			Rev. Revisionstekst:		Sign.:	Dato:
Materiale:	1,5mm rustfri stål - AISI 304		Titel:	Konstr.:	KDU	04.07.01
Vægt:	182.9 g Bearbejdes:	bores	Holder for bagsten	Frigivet:		
Overfladebeh.:	Ubehandlet	- m²	*	Tegn.format:	A4	
Måltolerance:	Mål uden toleranceangivelse DS/ISO 2768-1 m			Målforhold:		1:2
Ruhedstolerance:			Morsø 3600	Varenr.:	713	61361
Værktøjsnr.:	- Emnelegning		morsø	Tegningsnr.:		
Tegningstype:			By apprison a to High the Royal Daniel Court	36	600-36	



		3		Rev	. Revisionstekst:		Sign.:	Dato:
Materiale:	25 mm Isoleringsmåtte		Tite	el:	Konstr.:	KDU	11.07.01	
Vægt:	- kg.	Bearbejdes:	- 1-	Is	oleringsmåtte 3600 US	Arigivet:		
Overfladebeh.:	-	CHINE	- m²			Tegn.format:	A4	
Måltolerance:	: Mål uden toleranceangivelse			] .	A Company of the Comp	Målforhold:		1:5
Ruhedslolerance:				Morsø 3600	lorsø 3600	Varenr.:	79074800	
Værktøjsnr.:	- Emnetegning			morsø	Tegningsnr.:			
Tegningstype:				Openious to all telling brantous	36	3600-37		

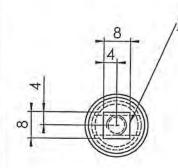


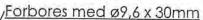
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0,5x45° 20° R 0,5	1410
0.5x45° 1 20° R 0.5	1B 2B 1126 '-
EDB nr. 541082	1610

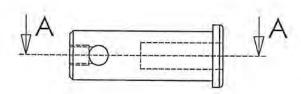
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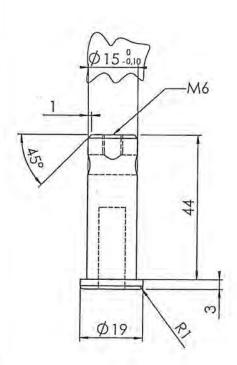
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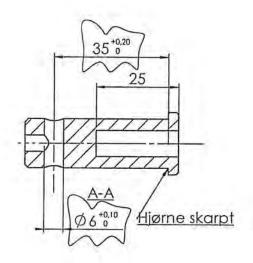
Titel:	Sign.: N.Aa.	Dato: 06.10.87	Revision	Sign.	Dato
Ø6 hængselstifter	Tegn.form.:	Målforhold	Gamdrup TegneTeknik	нсн	April 96
	A4	1:1	Tilføjet grader	KD	20.12.96
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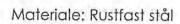


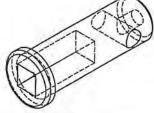




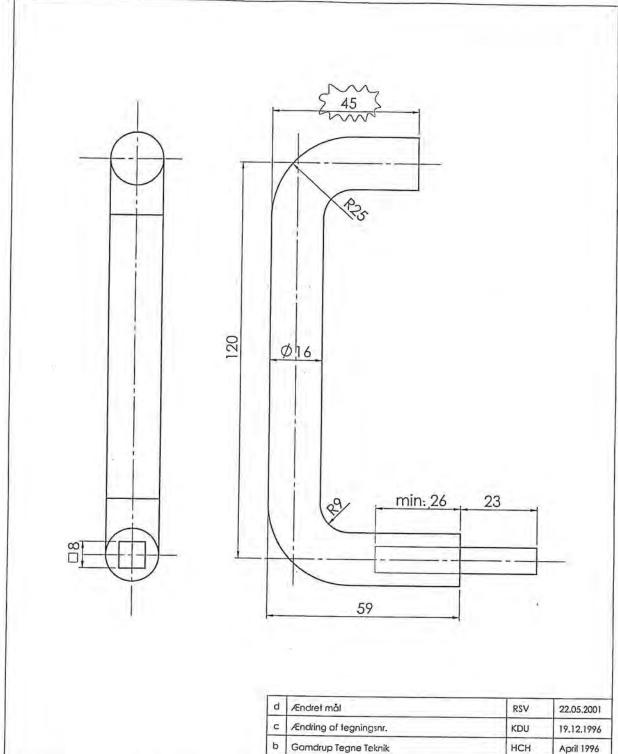








g	Tolerancer tilføjet	KDL	11.10.99		<i>y</i>		
f	Notater tilføjet	KDU	07.09.99	Titel:	Sign.:	Dato:	
е	Fjerne M4 - fiksering	KDU	07.09.99	Døraksel 1126	N.Aa Tegn.format:	03.12.87	
d	Tilføje M4m - fiksering	KAA	16.09.97		A4	Målforhold: 1:1	
С	Tilføje målsætning	KDU	20.12.96	Filnavn: 1126/1126-44.drw	Varenummer: 752627		
b	Gamdrup Tegneteknik	HCH	April 96	1120/1120-44.GIW			
Rev.		Sign.:		morsø Jernsløberi A/S	Tegningsnumm 1126	er: -44 g	



Materiale: Rustfast stål

Vægt: 317 g Bearbejdes: m²

Overfladebeh.: m²

Mål uden toleranceangivelse DS/ISO 2768-1 m

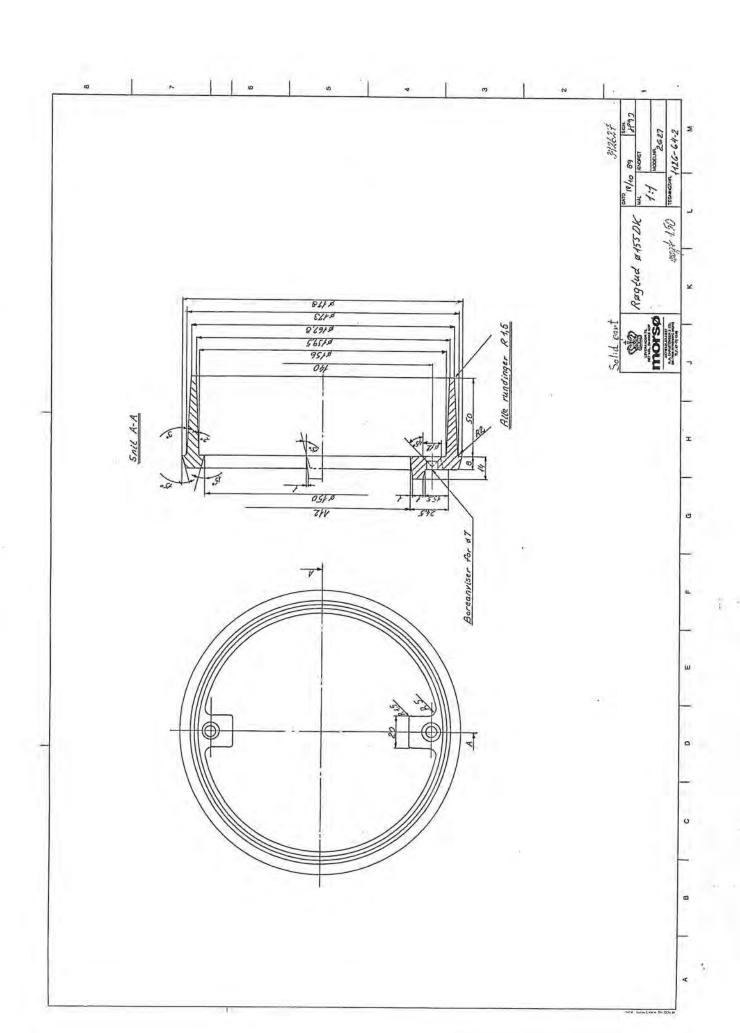
Ruhedstolerance: Værktøjsnr.:

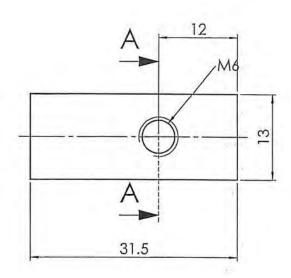
Tegningstype: Emnetegning

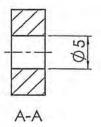
Gamdrup Tegne Teknik HCH Revisionstekst: Sign.: Dalo: Titel: Konstr.: N,Aa 14.10.87 1126 dørhåndtag Frigivet: Tegn.format: A4 Målforhold: 1:1 Morsø 1126 752625 Varenr.:

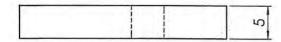
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Materiale:	Sort fladjern			
Vægt:	0,015 kg.	Bearbejdes:		]
Overfladebeh.:			m²	1
Måltolerance:	Mal uden to DS/ISO 2768	leranceangivelse -1 m		
Ruhedstolerance	:			1
Værktøjsnr.:				
Tegningstype:	Emnetegnin	9		1

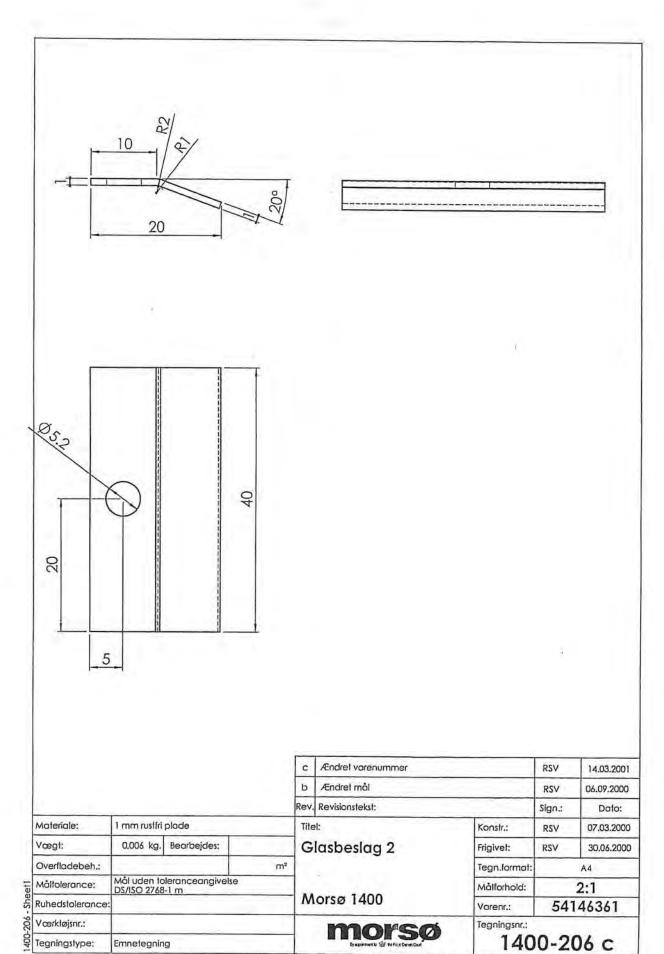
Rev. Revisionstekst:
Titel:
Lus med gevind
Morsø 1400

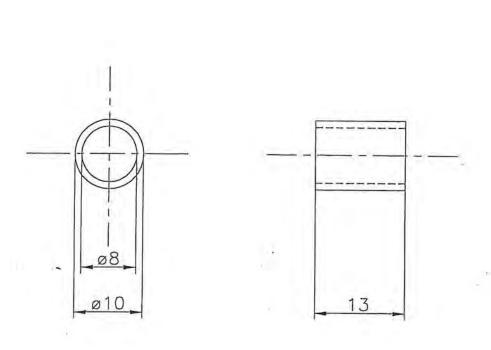
MOFSØ

Byggsdrivin 927 te Royclin th Cast

	Sign.:	Dato:
Konstr.:	RSV	03.03.2000
Frigivet:		
Tegn.format:		A4
Målforhold:		2:1
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Tegningsnr.:		

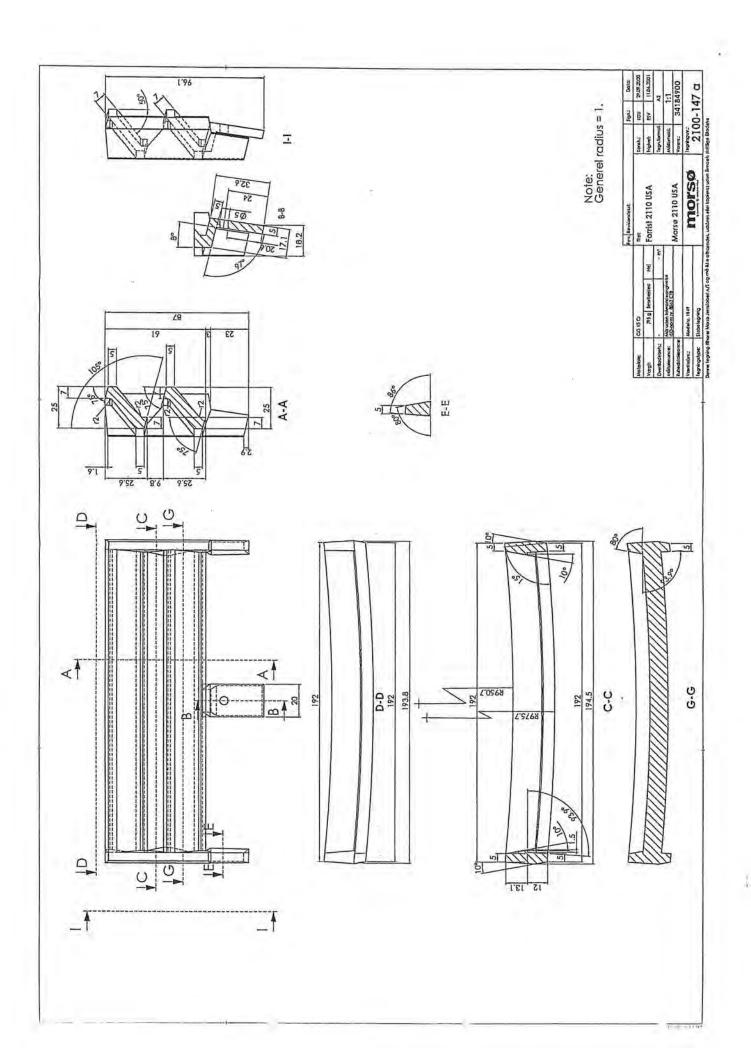
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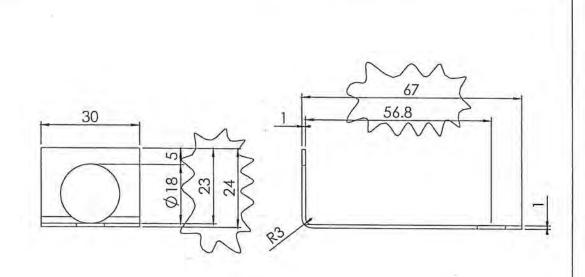


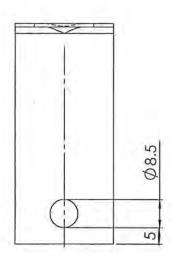


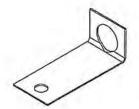
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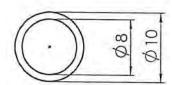


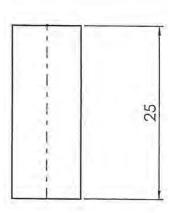




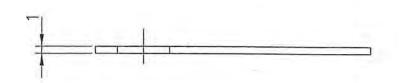


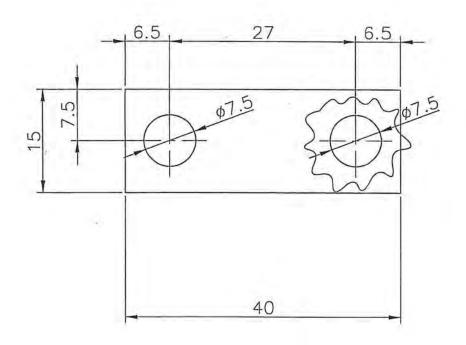
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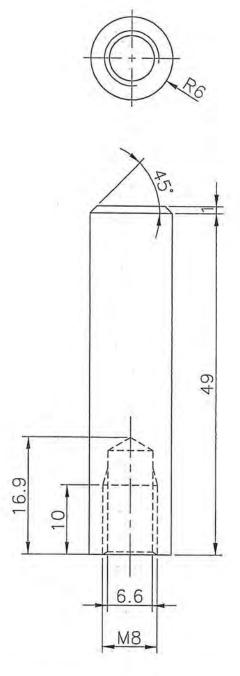


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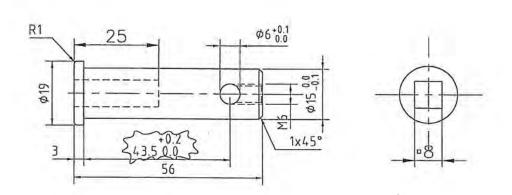


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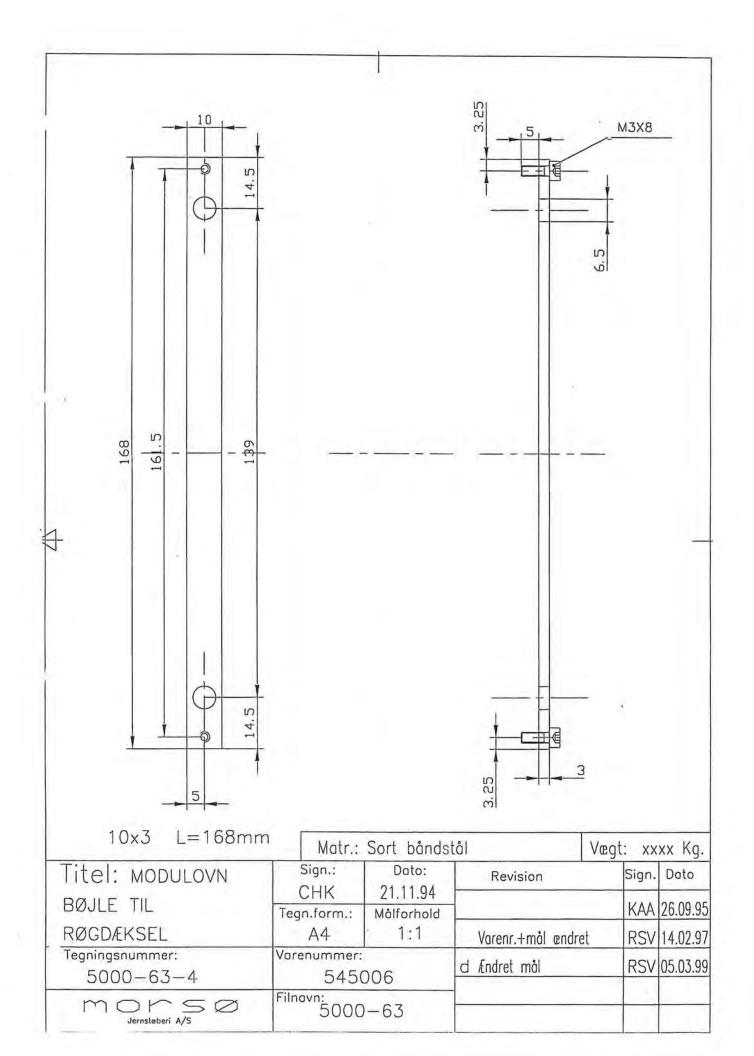
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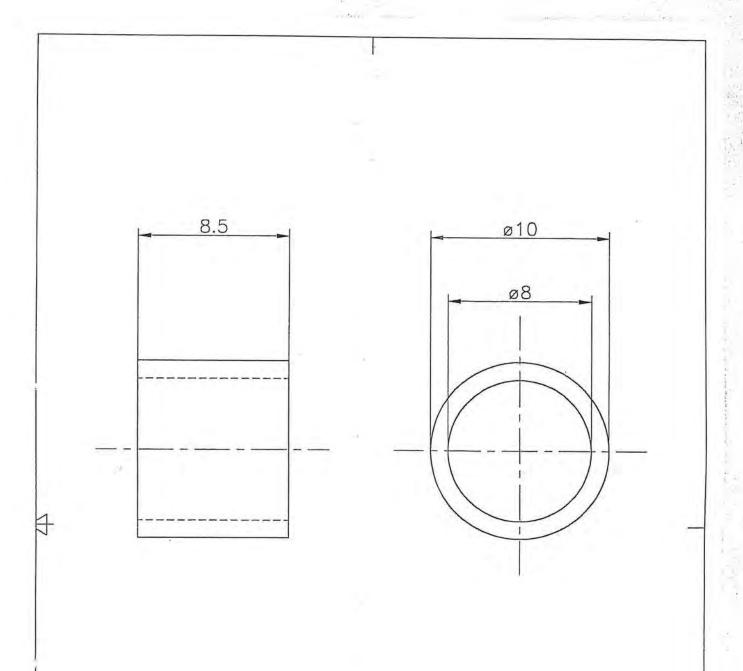
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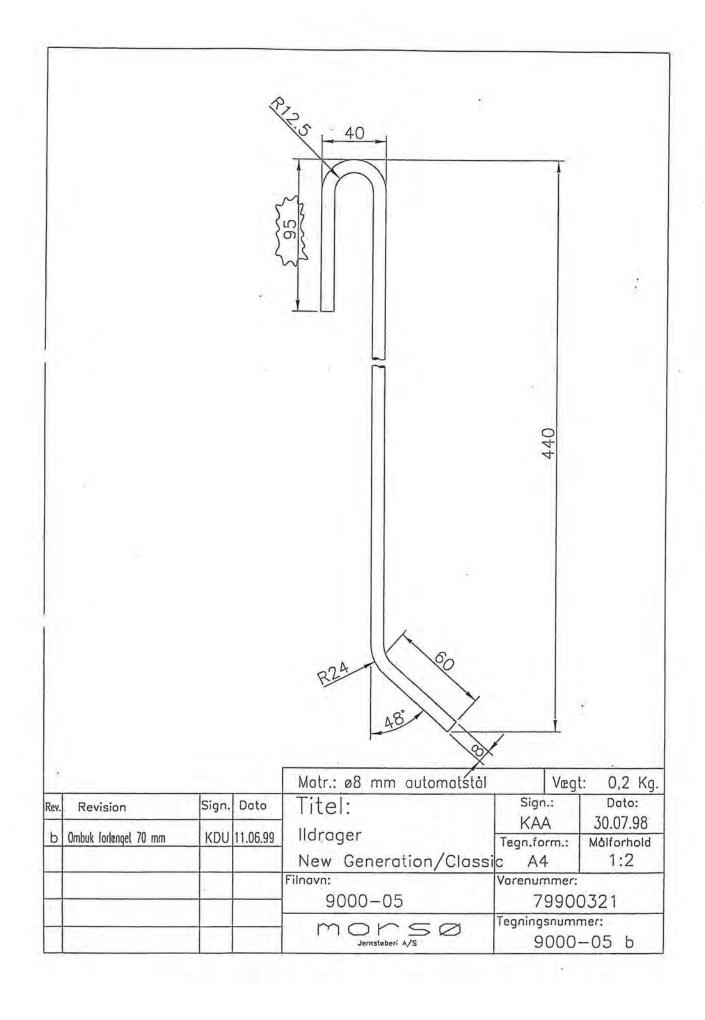
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# Ø10x1 Hydraulikrør galv.

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Jernstaberi A/S	Filnavn: 5000	)-64			



# APPENDIX G

# Ferguson, Andors & Company

P.O.Box 678, South Royalton, VT 05068 • 802-763-2339 (Voice and Facsimile)

August 1, 2001

Mr. Bill Keen Intertek Testing Services 8431 Murphy Drive Middleton, WI 53562

Dear Bill:

As you know, we will be representing Morsø Jernstøberi A/S during the upcoming EPA certification testing of their new Model 3600 non-catalytic woodstove. This product does not have a fan either as standard or optional equipment.

We would like to provide the following information regarding operating procedures and air settings that will be helpful in obtaining the required burn rate ranges.

First, for the lower burn rate tests (category 1 and 2), two pre-burn fuel loads should be burned in the stove prior to the actual test load. The stove should be shoveled out and the ash pan emptied after the first pre-burn load. This will help insure that the stove reaches a good equilibrium temperature and that the test runs will not exceed the allowable stove body "Delta T" requirements.

For the lowest air setting, the door should be left slightly open for the first 90 seconds and the air control should remain fully open for the full five-minute start-up period and then fully closed.

If this results in a burn rate above one kilogram per hour, repeat the procedure but close the air control in small increments starting at three and one-half minutes.

If the initial burn rate is below one kilogram per hour, repeat the test conditions to obtain a second run in category 2.

For the maximum burn rate test, it is not necessary to leave the door cracked open after loading the test fuel. Just be sure to add enough pre-burn fuel to obtain a good charcoal bed and make the one-hour required pre-burn time period.

For category 3, we recommend setting the air control lever to a position where the uppermost corner of the end of the control lever is 1.75" from the lowest plane of the ashlip. The door should be cracked open for 90 seconds and the air control set at maximum for the first five minutes.

These settings should be used as a guideline. Adjustments to meet the required burn rate categories should be made if needed based on your best judgements.

Sincerely,

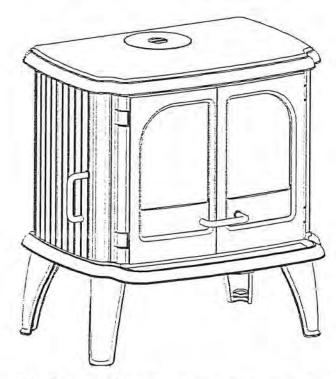
Bob Ferguson
Robert W. Ferguson



## **Installation and Operating Instructions**

3600

For use in North America



Read this entire manual before you install and use your new room heater. If this room heater is not properly installed, a house fire may result. To reduce the risk of fire, follow the installation instructions. Failure to follow instructions may result in property damage, bodily injury, or even death.

Contact local building officials about restrictions and installation inspectionequirements in your area.

Save these instructions

MORSØ JERNSTØBERI A/S . DK-7900 NYKØBING MORS E-Mail: stoves@morsoe.com · Website: www.morsoe.com

Distributed by: HEARTHLINK INTERNATIONAL 9 Maple St. - Randolph, Vermont - 05060 - USA

We congratulate you on your choice of a Morsø stove. Morsø has been producing some of the world's best stoves since 1853. If you follow this installation- and operating instruction carefully, we can assure you many years of warmth and pleasure.

#### **Optional Accessories**

A wide range of accessories (such as handling gloves, fireside tools, glass cleaner and heatproof paint) are available for use with your Morsø stove. They help with day-to-day running and maintenance. Contact your Morsø dealer for more information.

The Morsø 3600 meets the U.S. Environmental Protection Agency's emission limits for wood heaters sold on or after July 1, 1990



The Morsø 3600 have been tested by Intertek Testing Services and is listed by Warnock Hersey, Inc. The test standards are ANSI/UL-1482 for the United States and ULC S627 for Canada.

The stove is listed for burning wood only. Do not burn other fuels.

CONT	TENTS:		ear en seu.	
1.0	Insta	llation of your Morsø stove		
	≥ 1.1	Checking loose parts in the stove	4	14
	1.2	The chimney / flue system	4	
	1.3	Flue Connection	5	
	1.4	Connection to existing chimney	6	
	1.5	Positioning the stove	8	
2.0	Opera	ation		
	2.1	Before you start firing	10	
	2.2	Lighting and loading intervals	11	-
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	3.1	Exterior maintenance	12	. 7
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) 	3.3	Cleaning the Stove and the Flue	14	
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	3.5	Parts diagram	17	
	3.6	Parts list	18	7-3

## 1.0 Installation of your Morsø stove

Installation of woodburning stoves must be safe and legal.

If your Morsø stove is not installed correctly, it may cause a house fire. To reduce the risk of fire, the installation instructions must be followed carefully. Contact the local building officials about restrictions and installation inspection in your area.

Before you start installing your stove, make sure that:

- The stove and chimney connection are placed far enough from combustible materials to meet all clearance requirements.
- The floor protection must be adequate and must be made correctly according to 'the requirements.

All neccessary approvals are needed from the local building officials.

The data plate, which is located on the back of the stove, provides information regarding safety testing information, name of certified testing laboratory, and installation requirements.

Installation requirements vary in different districts, and the local building officials have the final authorization to approve your installation. You should discuss the installation with them before beginning. Please ask your dealer for further information.

Do not connect to any air distribution duct or system.

Important: If the installation instructions are not followed carefully, it may cause dangerous situations like chimney - and house fires. Follow the instructions carefully and do not deviate from them as it may cause injuries to people or property.

## 1.1 Checking loose parts in the stove

After unpacking, check that the fire bricks are firmly in position and have not shifted in transit. Check also that the air control works freely.

#### Standard Accessories

Poker, ceramic flue connection gasket and ash can tools are standard accessories, and can usually be found in the ashpan or firebox area.

## 1.2 The chimney / flue system

Note that the flue system must be independently secured and must not rely on the stove for support.

The stove must not be connected to a chimney flue serving any other appliance. (Several flues may run up a single chimney stack; use one flueway per appliance).

Use a residential type masonry or listed type HT factory-built chimney.

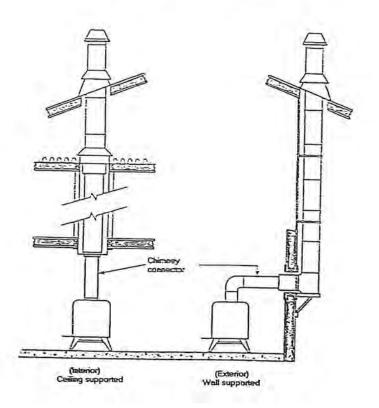
High Temperature (H.T.) Chimney Standard UL-103-1985 (2100° F.) for the USA, and High Temperature (650°C) Standard ULC S-629 for Canada.

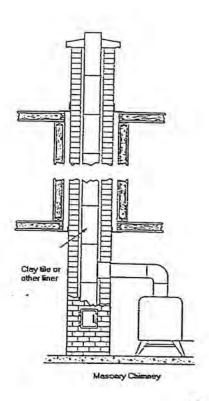
The internal dimensions of the chimney connector and chimney must not be less than 6 inches diameter (or equivalent cross section), and should not be significantly larger than this. Too large a section will tend to allow the flue gases to cool excessively, causing sluggishness or unpredictability in the stove's performance.

We recommend the length of the chimney system should be at least 16 feet (not required) above the stove in normal domestic situations, measured from the flue collar to the top of the chimney.

Local conditions like for example - roof constructions, large trees nearby and high altitude, may influence the chimney draft and height. Therefore, contact the local professional chimney sweep or your Morsø dealer.

## Typical Factory-Built or Masonry Chimney Installations





#### 1.3 Flue Connection

The stove is supplied from the factory with a flue collar fitted to the top plate and a round blanking plate blocking off the rear flue exit (behind the rear shield plate).

Use a 24 MSG black or blue chimney connector or listed double wall chimney connector. Refer to local codes and the chimney manufacturer's instructions for precautions required for passing a chimney through a combustible wall or ceiling. Remember to secure the chimney connector with a minimum of three screws to the product and to each adjoining section. The collar can be fitted to the rear outlet. Simply knock out the round panel on the rear heat shield plate to reveal the cast iron plate. Untwist the blanking plate and the flue collar and swap

their positions. Re-secure by pushing down and tighten the enclosed screws.

Position the stove and connect to the flue system.

Wear gloves and protective eyewear when drilling, cutting or joining sections of chimney connector

## 1.4 Connection to the existing chimney

A chimney connector is the double-wall or single-wall pipe that connects the stove to the chimney. The chimney itself is the masonry or prefabricated structure that encloses the flue. Chimney connectors are used only to connect the stove to the chimney.

Double-wall connectors must be tested and listed for use with solid-fuel burning appliances. Single-wall connectors should be made of 24 gauge or heavier gauge steel. Do not use galvanized connector; it cannot withstand the high-temperatures that smoke and exhaust gases can reach, and may release toxic furnes under high heat. The connector must be 6 inches (150mm) in diameter.

If possible, do not pass the chimney connector through a combustible wall or ceiling. If passage through a combustible wall is unavoidable, refer to the sections on Wall Pass- Throughs. Do not pass the connector through an attic, a closet or similar concealed space when installing the chimney connectors.

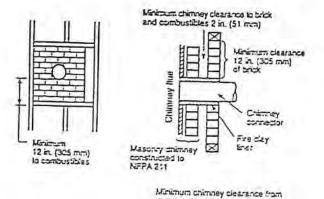
It is important to keep the flue gases moving smoothly in the right direction. Do not vent into a large void at this location; rather form one continuous section all the way up. Use mild bends (e.g. 45° vs. 90°) rather than sharp angles where a change of direction is required. All parts of the venting must be accessible for cleaning purposes.

In horizontal runs of chimney, maintain a distance of 18 inches from the ceiling. Keep it as short and direct as possible, with no more than two 90 degree turns. Slope horizontal runs of connector upward 1/4 per foot (20 mm per metre) going from the stove toward the chimney. The recommended maximum length of a horizontal run is 3 feet (1 metre), and the total length should be no longer than 8 feet (2.5 metres).

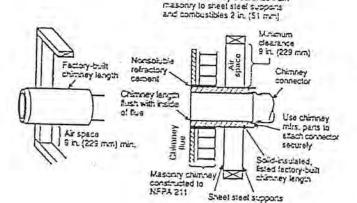
Information on assembling and installing connectors is provided by the manufacturer's instructions exactly as you assemble the connector and attach it to the stove and chimney.

Be sure the installed stove and chimney connector are correct distances from near by combustible materials. See the clearance paragraph page 8.

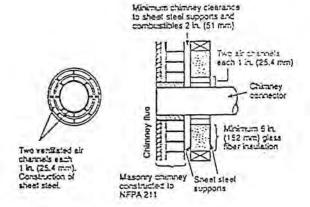
## Chimney Connector Systems and Clearances from Combustible Walls for Residential Heating Appliances



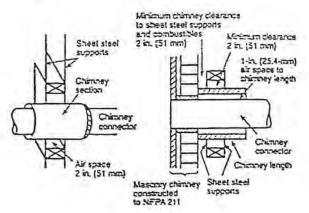
A Minimum 3.5-in thick brick masonry all framed into combustible wall with a minimum of 12-in brick separation from clay liner to combustibles. The fireclay liner shall run from outer surface of brick wall to, but not beyond, the inner surface of chimney flue liner and shall be firmly cemented in place.



B Solid-insulated, listed factory-built chimney length of the same inside diameter as the chimney connector and having 1-in. or more of insulation with a minimum 9-in. air space between the outer wall of the chimney length and combustibles.



C Sheet steel chimney connector, minimum 24 gauge in thickness, with a ventilated thimble, minimum 24 gauge in thickness, having two 1-in. air channels, separated from combustibles by a minimum of 6-in. of glass fiber insulation. Opening shall be covered, and thimble supported with a sheet steel support, minimum 24 gauge in thickness.



D Solid insulated, listed factory-built chimney length with an inside diameter 2-in. larger than the chimney connector and having 1-in. or more of insulation, serving as a pass-through for a single wall sheet steel chimney connector of minimum 24 gauge thickness, with a minimum 2-in. air space between the outer wall of chimney section and combustibles. Minimum length of chimney section shall be 12-in. chimney section spaced 1-in. away from connector using sheet steel support plates on both ends of chimney section. Opening shall be covered, and chimney section supported on both sides with sheet steel supports securely fastened to wall surfaces of minimum 24 gauge thickness. Fasteners used to secure chimney section shall not penetrate chimney flue liner.

## 1.5 Positioning the stove

#### Distance to walls and lintel

When the stove is positioned near <u>combustible</u> materials, observe all current local and national building regulations with regards to clearances. Whatever regulations apply to your area, do not in any case install the stove within 8 inches of combustible materials around the sides or 16 inches above the top of the stove (fireplace installations require greater clearances above the stove - see below in the clearance chart). These distances may need to be increased if the materials are sensitive to heat. Note also that wall paper and other decorative materials may become detached with the effects of heat and care should be taken to ensure that they do not fall towards the stove in such an event.

When the stove is positioned near <u>non-combustible</u> materials, a gap of 4 inches or more is recommended for cleaning purposes and to ensure that heat circulates around the stove and out into the room.

Appliance Clearances

Chimney connector	Unprotect	ted Surfaces	1	Protected	Surfaces (I	es (NFPA-211)			
clearances	Par	allel	Corner	Par	allel	Corner			
	Side	Rear		Side	Rear				
Single wall connector	-in	-in	-in	-in	-in	-in			
	-mm	-mm	-mm	-mm	-mm	-mm			
Double wall connector	-in	-in	-in	-in	-in	-in			
	-mm	-mm	-mm	-mm	-mm	-mm			

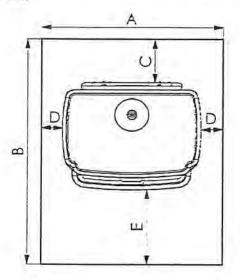
Fireplace Hearth Installation							
	In	Mm		ln	Mm		
Unit to top trim		1	Unit to side trim				
Unit to mantle			Unit to sidewall				

#### On the floor

If the stove is to be placed on a combustible floor, a, solid, non-combustible layer should cover the floor beneath the stove. This layer should cover an area of at least 16 inches in front of the stove doors and at least 8 inches either side of the opening and 6" to the rear. You must ensure that the floor in this area can hold the weight of the stove comfortably.

The floor protection in front of the unit must have an insulative R-value of 1.0 (English units).

In Canada non-combustible floor protector is required under the stove as well. The floor protector must extend 18 inches (460mm) to the front and 6 inches (155mm) from the sides and rear.



	U.S.	Cana	ada
A.	"	" (	mm)
В.	33	" (	mm)
C.	22	" (	mm)
D.	31	" (	mm)
E.	11	" (	mm)

#### Distance to furniture

The recommended minimum distance from stove to furniture is 30 inches. Note that some furniture is more easily affected by heat and may need to be moved to a greater distance. This is your responsibility.

In addition other combustible materials, away from the stove. In general, a distance of 30 inches must be maintained between the stove and moveable combustible item such as drying clothes, newspapers, firewood etc.

#### Note:

#### Acid Protection

If acid-washing the masonry around the stove, protect the stove surface with an acid-proof cover

#### Fresh Air Inlet

Unless there is deemed to be sufficient ambient leakage of air into the room via doorways, windows and the like, a dedicated fresh air inlet will be needed. This inlet should have 2 square inches (1250 square mm) of free air space. This is particularly importent where the room is well sealed, or where an extractor hood or ventilation system disturbs the natural air pressure. Such an inlet should not be on a wall that is usually subject to negative pressure from normal wind pattern. Avoid placing the inlet directly across the room from the stove, thus causing a cold air draft.

## 2.0 Operation

## 2.1 Before you start firing

For Use with Solid Wood Fuel Only. Do Not Overfire, If Heater or Chimney Connector Glows You Are Overfiring. Inspect and Clean Chimney Frequently. Under Certain Conditions of use creosote buildup may occur rapidly. Because of risk of smoke and flame spillage, operate only with door fully closed.

#### Caution:

Hot while in operation. Keep children, clothing and furniture away. Contact may cause skin burns.

Do not use chemicals or fluids to start the fire.

Do not burn garbage or flammable fluids.

Do not use gasoline, gasoline-type lantern fuel, kerosene, charcoal lighter or fluid or similar liquids to start or freshen up a fire in this heater. Keep all such liquids away from the heater while it is in use.

#### Choosing your fuel

All types of natural wood can be burned on your stove, but they must be well-seasoned and dry. Once the wood is cut to length, it should be split down middle - to suit the dimensions given below - to allow moisture to evaporate.

Cut the wood to a length of max 22 inches (56 cm) and approx. 3 to 3.5 inches (7-8 cm) in section. If you can weigh your wood, aim for around 1.0 kg. The maximum moisture content of the wood should be around 20%.

Store the logs under cover in a location where fresh air can move through the stack. Some soft woods may take as little as one good summer to season whereas harder woods such as oak, maple, and elm may require seasoning up to 18 months. Avoid overly dry wood that is gray in color as it can cause performance problems, such as backpuffing and sluggishness, under certain conditions. Well seasoned wood will be remarkably light to hold and will probably have radial cracking at the ends. If your wood spits or sizzles when burnt, and your stove's door glass persistently mists up, your wood is not properly seasoned. Never use drift wood (from the sea), whose salt content may cause corrosion, nor construction wood that may have been impregnated with chemicals.

## Starting the First Fire

The initial fire should be small, so that the stove paint can cure and the main plates of the stove can settle into position. Some fumes will be given off by the paint. Ventilate the room during this phase.

The setting of the air control, lighting techniques and loading intervals will depend on chimney draft, the fuel used, the heat required and so on. Some basic techniques are outlined below.

## In principle

Your stove is fitted wih Primary and Secondary air inlets.

Primary Air is controlled using the lever situated under the ash lip of the stove. Moving the control lever into a downward position will open the air inlet and will allow a supply of preheated air to enter the firebox via the 'airwash' system situated inside the stove and the above glass.

Secondary Air is right to the firebox using the specially designed baffle at the back of the firebox. The secondary air is injected into the flue gases both above and in front of the fire resulting in a cleaner, more efficient combustion process. The supply of secondary air is fixed open and is not adjustable.

For extra safety, your stove has been fitted with a removable handle. When not in use the handle can be stored using the lug by the right leg of the stove.

## 2.2 Lighting and loading intervals

When first lighting the stove, a large volume of air is needed. When the stove is cold, you should leave the door open an inch or two for the first few minutes and open the primary air supply completely. While the doors is open, do not leave the stove unattended.

To form a reasonable bed of ash on the floor of the stove, you should use 5-6 inches thickness (2-4 pound) of dry kindling at the initial lighting. Always maintain a 1-1.5 inch (2-3 cm) layer of ash on the floor of the combustion chamber at all other times.

#### Step-by-step procedure

- 1. The air supply must be fully open.
- 2. Light the fire. An ember bed will quickly be formed by lighting with firelighters, morsø kindling bags or 7-10 pieces of twisted paper under the dry kindling wood (see above).
- 3. After lighting, partially close the doors, leaving them open an inch or two to allow in plenty of combustion air.
- 4. When the chimney is warmed through after 5-10 minutes, the doors should be closed. A suitable ember bed will be formed after a further 15-20 minutes.
- 5. When ready to reload, use a poker to spread the ember across the firebox floor, bringing plenty towards the front of the stove.
- 6. Lay three pieces of wood (see dimensions above) onto the embers. Leave half an inch (1 cm) or more between each piece. When using 10 inches (25 cm) logs, place the ends of your logs towards the opening, but not too close to the front.





- 7. Close the door. Leave the primary air supply fully open.
- 8. After a few minutes, and adjust the primary air supply to suit your heating requirements.
- Anticipate each refueling, remembering to add a modest layer of wood while there are still plenty of live embers, Repeat steps 5-8.

11

Do not for any reason attempt to increase the firing of your heater by altering the air control adjustment range outlined in these directions.

Warning: Fireplace stoves must never be left unattended with doors open.

If doors are left partly open, gas and flame may be drawn out of the fireplace stove opening, creating risks from both fire and smoke. We recommend you to fit a smoke detector in the room where the stove is installed.

DO NOT OVERFIRE THIS HEATER. Overfiring may cause a house fire, or can result in permanent damage to the stove. If any part of the stove glows, you are overfiring.

#### Draft conditions

If smoke or fumes come out of your stove when lightning up and reloading, or if the fire simply will not respond, a poor draft is almost certainly to blame. (In a very few cases, there may be insufficient fresh air getting into the room - see installation advice above). Take advice from your stove supplier on how best to upgrade your flue system to improve draft.

#### Rules of woodburning

If you want less heat, put fewer logs on the stove and reduce the amount of air. It is still important to maintain a good layer of embers.

Less heat - less wood - less air

Greater heat - more wood - more air

Soot deposits will settle on the glass if the stove is run too slowly or if your wood is not well seasoned.

## 3.0 MAINTENANCE

When perfoming maintenance on your stove, always protect yourself, using safety goggles or gloves

#### 3.1 Exterior Maintenance

The stove surface is painted with heat-resistant Senotherm paint. It is best kept clean by vacuuming with a soft brush attachment or by wiping with a lint-free cloth.

Over a period of time, the painted surface may become slightly grey. A can of Morsø touch-up spray paint should be available from your stove supplier. This can be applied - in accordance with the instructions - in just a few minutes. When first firing after touching up, the stove will give off a slight smell as the paint cures. Make sure to ventilate the room well during this phase.

### 3.2 Internal maintenance

#### Glass

If the stove is generally run at the correct temperatures, there should be little or no dirt on the glass. If dirt does settle during lighting, most will burn off as temperatures increase. For heavier deposits that will not burn off, use morsø glass cleaner, applied when the glass is cold, in accordance with the instructions. Never use abrasive cleaners on the glass surface.

## Reasons for dirty glass

- · Fuel too wet
- · Logs too large or not split
- · Combustion temperatures too low

Replace broken glass immediately.

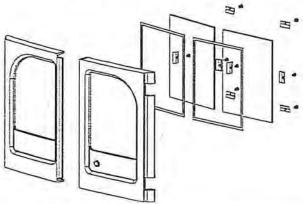
Do not operate your stove if the glass in the door is damaged.

If you need to replace the glass, it should be replaced with the high temperature ceramic class supplied by Morsø, contact your Morsø dealer.

#### Installing the glass

Never install the glass when the stove is in function.

 Lift the door off its hinges an place face-down on a sheet of cardboards or other nonabrasieve fabric.



- 2. Unscrew the 4 bolts that secure the glass. (In the event that a bolt sheers off when being unscrewed, remove the remaining body of the bolt by drilling down its cnetre with 1/8 inch high speed steel drill bit. Smaller drill bits may be successful, but do not use a lager bit. Make sure the bit stays away from the edges of the bolt this may damage the thread in the cast iron).
- 3. Remove the old ceramic gaskets and clean up the surface underneath with wire wool or emery paper to remove loose particles.
- 4. Place the new gasket material in position around the perimeter of the window area, making sure to pinch them to the length in such a way that they make a continuous seal. Leave no gaps.
- Place the new glass in position on the strips and screw home the fresh bolts and fitting by hand.
- 6. Finally, give each of the bolts an extra half turn or so. The glass should held tight enought that cleaning will not dislodge it. Do not over-tighten the bolts as this may put excessive pressure on the glass, resulting in cracking important!

To reduce the risk of breaking the glass, avoid striking the glass or slamming the door.

#### Internal service parts

The flame-path equipment - consisting of the ashpan, grate, firebricks, Cast iron fire plates, glass, baffle and flue collar - are subject to the extremes of heat produced by the fire. From time to time, one or other of these parts may need replacing as a matter of routine maintenance.

NOTE: The flame-path equipment, the ceramic rope and the paint finish are not covered by guarantee.

All of these service parts can be bought from your morsø dealer, and we recommend that damaged parts are replaced as soon as possible to avoid collateral damage.

Should the baffle be distorted by an overfire, the stove will still function, although its efficiency may be compromised. Replace it as soon as possible. The radiation shield on the back of the stove is first removed by loosening the 4 screws. The rear casing is removed (four bolts). Remove these and remove the 2 M8 bolts keeping the baffle plate, withdraw the baffle from the firebox.

Before replacing the baffle, scrape out the old fire furnace and replace with new to make an effective seal.

#### Reasons for fast internal wear and tear

Persistent heavy firing Soot and ashes left to accumulate

#### Ceramic Gasket

The gasket around the perimeter of the doors may harden over a period of time. It should be replaced if it becomes difficult to close the doors or if air starts to leak in around the perimeter of the doors, causing the fire to become a little less controllable. A morsø rope gasket kit is available from your stove supplier.

#### 3.3 Cleaning the Stove and the Flue

Check for soot above the baffle plate and around the flue outlet every month or so to start with. If the stove suddenly becomes sluggish, check for a soot fall around the flue collar or in the flue/chimney. - at least once a year. Inspect every month.

Clean the flue/chimney - all the way from the stove to the flue terminal point above the house.

A good routine is to clean the flue after each heating season in any case, and inspect prior to the season to ensure that bird's nests or other blockages have not ocurred during the off season.

#### Ash disposal

Empty the ashpans on a daily basis or as needed. Ash allowed to build up towards the underside of the grate will trap heat and could cause premature failure of the grate.

#### Empty the ashpan according to this procedure:

Open the front doors, and use a shovel or poker to stir excess ash through the ash slots in the grate down into the ash pans. Remove the ash pans, making sure to keep it level.

grate down into the ash pans. Remove the ash pans, making sure to keep it level.

Dispose the ash in a metal container with a tight fitting lid.

The closed container of ashes should be placed on a noncombustible floor or on the ground, well away from all combustible materials, pending final disposal. If the ashes are disposed of by burial in soil or otherwise locally disperded, they should be retained in the closed container until all cinders have thoroughly cooled.

Return the ash pans to its original position in the stove, and close.

#### Caution:

Never empty a stove in operation.

Never use your household or shop vacuum cleaner to remove ash from the stove; always remove and dispose of the ash properly.

Creosote - formation and need for removal

When wood is burned slowly, it produces tar and other organic vapors, which combine with expelled moisture to form creosote. The creosote vapors condense in the relatively cool chimney flue of a slow-burning fire. As a result, creosote residue accumulates on the flue lining. When ignited this creosote makes an extremely hot fire. When burning wood, inspect the chimney connector periodically to determine if a creosote buildup has occurred.

#### Chimney sweeping

Inspect the system regularly during the heating season as part of a regular maintenance schedule. To inspect the chimney, let the stove cool completely. Then, using a mirror, sight up through the flue collar into the chimney flue. If you cannot inspect the flue system in this fashion, the stove must be disconnected to provide better viewing access.

Clean the chimney using a brush the same size and shape as the flue liner. Run the brush up and down the liner, causing any deposits to fall to the bottom of the chimney where they can be removed through the clean-out door.

Clean the chimney connector disconnecting the sections, taking them outside, and removing any deposits with a stiff wire brush. Reinstall the connetor sections after cleaning, being sure to secure the joints between individual sections with sheet metal screws.

If you cannot inspect or clean the chimney yourself, contact your local Morsø Dealer or a professional chimney sweep.

## If you do experience a chimney fire, act promptly and:

Close the air control.

Get everyone out of the house.

Call the Fire Department.

#### Annual maintenance

Before the heating season, perform a thorough cleaning, inspection and repair:

Thoroughly clean the chimney and chimney connector.

Inspect the chimney for damage and deterioration. Replace weak sections of prefabricated chimney. Have a mason make repairs to a masonry chimney.

Inspect the chimney connector and replace any damaged sections.

Check gasketing for wear or compression, and replace if necessary.

Check the glass for cracking; replace if needed.

Check door and handles for tightness. Adjust if needed.

## 3.4 Leaving the stove for extended periods

#### Important:

If the stove is to be left unused for any period of time, clean it out thoroughly and leave the air control slightly open to allow airflow. Make sure that the flue does not allow rainwater to come anywhere near the stove; install a chimney cap, but do not block off the flue completely.

These measures should ensure there is a slight movement of air through the stove, and that the body of the stove remains dry, right into the corners.

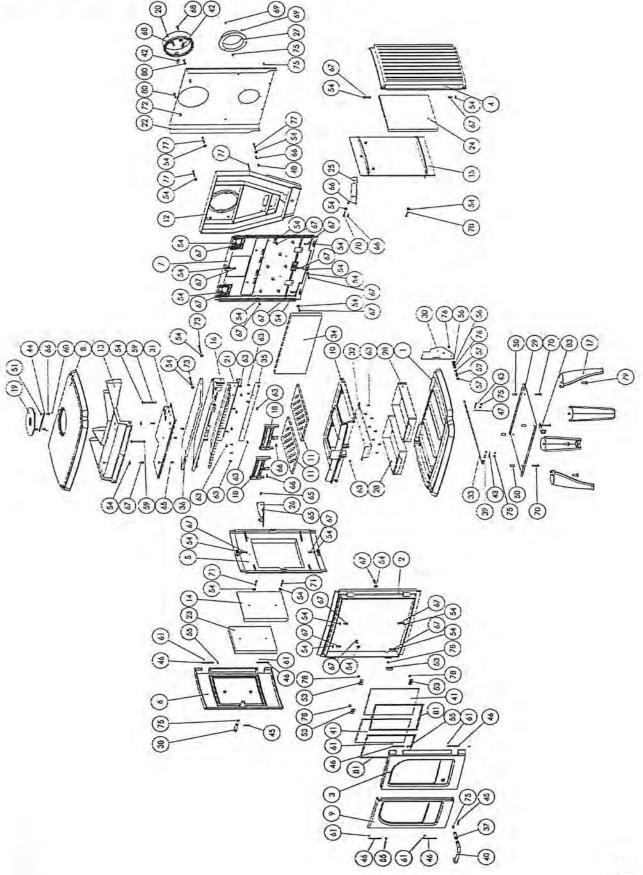
Any ash left within an unfired stove can attract moisture like blotting paper. If moisture is allowed to settle within the stove, rust will form. Rust expands as it takes a grip. This can lead to undue pressure on the stove joints, and this in turn may result in damage to the stove.

NOTE: It is best to thoroughly clean the stove after the heating season has concluded. Adding a dessicant, such as kitter litter, into the ash pan helps absorb moisture during the summer months. Be sure to remove this prior to the heating season.

#### Thank you for buying a morsø stove.

We hope you have many years of carefree warmth in its company. Some initial experimentation with loading and running techniques will decide your normal routine. If you have any problems after this short learning phase, please refer to your stove dealer. Should they be unable to help for any reason, please contact us in writing at the address on the front of this publication.

## 3.5 Parts diagram for model Morsø 3600



# 3.6 Parts list for model Morsø 3600

Pos.No.	Parts
1	Base plate
2	Front frame
3	Door right
4	Side plate
5	Side frame
6	Door side
7	Inside rear plate
8	Top plate
9	Door left
10	Intermediate frame
11	Grate
12	Outside back plate
13	Inside top plate
14	
15	Fire plate for side plate
16	Fire plate for side plate
17	Baffle plate, cast iron
18	Leg
19	Front grate Cover
20	Flue collar
21	
22	Baffle plate, stainless
23	Convection rear plate
24	Stone side door
25	Stone side plate
26	Angle brace f. fire plate
27	Angle brace f. sideframe (Lefthand sidedoor)
28	Airadaptor
29	Ash tray
30	Radiant shielding, bottom
31	Draught control
32	Baffle plate, stainless, inside top
33	Plate for intermediate frame
34	Air inlet arm
	Stone back
35	Securing bracket f. back brick
36 37	Insulation
	Axis for handle
38	Axis for handle
39	Stainless handle for adjustment
40	Door handle, stainless steel
41	Ceramic glass
42	Fitting w. thread for flue collar
43	Assemble steel
44	Flat bar
45	Hinge pin
46	Hinge pin
47	Cotter pin

48	Distance tube
50	Distance tube
51	Distance tube
52	Pressure spring, stainless
53	Glass fitting
54	Washer
55	Washer
56	Washer
57	Washer
59	Screw
60	Screw
61	Screw
63	Screw
65	Screw
66	Screw
67	Screw
68	Screw
69	Screw
70	Screw
71	Screw
72	Distance tube
73	Screw
74	Screw
75	Screw
76	Nuts
77	Screw
78	Screw
79	Screw
80	Screw
81	Tightening tape
83	Hanging for handle

# APPENDIX H

#### TUNNEL FLOW RATE

Tunnel flow rates are determined using the velocity pressure measurement made by a standard Pitot tube. The Pitot tube is located at the center of the dilution tunnel. Three x/y axis traverses were used to determine the relationship between the center velocity pressure and the average obtained by traversing. This procedure was carried out in accordance with EPA Method 2.

Velocity pressure and tunnel temperature data are used to calculate tunnel velocity via EPA Method 2, equation 2-9 as follows:

$$T_{v} = K_{\rho} * C_{\rho} * \sqrt{\Delta P} * \sqrt{\frac{T_{s}}{P_{s} * M_{s}}}$$

Where:

 $K_p = 85.49$  (English units constant for ft/sec.)

 $F_p$  = Pitot tube center point coefficient determined from traverses

 $C_p = .99$  Coefficient for standard pitot tube

 $\Delta P$  = Pitot tube velocity pressure (in. w.c.)

Ts = Absolute tunnel temperature (1R)

Ps = Absolute tunnel pressure (in. Hg)

Ms = Mole. Wt. of tunnel gas stream (lb./lb.-mole, wet basis) = 29

\* (1-.04) + 18 \* .04 = 28.56

 $T_v = Tunnel velocity (ft./sec.)$ 

Tunnel flow is calculated by multiplying the average velocity as calculated by the above formula by the following equation (adaptation of EPA Method 2, formula 2-10).

$$T_f = \overline{T_v} * 60 * 0.1961 * \frac{528}{TT_{ace}} * \frac{PS}{29.92} * 1 - .04$$

Where:

 $\overline{T}v$ 

= Average tunnel velocity (ft/sec.)

0.1961 = Tunnel cross sectional area (ft5)

 $T_f = Tunnel flow rate (SCFM)$ 

 $TT_{ave} = Average tunnel temp. (1R)$ 

PS = Average barometric pressure during test.

60 = sec. to min. conversion

0.04 = Assumed tunnel moisture content (4% by Vol.)

#### 2. EMISSIONS RATE CALCULATION

Emissions rates are calculated from the total weight gain of the probe and first and second filters of each sampling system as follows:

$$ER = \left(\frac{T_f * Wt.Gain * 60}{vol.sampled}\right)_{0.83} * 1.82$$

Where:

ER = Emissions rate (grams/hour OM7 equivalent)

Vol. Samp. = Total volume sampled (SCFM, Dry) Wt. Gain = Total weight gain for filter system (grams)

 $T_f = Tunnel flow rate (SCFM, Dry)$ 

#### CORRECTIONS TO STANDARD CONDITIONS

The tunnel flow rate is corrected to standard conditions through the EPA Method 2 formulae. The volume sampled is measured by dry gas meters and must be corrected for meter temperature and ambient barometric pressure. The inlet and outlet temperatures of each dry gas meter are measured and recorded at 10-minute intervals during the test. The ambient barometric pressure is recorded at the beginning and end of each test.

The following formula is used to correct the total volume as measured by the dry gas meter to total volume at standard conditions (681F, 29.92 in. Hg):

$$VOL_{std} = VOL_m * \frac{PS}{29.92} * \frac{528}{AMT} * Y$$

Where:

VOL<sub>std.</sub> = Total volume in Standard Cubic Feet

VOL<sub>m</sub> = Total volume as measured by dry gas meter.

PS = Average barometric pressure

AMT = Average meter temperature (1R)

Y = Dry gas meter calibration factor

pg. 3

#### **EXAMPLE CALCULATIONS**

#### TUNNEL VELOCITY

INPUTS: P = .038 in. w.c.  $T_s = 1001F$   $P_s = 29.3$  in. Hg.  $M_s = 28.56$  lb./lb.-mole  $C_p = .99$  $F_p = .945$ 

$$T_{\nu} = 85.49 * .99 * .945 * \sqrt{.038} * \sqrt{\frac{560}{29.3 * 28.56}} = 12.754$$

#### 2. TUNNEL FLOW RATE

INPUTS:  $T_v = 12.754 \text{ ft./sec.}$   $TT_{ave} = 5601R$ PS = 29.3 in. Hg.

$$T_f = 12.754 * 60 * 0.1961 * \frac{528}{560} * \frac{29.3}{29.92} * (1 - .04) = 133.0 SCFM$$

#### 3. EMISSIONS RATE

INPUTS:  $T_f = 133.0 \text{ SCFM}$ Wt. Gain = .0200 grams

Vol. Samp. = 100 Std. cubic feet

 $ER = \left(\frac{133 * .0200 * 60}{100}\right).83 * 1.82 = 2.68 \,grams / hour$ 

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### 4. VOLUME CORRECTION FOR DRY GAS METERS

INPUTS:  $VOL_m = 104.479$  (Metered Feet3) PS = 29.3 (Average baro. pressure) AMT = 801F (Ave. meter temp.) = 5401R Y = .9996 (Meter cal. factor)

 $VOL_{std} = 104.479 * \frac{29.3}{29.92} * \frac{528}{540} * .9996 = 100.00S \tan dardFt_3$ 

### APPENDIX I

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Model:	3600						Overall He	ating Efficienc	V:		67.71%	2
Date:	8/6/01						PI.	stion Efficienc	•		90.76%	
Run:	1.			3			Heat Tra	nsfer Efficienc	v.		74.61%	
Control #:	J20049092				10010000		372300740				74.0176	
Test Duration:	270		177.2	D		I was a	Heat Ou	itput	16303	BTU/Hr	17186	KJ/Hr
i de la caracteria de l		Start	End :	1		300000000	Heat In		24076	BTU/Hr	25381	
Baro	meter (in.Hg):	29.3	29.3	£	mar to te te ta strate	V in the recent of	1035000		2.101.0	D. O. II	23301	NJITI
	Wet Bulb (F):			1	market make a se	de estienne S	Burn Dur	ation:	4.50	Hours		
	Dry Bulb (F):	74	79		***************************************	30 - 10 11 10 10 2			4.00	Hours		
	Humidity (%):	84	63		AND THE PERSON IN	2- 31 3- 11-35 4-	Burn R	ate:	2.73	Lb/Hr	4 000	10-00
				enanananan ;	manata is is is is is a	9.90 mm.m.	Dulli	ate.	2.13	LD/M	1.239	Kg/Hr
Average Stove Tempor	erature:	#DIV/0!	5 or 17 to 18	1 15110001050	1 15 15 15 15 15 15 15 15 15 15 15 15 15	8	Stack T	emp:	336.1	Deg.F	168.9	Deg.C
oisture content of woo	d (wet basis):	17.36			2 6 6 11 11 11 11 11 11 11 11 11 11 11 11	9 000000		and a	5-0-1	oug.,	100.3	Deg.C
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						Section 2	Comb	Combust	Heat	Net	7.34471	0.599
Elapsed	Weight				Flue	Room	%	Eff	Transfer	Eff	air	1759
Time	Remaining :	CO	CO <sub>2</sub>	02	Gas	Temp	K	%	Transfer	Eff		Unit
0	14.87	1.23	7.15	12.31	375	10 00 00 00 00 00 00 00 00 00 00 00 00 0	0.04	90.9%	22.7%		Fuel	MN
10	13.00	1.70	5.17	14.11	438	90	0.49	74.2%	36.1%	20.6%	8	6.75
20	11.40	0.33	13.44	6.46	521	90	1.99	75.6%	57.7%	26.8%	11	5.90
30	9.40:	0,35	13.98	6.35	536	90	2.48	72.2%	64.6%	43.6% 46.7%	6	5.17
40	7.70	0.65	14.79	5.47	547	90	2.05	77.3%	71.0%	0.000	6	4.26
50	6.40	0,39	14.01	6.16	522	90	0.81	89.4%	75.8%	54.9% 67.7%	6	3.49
60	5.40	0.97	10.09	9.66	458	90	-0.04	95.8%	77.1%	73.8%	7	2.90
70	4.70	1,51	7.63	11.81	389	90:	-0.34	97.2%	78.3%	76.1%	10	2.45
80	4.10	1.28	7.65	11.93	358	90	-0.47	101.3%	80.8%	81.8%	15	2.13 1.86
90	3.50	1.16	8.24	11.31	358	90:	-0.68	106.4%	82.5%	87.8%	15	1.59
100	3.00	0.58	8.52	11.13	353	90	-1.06	119.8%	83.7%	100.3%	18-	1.36
110	2,70	0.36	7.85	11.93	332	90	-1.10	125.4%	84.1%	105.5%	21	1.23
120	2.40:	0.49	7.44	12.40	315	90	-0.93	120.6%	84.8%	102.2%	22	1.09
130	2.30	0.74	7.26	12.47	305	90	-0.88	116.9%	85.2%	99.5%	22	1.04
140	2.10	0.89	6.72	12.96	292	90	-0.83	115.3%	85.4%	98.4%	24	0.95
	2.00	0.87	6.52	13.21	280	90	-0.79	114.6%	85.8%	98.4%	25	0.91
160	1.80	1.01	6.27	13.43	273	90	-0.72	111.5%	86,1%	96.0%	26	0.82
	1.70	1.31	6.02	13.54	270	90	-0.66	107.0%	86.2%	92.2%	26	0.77
	1.60	1.46	5.84	13.71	266	90	-0.56	102.6%	86.3%	88.6%	26	0.73
	1.40	1.70	5.41	14.06	259	90	-0.47	97.9%	86.4%	84.6%	27	0.64
200	1,30	1.65	5.29	14.16	253	90	-0.53	100.2%	86.6%	86.8%	29	0.59
	1.20	1.61	5.18	14.24	249	90	-0.60	102.8%	86.7%	89.1%	31	0.54
	1.00	1.58	5.18	14.32	246	90	-0.51	100.2%	87.2%	87.4%	31	0.45
230	0.90	1.75	5.12	14.30	247	90:	-0.47	97.4%	87.3%	85.0%	31	0.41
240	0.60	1.84	4.94	14.49	247	90:	-0.37	93.3%	87.4%	81.6%	33	0.27
250	0.30	1.85	4.87	14.63	241	90	-0.25	89.4%	88.2%	78.8%	34	0.14
	0.10	1.64	5.11	14.48	242	90	-0.28	92.3%	88.6%	75.7%	36	0.05
270	0.00:	1.56	5.17	14.43	239	90	-0.32	94.3%	88.9%	83.8%	37	0.00

Model:	3600	0.000		i amar na ik		( (* )) (i		ada a Fred	al a		E CHEN	
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		Start	End	Green an and		*******	Heat Ou		12678	BTU/Hr	13364	
Raro	meter (in Hg):	29.28	29.26		*********		Heat In	put	18277	BTU/Hr	19267	KJ/Hr
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of the control of the section to the control of	TERREST HAT WORKS	75	- 00				Burn Dur	ation:	6.17	Hours		
	Dry Bulb (F):	75	80				10 5					
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verage Stove Tempe	roturo:	#DIV/0!	أويدة بناجه		1000000000000		2012					
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Elapsod			· Correction of the				Comb	Combust	Heat	Net		*
Elapsed	Weight	war in it is	Service and	man of	Flue	Room	%	Eff	Transfer	Eff	air	Un
The second second second second	Remaining	co	CO <sub>2</sub>	O <sub>2</sub>	Gas	Temp	K	%	Transfer	Eff	Fuel	MN
	15.54	0.51	7.90	11.90	324	90	-0.09	98.5%	33.8%	33.3%	8	7.05
	14.10	0.84	5.96	14.01	434	90	0.64	77.7%	35.5%	27.6%	11	6.40
	12.9	0.4	11.03	9.28	480	90	2.03	70.4%	49.6%	35.0%	6	5.85
	11.40	0.35	13.72	6.91	515	90	3.21	64.7%	57.1%	36.9%	5	5.17
40:	10.20:	0.48	14.20	6.35	527	89	3.13	66.6%	62.5%	41.7%	5	4.63
50	8.60	0.48	14.74	5.59	544	90	2.25	75.7%	69.4%	52.5%	5	3.90
60	6.80	0.28	13.09	7.30	509	90	0,95	87.4%	75.1%	65.6%	7	3.09
70	5.90	0.49	9.51	10.65	439	90	0.12	95.3%	76.6%	73.0%	11	2.68
80	5.30	0.60	8.90	11.20:	406	90	-0.08	98.0%	78.4%	76.9%	12	2.40
90	5.00	0.91	8.61	11.28	393	90	-0.19	98.1%	79.2%	77.7%	12	2.27
	4.70	0.77	7.27	12.51	351	90	-0.58	107.9%	80.0%	86.3%	16	2.13
	4.40	0.66	7.03	12.73	332	89	-0.76	113.9%	81.0%	92.3%	18	2.00
120	4.20:	0.40	6.99	12.96	315	89	-0.75	116.7%	82.0%	95.7%	19	1.91
130	4.00	0.63	6.57	13.21	301	90	-0.82	117.3%	82.4%	96.7%	20	1.81
140	3.80	0.74	6.59	13.11	294	90	-0.86	117.1%	83.1%	97.3%	20	1.72
160	3.60	0.87	6.01	13.74	281	89:	-0.72	112.9%	83.1%	93.8%	22	1.63
. 170	3.30	1.08	5.77	13.95	268	89:	-0.79	115.9%	83.6%	96.9%	23	1.59
180	3.20	CONTRACTOR OF SEC.	5.54	14.08	263	89	-0.75	112.5%	83.8%	94.3%	24	1.50
190	2.90	1.22	5.47	14.08	257	89	-0.73	110.6%	84.2%	93.1%	24	1.45
200	2.70:	1.41	5.55	14.00	254	89;	-0.78	112.4%	84.8%	95.4%	25	1.32
210	2.60	1.32	5.32	14.26	250 247	88	-0.72 -0.64	108.4%	84.9%	92.1%	25	1.23
220	2.40	1.42	5.24	14.21	246	88	-0.64	106.8% 108.9%	85.3%	91.1%	26	1.18
230	2.20	1.65	4.66	14.58	241	88:	-0.73	110.5%	85.4% 85.0%	93.0%	27	1.09
240	2.10	1.82	4.46	14.70	237	89:	-0.80	107.7%	85.1%	93.9%	30	1.00
250	1.90	1.83	4.40	14.76	233	88	-0.79	107.7%	85.4%	91.6% 91.7%	30	0.95
260	1,80	1.72	4.29	14.95	231	88	-0.78	108.4%	85.4%	92.6%	31	0.86
270	1.60	1.90	3,93	15.15	225	88	-0.84	109.2%	85.3%	93.1%	36	0.82
280	1,50	1.83	4.42	14.83	223	88	-0.67	102.9%	86.6%	89.2%	32	0.73
290	1.20:	1.88	4.01	15.14	218	88	-0.75	105.9%	86.4%	91.5%	37	0.54
300	1.10	1.84	3.68	15.54	213	88	-0.70	104.6%	86.2%	90.1%	40	0.50
310	1.00	1.77	3.51	15.66	208	88	-0.82	111.3%	86.1%	95.8%	44	0.45
320	0.80	1.85	3.45	15.73	204	88	-0.73	106.3%	86.5%	92.0%	45	0.36
330	0.70	1.88	3.44	15.74	202	88	-0.70	104.6%	86.8%	90.8%	45	0.32
340	0.60	1.87	3.28	15.88	200	88	-0.74	106.5%	86.6%	92.2%	48	0.32
350	0.40	1.68	3.60	15.77	202	88	-0.60	102.8%	87.5%	89.9%	47	0.18
360	0.20	1.89	3.47	15.72	201	88	-0.65	102.3%	87.5%	84.2%	48	0.18
370	0.00:	1.86	3.48	15.73	202	88	-0.64	102.1%	87.6%	89.4%	50	0.00

Model: Date: Run: Control #: Test Duration: Baromete	3600 8/8/01 3	energi.			exconomic may	and the second	Carlotte In the Alice of							
Run: Control # Test Duration: Baromete	3:		** ** ** ** ***		12 SEAL OF THE TEAL OF			ting Efficiency			59.14%			
Control #: Test Duration: Baromete		e ich ich			ta di atala di arabara			tion Efficiency			77.07%			
Test Duration: Baromete	85	Cecure in Se	reservati	aranin da			Heat Trans	sfer Efficiency			76.74%			
Baromete	85:					eneve	Vie. 10 85 6	TVY		Sharrer.				
	ALCOHOLDS AND AND ADDRESS OF THE				15 . 6 . 15 . 6 . 75 . 9 5 . 15	31. 91. 11. 11. 11. 1	Heat Out		49937	BTU/Hr	52642			
		Start	End			**********	Heat Inp	ut	84437	BTU/Hr	89012	KJ/Hr		
		29.04	29.03		Satisficación de la	31 31 31 28 38 3			4	44.11				
	t Bulb (F):	74			ACTION CONTRACTOR		Burn Dura	tion:	1.42	Hours				
	Bulb (F):	74	86					20		22.44	1124	50.21		
Hun	nidity (%):	79	61		***********		Burn Ra	ite:	9.05	Lb/Hr	4.104	Kg/Hr		
ويروانه والمراجع والمراجع	يرزف مستوري	SN 1101				Celarate			-2.5		2000	0.75		
rage Stove Temperatu	ire: #L	01V/0!			Crecrossessis	3X 94 3 ( ++ ) c +	Stack Te	emp:	714.7	Deg.F	379.3	Deg.C		
ire content of wood (w	40 40 30 40 70 70 40 43101.40	40.00.00.00	*****	TATALE.	74470	90.00	0.04004	0.40405447	4D0 404	#D11 (10)	4.00000			
	Average	0.19	9.10	11.04	714.70	89.80		0.10465447	#DIV/0!	#DIV/0!	1.99657	0.244		
	Majaht	n ======			This	Dann	Comb	Combust	Heat	Net		4.654		
the property of the second second second second	Weight				Flue	Room	%	Eff	Transfer	Eff	air	Unit		
and the second of the second second		co :	CO <sub>2</sub>	O <sub>2</sub>	Gas	Temp	K	%	Transfer	Eff	Fuel	MN		
0	15.69	0.02	0.19	19.79	658	88	0 40.730	-107.2%	-3.9%	4.2%	-61	7.12		
	11.20	0.25	19.71	0.41	1046	90		70.7%	44.5%	31.5%	4	5.08		
20	7.30	0.10	18.20	1.66	999	90		91.2%	64.0%	58.4%	5	3.31		
30	3.70:	0.04	13.65	6.13	855	90	Maria Carlo Carlo	116.1%	72.7%	84.3%	11	1.68		
40	2.30	0.06	9.06	10.99	732	90		122.1%	70.5%	86.1%	20	1.04		
50	1.60	0.07	7.38	12.92	659	90		118.3% 112.1%	69.3% 70.3%	81.9% 78.8%	27 30	0.73		
60 70	0.60	0.11	5.70	13.58	554	90	40.00	112.7%	68.9%	77.7%	39	0.45		
80	0.20	0.42	5.23	15.07	527	90	4 6 6	108.6%	68.7%	66,1%	43	0.09		
85	0.00	0.58	5.04	15.22	511	90		103.2%	69.0%	71.2%	44	0.00		
							-0.27	103.270	03.070	11.270	***	0.00		

Manufacturer:	Morso			1 44 4 4 4 4	- 201011104040404040	Season agra-		Hersey Efficien	-1 100111	-Heir		
Model;	3600	A morning	2			) M	Overall He	ating Efficiency	r		65.26%	
Date:	8/9/01							stion Efficience				
Run	4.			kon ir ir id i	19.151.65 inn mai			ster Efficiency			92.15%	
Control #.	120049092	a recession i		a - man dra			rieal Ital	isiei Ellicielic)			70.82%	
Test Duration:	193		~~~~	- cr ++ () +(2)	0.000-040-660-6		Heat Ou	the state	23263	DTI (6.6-		
4 11 11 11 11 11 11 11 11 11 11 11 11 11		Start	End	** ** 1130 114.	************	discussions.	Heat In	C. C. C.		BTU/Hr	24524	KJ/Hr
Baron	neter (in.Hg):	29	28.96	*******	received maring	Ten backer	rieatin	put.	35646	BTU/Hr	37577	KJ/Hr
TOTAL OR HE SELECTED SELECTED AND AN AN AND AND AND AND	Vet Bulb (F):	20	20.30	********	manaraem medesā	reconstruction (	Burn Dur	and a second	0.00	490.00		
THE RESERVE OF THE PARTY OF THE	Dry Bulb (F):	73	74				Buth Dut	auon.	3.22	Hours		
	lumidity (%):	63	70	o a security		*****	Down D	ake.	1.86		1200	VA 7457
• • • • • • • • • • • • • • • • • • • •	inning 7 Vov.	031		o maranaga		erenen	Burn R	ate:	4.03	Lb/Hr	1.827	Kg/Hr
Average Stove Tempe	rature:	#DIV/0!	on à manif	essención	(11)11111111111111111111111111111111111		Stack T	omn'	420.0	Deec	005 5	
sture content of wood		17.02			ee 50 se 50 1514-151-151		Stack I	emp.	438.6	Deg.F	225.9	Deg.C
	Average	0.61	6.73	13.29	438.62	88.10	-0.0452	0.27222877	4011/101	450.00	40.00	4.454
				10.20	430.02	00.10	Comb	A Charles of the Control of the Cont	#DIV/0!	#DIV/0!	7.04944	0.492
Elapsed	Weight		t er mer mej	annania alje	Flue	Room	%	Combust Eff	Heat	Net		- A
THE PERSON NAMED IN COLUMN TWO IS NOT THE PARTY.	Remaining	co	CO	0	STATE OF STREET	CHENCH COMPANY			Transfer	Eff	air	Unit
ALTERNATION OF THE PROPERTY OF	14 D + 35 11 15 10 (F + 12)	2 12 12 12 14 15	CO <sub>2</sub>	O <sub>2</sub>	Gas	Temp	K	%	Transfer	Eff	Fuel	MN
	15.61	0.32	5.00	14.90	431	84	-0.53	115.8%	27.1%	31.3%	15	7.08
	13.50	1.20	5.78	14.33	486	85	1.36	61.7%	27.1%	16.7%	10	6.13
30	11.60	0.18	10.80	9.37	601	85	1.59	76.0%	52.6%	39.9%	7	5.26
40	7.40	0.50	14.26	5.87	688	87	2.22	74.9%	61.3%	45.9%	6	4.26
50	5.10	0.43	12.19	7.94	636	88		86.8%	68.4%	59.4%	7	3.36
60	4.20	0.13	9.39	10.67	594	89	-0.25	102.8%	74.5%	76.6%	10	2.31
70	3,50	0.13	7.38	12.65	554	90	-0.75	114.3%	75.6%	86.4%	14	1.91
- 80	2.90	0.35	6.19	13.63	497	90		114.6%	75.3%	86.3%	19	1.59
90	2.60	0.38	5.72	14.34	451 409	89		132.6%	75.7%	100.3%	27	1.32
100	2.40	0.46	5.66	14.45	4	89	-0.76	122.3% 116.8%	76.7%	93.8%	29	1.18
110	2.10	0.51	5.68	14.43	390	89	-0.60	2.121277	77.8%	90.9%	29	1.09
120:	1.90	0.62	5.36	14.68	368	89		114.8% 114.4%	79.0%	90.6%	30	0.95
130:	1.50	0.59	5.51	14.58	365	88	-0.61	112.7%	78.8% 79.7%	90.2%	32	0.86
140	1.30	0.70	5.24	14.76	358	88	-0.58	113.0%	79.7%	89.8%	33	0.68
150	1.10	0.87	4.80	15.15	351	89	2027	108.8%	79.0%	89.9%	35	0.59
160	0.80	1.01	4.71	15.11	344	88	-0.55	108.9%	79.5%	86.0% 86.6%	38	0.50
170	0.50	1.01	4.54	15.37	339	88	-0.42	104.0%	79.5%		40	0.36
180	0.30	1.02	4.15	15.73	330	to do to the day.	-0.42	104.0%	78.8%	82.6%	42	0.23
AND ADDRESS OF THE PARTY OF THE			30 11 41 41 41 11		ACCUSATION ASSESSMENT OF A	88				83.1%	47	0.14
190	0.10	1.02	4.08	15.87	323	89	-0.35	101.1%	79.2%	73.5%	49	0.05

# APPENDIX J

## ITS Intertek Testing Services

Manufacturer Morso	Model 3600 Wood Stove	Date 5:/3/0/
Job#J20049092		2/11
Break-in Data log		
Type of fuel used: Recl Oak Moisture content corrected to 2-pin and for the	e type of fuel used.	
Catalytic	Non-catalytic ×	

Date	Time	Flue Temp	Comb. Cham. Or Catalyst Temp	lbs. Fuel weight added	Moisture content
8/3/01	12:25	54	84	3.5K. Endling	
8/3/01	12:30	387	590	17.5	19.8
8/3/01	14:08	552	836	12.08	201
7/3/0/	(5,58	792	606	216	240
ş.					

